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# Experiments on Incompressible Turbulent Boundary Layers with Distributed Injection

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Summary.

An extensive series of mean velocity measurements on the incompressible turbulent boundary layer with distributed injection is described. Boundary-layer developments have been measured along a porous flat plate under a variety of conditions, using 'Vyon' sintered polythene as the porous surface. The experiments included both zero and non-zero pressure gradients but were restricted to air-to-air injection without heat transfer. The boundary layer developments were measured with injection rates  $(v_0/U_1)$  between 0 and 0.008 at free stream velocities of 50 and 150 ft/sec while some additional velocity profiles at one station only with injection rates up to 0.0145 were also measured. In addition, an experiment on a bounary layer where the injection rate was suddenly reduced to very nearly zero has been carried out. Direct measurements have been made to determine whether any significant convergence or divergence of the tunnel flow or significant static pressure variations through the boundary layer were present. The question of the aerodynamic smoothness of the porous surface used is also discussed. All the results obtained are presented in tabular form.

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#### 1. Introduction.

The problem of maintaining the surface temperature of high speed aircraft within a metallurgically acceptable limit is becoming increasingly important as flight speeds increase. At high supersonic speeds, the air in contact with an aerofoil surface, and hence the surface itself, will attain high temperatures due to the temperature rise through the compression shock ahead of the aerofoil and the skin-friction heating at the surface. The upper temperature limit to which even advanced materials maintain their strength is considerably less than the temperature likely to be attained at the surface and hence some method must be used to protect the surface against such excessive temperatures. In gas turbines, the performance of the turbine increases with an increase in the gas temperature at the inlet. An improvement in performance will result in turbines having a higher power-to-weight ratio, which are therefore likely to be of importance as power plants for VTOL or long-range aircraft. The problem of protecting the exposed surfaces of the turbine from high temperatures is again present. The problem arises also in some industrial applications, a particular example being the outlet manifold from oxygen blown steel converters, which are at present water jacketed steel pipes requiring large amounts of expensive cooling water.

Various methods have been proposed for offering protection to such exposed surfaces, the methods being subdivided into internal cooling, where the coolant remains within the heated body, or external cooling, either by ablation of a suitable surface coating, or by transpiration of a gas or liquid through pores in the surface. The ranges of application of the different methods have been discussed by Eckert<sup>8</sup> and Dukes<sup>6</sup> for the high speed aircraft cooling problem, while some calculations on a transpiration cooled aerofoil have been made by Squire<sup>28</sup> who showed that transpiration cooling had an advantage over internal cooling. A transpiration cooled gas turbine has been described by Lombardo, Lauziere and Kump<sup>17</sup> who demonstrated the practical feasibility of the method.

We will here only be concerned with transpiration cooling, in which coolant gas, which may be different from the main stream gas, is injected into the boundary layer through the porous surface forming the body in contact with the hot stream. A considerable body of experimental and theoretical work on various aspects of this problem has been built up (for a recent review, *see* Ref. 12). Most of the work has, however, been confined, for the incompressible case, to boundary layers in zero pressure gradient while for compressible flow attention has been concentrated on the gross effects of injection.

A comprehensive programme of research into the problem of transpiration cooling has been initiated at the Cambridge University Engineering Laboratory, involving concurrent experimental investigations of both incompressible and compressible turbulent boundary layers with injection. The programme on compressible flow and the results obtained are described by Jeromin<sup>13</sup>. The present Report is concerned with an investigation of the incompressible turbulent boundary layer without heat transfer and with air-to-air injection only. A clear understanding of this (relatively) simple case is essential to an understanding of the more complex general problem.

At the outset of the present investigation, the primary objective was to obtain reliable data for such boundary layers with non-zero pressure gradients, particularly the large favourable pressure gradients with which are associated large values of the skin-friction coefficient. The case of constant pressure layers had been covered by the experiments of Mickley and Davis<sup>21</sup> and it was hoped that these measurements, together with the proposed measurements with pressure gradient, would allow a method to be developed for the calculation of layers with combined pressure gradient and injection.

Theoretically, there was available the extensive work of Black and Sarnecki<sup>1</sup> which showed good agreement with the results of Mickley and Davis in predictions of both the inner region velocity profile and the skin-friction coefficient. The experimental uncertainties in these measurements were such, however, that the later theory of Stevenson<sup>29</sup> also showed good agreement with the measurements, provided that pressure gradients which appeared to be present were taken into account, which had not been done by Black and Sarnecki. The theory of Stevenson was not reconcilable with that of Black and Sarnecki, considerable differences in skin-friction coefficient being obtained when each was compared to the measurements, although each theory was reconcilable with these measurements depending on whether the pressure gradient was or was not taken into account. Although the experiments were carried out in nominally zero pressure gradient, the tabulated values of free stream velocity do indicate that the pressure gradient was not zero. The detailed pressure distributions are not tabulated so that these gradients can only be obtained from the tabulated free stream velocities, which are widely spaced along the layer. The calculation of these gradients is thus liable to considerable uncertainties. A decision in favour of one or other of the proposals could not therefore be made on the basis of Mickley and Davis' data. For Stevenson's own less extensive data, the two theories did agree within the experimental errors. It was decided, however, in view of the uncertainties that it would be necessary to examine the constantpressure case anew before the work on pressure gradients could be commenced.

Detailed measurements on the constant-pressure layer have been made, with attention restricted to mean velocity measurements only; no hot-wire anemometer measurements have been made. Care has been taken to ensure that the two main sources of uncertainty in Mickley and Davis' experiments (i.e. the possible presence of appreciable pressure gradients and/or lack of two-dimensionality) had but small effect on the present data. Direct measurements were made to determine whether any flow convergence or divergence was present and provision was made for maintaining the pressure constant. Static pressures were measured at close intervals along the chord so that if any small but persistent departures from the mean pressure did occur, the resulting pressure gradients could be calculated accurately. Velocity profiles were measured in more detail than is usual and at close intervals along the layer. Experiments on three layers with different pressure gradients have also been carried out and the results are included in this Report.

A further purpose of the original programme of investigation was to determine which of the various ways in which the injection mass flow could be distributed over the surface would be the most effective in reducing the skin-friction coefficient. These different methods would include injection through spanwise porous strips or angled slots, as well as the case of uniform distribution. In addition, it is likely that surface construction considerations would dictate strip rather than uniformly distributed injection being used in practice. Little has, however, been done on this aspect of the problem, apart from an experiment on the boundary layer proceeding from a region of injection to the solid surface state, which will be a detail of the porous strip case. This layer, in which the profile shape factor, *H*, decreases rapidly with distance downstream from the cessation of injection, is of a type which is attracting considerable current

attention (see Bradshaw and Ferriss<sup>3</sup>). Although the experiment suffered from several inadequacies, the results obtained are sufficiently reliable from this point of view to warrant publication at this time. The programme of research is continuing and a more detailed examination of this type of layer is to be carried out.

This Report is concerned only with the details of the measurements which have been made. In the following sections, the wind tunnel and apparatus are described, together with the measurement techniques used. The detailed experimental results are presented in tabular form and the various measurements which were made to ensure the reliability of the results are discussed. Some of the results presented here have been used in a previous paper by the author<sup>18</sup> and also in the treatment of the compressible layer with injection<sup>14</sup>. The analysis of the measurements in the light of the theories of Black and Sarnecki, and Stevenson will be given elsewhere (Ref. 19).

#### 2. Wind Tunnel.

All the experiments to be described were carried out in an open-return suction type tunnel, a description of which has been given by Preston<sup>24</sup>. The free-stream turbulence level in the tunnel working section was 0.3 per cent at a free stream velocity of 100 ft/sec. The working section normally fitted had dimensions 20 in. high,  $7\frac{1}{2}$  in. wide and 40 in. long. For the present investigation, the tunnel was fitted with a new working section, the details of which are shown in Fig. 1. All the experiments were conducted on the vertical 20 in. side wall.

In order that the streamwise pressure gradient might be adjusted, the tunnel wall opposite the test wall was made flexible using 16 s.w.g. sheet steel. The flexible wall was set  $1\frac{1}{2}$  in. into the tunnel, with a smooth contraction at the upstream end and a trailing flap at the downstream end. The wall had three adjusting positions and could be used to obtain zero pressure gradient with injection rates up to about 0.014, or mild favourable gradients at any injection rate. Larger favourable gradients were obtained by attaching a blister to the flexible wall which, at maximum displacement, produced a 3:1 convergence of the tunnel width. Since the maximum divergence which could be obtained was limited by the maximum movement of the flexible wall (which was somewhat less than  $1\frac{1}{2}$  in. at the trailing edge), only comparatively mild adverse pressure gradients could be imposed, and then only at low injection rates. This shortcoming was not considered serious, however, since the combination of severe adverse gradients and injection is not of great practical interest. (Considerable practical difficulties would be involved in any attempt to obtain such a combination in this type of tunnel). With this flexible wall, a constant pressure distribution was easily obtainable as a small ripple about the mean pressure. However, because of the few adjusting positions, the flexible wall could not be used to give very precise adjustment of local pressures and hence the pressure distributions in the three pressure gradient cases examined are quite arbitrary, no attempt being made to obtain equilibrium pressure distributions. The flexible wall formed the door of the working section and was sealed along the top and bottom with foam rubber strips.

The tunnel side-wall boundary layer approaching the test wall was bled off through a suction slot which extended across the full span. The test wall was inset  $\frac{1}{4}$  in. into the tunnel to assist the removal of the wall boundary layer, which was of the order of  $\frac{1}{4}$  in. thick at this point. A brass insert in the balsawood leading edge had three 0.010 in. diameter tappings as shown in Fig. 1. To ensure the same starting conditions for each boundary layer, the suction rate was adjusted in each experiment so that the pressures indicated by the two extreme tappings were equal. The pressure indicated by the centre tapping was then a maximum and was equal to the tunnel total pressure. The available suction power was sufficient to give this condition up to the maximum tunnel speed used. A pitot-tube traverse, at 2.6 in. downstream from the leading edge, indicated a normal boundary layer with no remnants of shear flow from the upstream boundary layer when the above suction condition applied. Oil flow tests showed that no separation was occurring around the leading edge.

A trip wire 0.023 in. diameter was attached to the solid wall entry length at  $\frac{3}{4}$  in. from the leading edge to give instantaneous transition. A stethoscope attached to a pitot tube was used to check that transition did occur at the wire.

Considerable difficulties were initially encountered because of an unsteadiness in the tunnel speed, with consequent fluctuations in manometer levels, so that the taking of reliable mean readings was very

difficult. At first, the trouble was thought to be due entirely to boundary-layer separation in the tunnel diffuser. Wool tufts on the side wall confirmed that the boundary layer coming off the test wall separated almost immediately on meeting the adverse pressure gradient, particularly at high injection rates. The initial adverse gradient in the diffuser was more severe than that with the usual  $7\frac{1}{2}$  in. wide section in the tunnel, because of the additional divergence at the downstream end of the flexible wall. Vortex generators on the side wall did not give very much improvement. A wall jet, breathing directly from the atmosphere and arranged as shown in Fig. 1, helped to maintain unseparated flow for a much greater distance downstream. It was also found that the fan speed was being affected by fluctuations in the mains voltage and a separate stabilised voltage supply was obtained. Manometer levels still tended to fluctuate but reliable mean readings could now be obtained, the level of the fluctuations finally achieved being about  $\pm 1$  to 2 per cent of the mean reading. Preston<sup>24</sup> who used the same tunnel for some of his measurements, also reported having similar difficulties in obtaining mean readings.

#### 3. Injection Surface.

The injection surface used throughout was of  $\frac{1}{8}$  in. thick 'Vyon' sintered polythene sheet\*, maximum permeability grade. The porous test wall started at 4.9 in. from the leading edge, the porous sheet being attached using 'Holdtite' adhesive to the plywood grid shown in Fig. 2. The line of the grid intersections was slightly inclined to the flow direction, to avoid a build-up of blockage effects which could occur if succeeding joints were aligned with the flow direction. Such a build-up could result in a spanwise variation of boundary-layer properties at downstream positions. A close-up view of the jointing between the grid and the porous sheet is also shown in Fig. 2. The blockage represented by the grid was 8 per cent of the total area and from Fig. 2, it is seen that the blockage due to any fillets of adhesive is negligible. The thickness of the members of the grid was 0.04 in. compared to the porous wall thickness of 0.125 in., so that redistribution of the injected air within the wall would tend to reduce the effect of the discontinuities at the supports.

The advantages of the above material are that it has a substantially lower cost and is available in larger sheets (up to 32 in. x 32 in.) than any of the comparable sintered metal products, so that difficulties with joints did not arise. It is reasonably rigid and the pressure drop required for the flow rates envisaged was within the available capacity of the laboratory blowing system. Microphotographs and 'Talysurf' roughness traces of Vyon are compared with those for 'Porosint B' and 'Poroloy 5 micron rigid mesh' in Fig. 3. It will be seen that Vyon is comparable with Porosint B in roughness and somewhat less so in fineness of grain structure. The stylus on the recorder used to obtain the roughness traces had a 90° included angle conical tip, with a tip radius of 0.005 in.

An improved view of the surface of Vyon over that shown in Fig. 3 is shown in Fig. 4. This photograph was taken on the scanning electron microscope of the Cambridge University Engineering Department and shows the view at an angle of 30 degrees to the surface. The scale quoted is true for the east-west direction, but the view is foreshortened in the north-south direction.

The variation of porosity along the line of the velocity traverses was measured before a sheet was finally placed in position. This was done using the arrangement shown in Fig. 5. The flow rate through a circular area  $1\frac{3}{4}$  in. diameter was measured at intervals along the length, with the pressure differential across the sheet maintained at a constant value. The results for the two sheets used in the experiments are shown in Fig. 6. In the analysis of the velocity profile data, the variations shown in Fig. 6 have not been taken into account. These measurements were made before final assembly to ensure that the porosity of the sheet to be used did not increase (or decrease) monotonically along the length, or exhibit 'excessive' variations. Both of the distributions shown would not give rise to a consistent trend in the departure of the skin friction, obtained from the momentum integral equation, from the true skin friction.

The problem of deciding what is an 'excessive' variation of injection velocity can be approached in various ways. If the variations are exactly reproduced as corresponding ripples on the momentum-growth curve, then this scatter will make the choice of a smooth curve to be used to obtain the gradient somewhat more difficult. However, the calculation of the gradient from a smooth curve through the

\*Manufactured by Porous Plastics Ltd.

momentum growth even for nominally zero pressure-gradient conditions on an impermeable wall is usually no more accurate than  $\pm 3$  to 5 per cent. This is due to the difficulty of choosing a smooth curve through data with scatter arising from (i) errors in the experimental measurements themselves, (ii) pressure gradients due to small ripples on the nominally constant pressure distribution, (iii) possible lack of two-dimensionality and, in this case, (iv) variations of injection rate. The process of then differentiating the final choice of smooth curve is itself inherently inaccurate. A criterion for acceptable variations of injection velocity could then be that their effect would be no greater than any of the other sources of experimental scatter.

In nominally zero pressure-gradient conditions, very small deviations from the mean pressure can give rise to significant pressure gradients whose sign will fluctuate and whose effect will be expected to be similar to the effect of ripples on the injection velocity distribution, at least as far as momentum growth is concerned. A calculation which determines the magnitude of such fluctuations in the pressure-gradient term for a nominally zero pressure-gradient layer would be of some help in trying to assess acceptable limits for injection-velocity variation. This has been done for one of the layers measured in the present series (that at  $v_0/U_1 = 0.0032$ ,  $U_1 = 50$  ft/sec.). The velocity distribution for this layer is shown in Fig. 7. Over the greater part of the layer the velocity is constant within  $\pm 0.2$  per cent of the reference velocity, which is as good as is usually encountered in the literature (*see*, for example, Klebanoff<sup>15</sup> and Dutton<sup>7</sup>). The mean curve shown in Fig. 7 was selected as being a plausible representation and the corresponding velocity-gradient distribution was calculated.

The two-dimensional momentum integral equation is

$$\frac{d\theta}{dx} = \frac{c_f}{2} + \frac{v_0}{U_1} - (H+2)\frac{\theta}{U_1/U_{\rm ref}} \cdot \frac{d(U_1/U_{\rm ref})}{dx}.$$

The quantity

$$A = \frac{-(H+2)\frac{\theta}{U_{1}/U_{\text{ref}}} \cdot \frac{d(U_{1}/U_{\text{ref}})}{dx}}{v_{0}/U_{1}}$$

can therefore be regarded as an 'equivalent  $v_0/U_1$  variation' due to the stray pressure gradients, since it compares the magnitude of their effect on the momentum integral equation with the mean  $v_0/U_1$ . In Fig. 8 we plot (1+A) vers. x to obtain a direct comparison of this equivalent  $v_0/U_1$  variation with the real  $v_0/U_1$  variation in Fig. 6. It is seen that, even with such a very nearly constant velocity distribution, the two quantities are of the same magnitude and of similar wavelength. Hence, unless the velocity distribution can be maintained constant to a much better degree than in this case, it would appear that any attempt to obtain the  $v_0/U_1$  distribution to better than about  $\pm 10$  per cent of the mean would be an unwarranted refinement.

The effect of variations in  $v_0/U_1$  on the detailed velocity profile is, however, more difficult to assess. The outer profile can be taken to be relatively insensitive to what are, in this case, small variations in wall conditions with a wavelength of the order of only a few times the boundary-layer thickness. The results obtained in this series may be used to determine whether the variations in the injection velocity have a significant effect on the velocities near the wall. If the effect on the velocity is measurable, then it might be expected that the ripples on the  $v_0$  distribution would produce corresponding ripples on the  $u/U_1$  vers. x distribution at constant y. This has been checked by comparing the  $u/U_1$  distributions at y = 0.01 in. for four of the layers measured on the first sheet of Vyon with the  $v_0$  distribution for that sheet. The results are shown in Fig. 9. With the possible exception of the range of x from 10 in. to 15 in., any consistent trends are suppressed by the experimental scatter in the velocities.

With the arrangement used here to support the porous wall (shown in Fig. 2) it was not possible to smooth the distribution of injection velocity, as could be done with the arrangement used for suction experiments by Thompson<sup>31</sup>. He subdivided the supporting grid into cells which were completely

isolated from each other and with a backing skin which could be used to adjust the flow into each cell. The variation of porosity along the surface could thus be compensated by varying the resistance of this backing skin. However, the measurement of the flow into each cell to an accuracy rather better than the maximum assigned variation of injection velocity (say  $\pm 5$  per cent of the mean) presents a difficult practical problem. To ensure freedom from inter-cell leakages, the members of the supporting grid would probably have to be thicker than where this is not important. (Thompson used  $\frac{1}{8}$  in. wide supporting strips in  $\frac{1}{2}$  in. wide cells). The blockage would thus be increased locally, the effect of which would be to introduce variations whose magnitude would probably be much greater, and with a smaller wavelength, than those to be overcome. Since it is not possible, *a priori*, to make a rational choice between the two types of variation, it was decided to adopt the simplest approach of accepting the variations as they stood. (It may be noted that the problem of supporting the porous wall when only suction is to be applied is simpler than in the case of injection. Thompson has suggested that a grid of very thin strips of metal or plastic embedded in the porous wall would be a possible method of construction for the case of suction which would circumvent the difficulty noted above.)

### 4. Injection Air Supply.

The injection air supply was obtained in two ways. At the lower injection rates, the pressure differential across the porous wall to give the required injection velocity was less than the static depression below atmospheric pressure in the tunnel working section. Hence, a separate air supply was not needed and the plenum chamber was left open to atmosphere, with a regulating valve at the inlet. For conditions where the above did not apply, a blower was connected to the plenum chamber.

The mean injection velocity was obtained by metering the total flow when supplied and dividing by the total area of the porous surface. In the experiments at the lower tunnel speeds, a streamlined entry on the inlet supply pipe was used to measure the total flow rate. The discharge coefficient of the streamlined entry was taken as unity.

The disadvantage of the above method of metering was that the injected air supply was unfiltered, so that the porous surface, after a period of four months continuous use, was becoming progressively blocked with atmospheric dust. In the experiments at the higher tunnel speed, much larger flow rates were to be used, so that a filter system (also using Vyon) in the supply pipe became essential. The original porous sheet was removed and replaced by a second sheet. The metering was now done using an orifice plate constructed to British Standard 1042, Pt. 1, in the inlet pipe, with 40 diameters of straight piping upstream. The orifice plate was compared with the streamlined entry previously used by placing the entry at the open end of a pipe connected to the laboratory suction system and in which the orifice plate was placed 80 diameters downstream from the entry. The result of the comparison is shown on a percentage basis in Fig. 10. Also shown are the flow rates corresponding to each of the layers for which the streamlined entry was used as the method of measurement. The difference between the two methods is generally less than 2 per cent of the flow rate, with a tendency to increase to 5 per cent at the lowest flow rate. However, B.S. 1042 indicates that the discharge coefficient of the type of orifice plate used increases slowly with reduction of orifice Reynolds number. For the streamlined entry, the tendency would be for the discharge coefficient to fall with reduction of the flow rate, since the proportion of the crosssectional area occupied by the boundary layer will increase. The streamlined entry will tend slightly to overestimate, while the orifice plate will tend slightly to underestimate the flow rate, if the discharge coefficients are assumed constant and equal to the asymptotic values for large Reynolds numbers, as was done here. The error in the measurement of flow rate will therefore be less than the percentage differences shown in Fig. 10. If the difference is made up equally by the streamlined entry and the orifice plate, then the inaccuracy of the flow rate measurement is at worst  $\pm 2\frac{1}{2}$  per cent.

### 5. Measurement of Pressures and Wall Distances.

The pitot tube used for most of the measurements had a flattened mouth with dimensions 0.010 in. overall height, 0.005 in. mouth and 0.09 in. wide. Two other probes (of dimensions 0.016 in. overall height, 0.011 in. mouth, and 0.0066 in. overall height, 0.0028 in. mouth) were used for some profiles in the early

experiments. The Preston tube used had an outside diameter of 0.035 in. The wall static tappings were of 0.04 in. inside diameter, while a static probe 0.042 in. outside diameter constructed in the standard way was used on occasions to check the indications of the wall tappings and to record static-pressure variations through the boundary layer.

The traverse gear used was fitted with a dial gauge which had a total travel of 0.8 in. and was graduated in steps of 0.0005 in. For wall distances greater than 0.8 in., a Vernier scale on the traverse gear was used; this could be read to 0.01 in. The total travel available was 4.5 in.

Several types of liquid displacement manometer were used to measure pressures. Tunnel reference and metering device pressures were measured on tilting single-tube manometers with industrial methylated spirits as fluid. Probe pressures were measured either on this same type of manometer, or on a null reading micromanometer, depending on the pressure range. The dynamic pressure was obtained from the pitot pressure using the static pressure at the adjacent wall tapping as reference pressure. Where a wall tapping did not coincide with a measuring station, the tapping immediately upstream was used to give a reference static pressure and a correction obtained from the static-pressure distribution was applied to obtain the local static pressure. This correction was only important where the pressure gradient was appreciable. Errors, due to density differences, slightly non-linear scales or other extraneous causes, in the readings of tilting manometers used for the measurement of absolute pressures were eliminated by recalibrating a manometer after any change of conditions (e.g. in angle of tilt, or through changes in manometers). This was done using the micromanometer, which was itself checked periodically (for longterm density variation) against a Betz water-filled micromanometer. No variation was noted over the period of the experiments. The effect of variations in ambient pressure and temperature on manometer fluid densities has been assumed to be negligible.

The magnitude of the fluctuations in manometer levels, referred to previously, determined the precision of the probe pressure measurements. The level of the fluctuations was constant at about  $\pm 1$  to 2 per cent of the local reading throughout the thickness of the layer. Manometer readings could, under these conditions, be repeated to  $\pm 1$  per cent on local dynamic pressure, or  $\pm \frac{1}{2}$  per cent on local velocity. At large injection rates and small wall distances, the dynamic pressures were small and the accuracy of a reading was then governed by the accuracy with which the manometer scale could be read, which was about  $\pm 0.02$  cm, for a free stream dynamic pressure of 12 to 15 cm on the same scale. Thus local values of  $u/U_1$  for these conditions would be no more accurate than about  $\pm 1.5$  per cent at  $u/U_1 = 0.2$ , or  $\pm 4$  per cent at  $u/U_1 = 0.1$ .

Since Vyon is non-metallic, an electrical method of locating the wall could not be used directly. Also, since the traverse gear was mounted on the door of the working section, it was impracticable to determine the position of the probe relative to the wall before starting the tunnel. The method adopted was to press the probe against the wall and then traverse away from the wall in steps of 0.001 in. until the reading changed. Up to injection rates  $(v_0/U_1)$  of 0.005, the change of manometer level for 0.001 in. movement of the probe at the wall was greater than the accuracy with which the manometer could be read, so that the method gave a distinct indication repeatable to  $\pm 0.001$  in. In layers with high rates of shear at the wall, the position could be determined, using this method, to  $\pm 0.0005$  in. At high injection rates, the change of probe pressure per 0.001 in. movement at the wall becomes of the same order as the accuracy of reading and the method is thus no longer reliable. For these conditions, the probe position relative to the wall was located by sighting through the transparent tunnel roof. The sighting was almost vertically along the wall and could be repeated to  $\pm 0.002$  in. after some experience. In only two of the layers has complete reliance had to be placed on visual sighting alone (i.e. the layers for  $v_0/U_1 = 0.008$ ,  $U_1 = 50$  ft/sec, and Pressure Distribution II).

The static pressures at the wall tappings were measured on an inclinable multitube manometer which could be read to  $\pm 0.03$  cm in a typical reading of 25 cm. The line of the wall static tappings was offset about 1 in. below the line of the velocity traverses. The static pressure distributions were always measured with the pitot probe and probe holder removed from the tunnel working section. The static-pressure distributions in the zero pressure-gradient layers could be adjusted to give a ripple of generally less than  $\pm 0.5$  per cent of the free stream dynamic pressure about the mean. This was true except at the extreme ends of the injection surface where precise adjustment could not be obtained. In only one of the layers

with uniformly distributed injection was the pressure distribution such that the pressure gradient had to be taken into account. This particular distribution is shown in Fig. 11, together with a distribution representative of the remainder. In the layer with a discontinuous distribution of injection velocity, although the pressure gradient was again nominally zero, the pressure distribution could not be precisely adjusted because of the streamwise variation in conditions and again the pressure gradients present have been taken into account.

### 6. Injection Velocity Distribution for Layers with Pressure Gradient.

The injection rate in each of the three layers with pressure gradient varied in the x-direction. This variation was caused by the streamwise pressure gradient producing a variation of the pressure differential across the porous test wall. In order to obtain the distribution of the local injection velocity, the distribution of the ratio (local pressure differential/overall mean pressure differential) was first obtained from the measured plenum chamber pressure and tunnel working section pressure distribution. From this, the distribution of the ratio (local injection velocity/mean injection velocity), and hence the distribution of the local injection velocity, was obtained by assuming that the injection velocity is directly proportional to the pressure differential, which is very nearly true for Vyon.

#### 7. Experimental Results.

In all, 12 complete boundary-layer developments have been measured along the centreline of the test wall. The details of the layers are summarised in Table 1. The velocity distributions and, for the layers with pressure gradients, the smoothed velocity-gradient distributions are tabulated in Table II. The complete velocity-profile data are tabulated in Table III. The profiles are identified by the distance in inches from the leading edge; the distance from the start of injection is that shown less 4.9 in. The x-coordinates of the measuring stations are the same for all the layers with the exception of Pressure Distribution III. In that case, a blister was attached to the flexible wall to produce the large favourable pressure gradient and this necessitated a slight alteration in some of the x-co-ordinates for this layer. For the layer with a discontinuity in the injection rate, additional velocity profiles have been measured at intermediate positions in the vicinity of the discontinuity.

All the calculations involved have been carried out on the EDSAC 2 and TITAN Computers of the University Mathematical Laboratory. The integrations for displacement and momentum thicknesses were performed using the trapezium rule. The tables in Table III are reproductions of the printed computer output and the form of identification of the usual parameters is due to restrictions on the line printer; the parameters are explained in the Notation. The linear dimensions (x and y) occurring in the Tables are in inches. Some of the calculated parameters have been printed to a greater number of significant figures than the precision of the data justifies. The small variation in the calculated values of  $v_0/U_1$  in each of the zero pressure-gradient layers is due to the variation of  $U_1$ , an overall mean value of  $v_0$  having been taken in each case. All the tabulated data are as measured and have not been corrected for the effects of either pitot-probe displacement, turbulent fluctuations, or static-pressure variation normal to the wall.

It should be mentioned that, since injection started at x = 4.9 in., the first few velocity profiles in each boundary layer may not be fully adjusted to the injection state and thus these velocity profiles would not be suitable for testing theories based on fully developed conditions. Little is known about the length of the region of adjustment to this state. In addition, the Reynolds numbers at the initial stations are small in some cases. As a general rule, only the measurements for  $x \ge 11.5$  in. and/or  $R_{\theta} > 1000$  have been used in comparisons with theoretical predictions. All the data measured at x = 5.6 in. and 8.3 in. are, however, included for the sake of completeness.

In the experiments no attempt was made to maintain the reference Reynolds number constant in the face of day-to-day variations in ambient temperature and pressure since these did not vary sufficiently to warrant this. (The reference pressure was, of course, kept constant). The Reynolds numbers and free-stream velocities are therefore subject to a small random drift about the mean and have not been used to obtain velocity gradients; for this purpose the velocity distributions obtained from the 'frozen'

static-pressure distributions have been used. These velocity distributions are those given in Table II.

After the completion of the main experiments, several velocity profiles were measured using an electrical method to locate the pitot probe relative to the wall in order to confirm the accuracy of the wall distance measurements described in Section 5. The method used was somewhat troublesome and could not be conveniently adopted for each measuring station and velocity profile. These additional measurements were therefore made at one measuring station only. The wall position was located using a ground gauge block manipulated through the tunnel roof. The block was positioned between the probe and the wall and contact between the probe and the block was detected electrically. The wall position thus determined could be repeated to 0.0005 in. These additional results covered a range of  $v_0/U_1$  from 0.003 up to 0.0145 at free stream velocities of 30 and 50 ft/sec, with the profile at x = 31 in. only being measured; these results are included in Table III. All the profiles measured in this way behaved in a precisely similar manner to those of the main experiments when compared to the available theories. They thus confirmed the general accuracy of the wall distances measured in the main experiments.

For all the boundary-layer developments, the experimental distributions of momentum thickness have been used to obtain the distributions of the local skin-friction coefficient using the two-dimensional momentum integral equation. Before presenting these results it is first necessary to examine the magnitude of the more significant effects which can contribute to errors in this quantity, in order that an approximate assessment of the reliability of the skin-friction results can be made. This is done in the following sections.

### 8. Two-dimensionality of Boundary Layers.

In a recent review, Thompson<sup>30</sup> has pointed out that most of the boundary layers for which data had been published up to that time were almost certainly not two-dimensional to a greater or lesser extent. Discrepancies between the predictions of the two-dimensional momentum integral equation and experiment were often very large and he suggested that the most reasonable explanation for the observed discrepancies was the lack of two-dimensionality of the layers. This was most probably caused by the effect of the adverse pressure gradients on the tunnel side wall boundary layers, causing them to grow rapidly and produce a convergence of the main flow. In the present experiments, the tunnel floor and roof boundary layers should be thin and relatively unaffected by the injection through the test wall, or the pressure gradients envisaged. In addition, the aspect ratio of the tunnel was reasonably large (about 4 to 1), so that the above effects should not be very important. Nevertheless, it was important to ensure that such three-dimensional effects were negligible, since the two-dimensional momentum integral equation integral equation was the only method to be used to obtain the skin friction.

The method\* used was to attach two cylindrical rods to the test wall near the leading edge and to obtain total pressure traverses across the wakes of the rods at various distances downstream. Any gross convergence or divergence of the flow should manifest itself on the separation of the wake centrelines. The rods were 2 in long by  $\frac{1}{8}$  in diameter and either 3 in. or 6 in. apart. They were attached near the mid-span at 4 in. from the leading edge. Total pressure traverses were taken at 12 in. and 28 in. downstream of the rods, both at 1 in. from the wall. The test was done for  $v_0/U_1 = 0$  and  $v_0/U_1 = 0.008$  at  $U_1 = 50$  ft/sec, both with constant pressure and also for the conditions of Pressure Distribution III. A representative result\*\* is shown in Fig. 12.

For a radially convergent or divergent boundary layer, the momentum integral equation can be written as (Bradshaw and Ferriss<sup>3</sup>),

$$\frac{d\theta}{dx} - \frac{\theta}{x_0 - x} = \frac{\tau_0}{\rho U_1^2} + \frac{v_0}{U_1} - (H + 2)\frac{\theta}{U_1}\frac{dU_1}{dx},$$

where  $x_0$  is the position of the virtual origin of the convergence or divergence. If the cylinder spacing is

<sup>\*</sup>suggested by Dr. M. R. Head.

<sup>\*\*</sup>the particular shapes of the wake profiles in Fig. 12 is due to the trailing vortices shed on either side of a cylinder immersed in a shear flow. The rotational sense of these vortices is such as to thin the boundary layer in the x-y plane of the cylinder centreline.

h, the wake centreline spacing at the measuring position is  $h + \Delta h$  and the distance from the cylinders to the measuring position is  $x_1$ , then

and

$$x_0 - x = \frac{h + \Delta h}{\Delta h} \cdot x_1 ,$$
$$\alpha = \frac{h + \Delta h}{2(x_0 - x)},$$

where  $\alpha$  is the angle of convergence to, or divergence from, the x-direction at  $z = (h + \Delta h)/2$ .

With the present method of measurement, the minimum  $\Delta h$  which can be measured is about 0.025 in. which, with  $x_1 = 28$  in. at the rearmost measuring position and h = 6 in., corresponds to a value for  $x_0$  of 560 ft. This corresponds to a minimum value of  $\alpha$  which can be measured of 0.03°, which is better than that obtainable using a yawmeter probe. The above is based on the assumptions that the streamlines are straight lines radiating from the virtual origin and that the tunnel centreline lies in the plane of symmetry of this radial flow.

The additional term in the momentum integral equation has been calculated for the three conditions for which measurements were made and the results are shown in Table IV, together with the resultant error in  $d\theta/dx$ . In many of the measurements, the wake centreline spacing equalled the cylinder spacing within the accuracy with which the former could be measured. For these measurements, the limits of accuracy ( $\pm 0.025$  in.) were therefore used for  $\Delta h$  to obtain the possible error in  $d\theta/dx$ . In all cases, the possible error in  $d\theta/dx$  was small so that remedial measures were not warranted.

#### 9. Aerodynamic Smoothness of Test Surface.

### 9.1. Experiments without Injection.

One of the principal purposes of the experiments which were carried out with zero injection and zero pressure gradient was to determine whether the porous surface behaved as an aerodynamically smooth surface. The experiments were conducted at both the free stream velocities used in the injection experiments. Although the mean injection rate was accurately zero, the presence of ripples on the static pressure distribution would give rise to alternating suction and injection along the surface. The maximum rates of suction or injection in the two layers was of the order of  $5 \times 10^{-5}$  which is small in comparison with the skin-friction coefficient.

From the roughness trace shown in Fig. 3, the mean roughness height is about 0.001 in. With a representative value of  $c_f$  of 0.004, the value of  $U_t k/v$ , where k is the roughness height, is about 1.2 for the lower and about 3.5 for the higher unit Reynolds number used. The surface would therefore be expected to be aerodynamically smooth by the usual criterion\* of  $U_t k/v < 5$ . This conclusion can be independently confirmed by determining whether the zero injection velocity profiles agree with the semi-logarithmic inner law for smooth impermeable walls, i.e.

$$u/U_{\tau} = A \log_{10} \frac{U_{\tau}y}{y} + B.$$

The values of  $c_f$  required to give a 'best fit' of the experimental profiles to this law were obtained by plotting the profiles on 'Clauser' plots (Clauser<sup>4</sup>), some examples of which are shown in Fig. 13. The values accepted for the constants in the law are those recently recommended by Patel<sup>23</sup> i.e. A = 5.5, B = 5.45. The values of  $c_f$  from Preston tube readings were evaluated using Patel's calibration curve. There was a tendency for these latter values of  $c_f$  to be consistently smaller than those obtained from the

<sup>\*</sup>Strictly, this criterion applies when the 'equivalent sand grain' roughness of the surface is used. But since the present surface is composed of sintered particles, this latter and the measured roughness should not differ greatly.

The relation for  $U_1 y_a/v$  has been evaluated and is shown in Fig. 17. The injection experiments were conducted at two constant values of unit Reynolds number, and if the roughness height is again taken to be 0.001 in., then the two roughness Reynolds numbers,  $U_1 k/v$ , are 25 and 75. These two values are also shown on Fig. 17. If the ordinate  $U_1 y_a/v$  obtained at a given  $c_f$  and  $v_0/U_1$  is greater than  $U_1 k/v$ , then the roughness height is less than the sublayer thickness and the surface is smooth. The range of values of  $c_f$  obtained for each injection rate in the present experiments are shown on Fig. 17 and it is seen that in all cases the surface is smooth. (The  $c_f$  values used in Fig. 17 are those obtained from the momentum integral equation; see Section 12).

From Fig. 17, it is seen that the sublayer thickness Reynolds number,  $U_1y_a/v$ , decreases slowly with increase of injection rate, while it is found experimentally that  $c_f$  will decrease rather rapidly with increasing injection rate. Hence the general conclusion can be drawn that if the surface is aerodynamically smooth without injection, it will remain smooth with injection at the same value of unit Reynolds number.

### 10. Spanwise Variation of Boundary-Layer Properties.

Spanwise variations of boundary-layer properties in nominally two-dimensional conditions have been described by Head and Rechenberg<sup>10</sup>, Fernholz<sup>9</sup> and Bradshaw<sup>2</sup>. They ascribed the variations to the screens in the tunnel settling chamber or to non-uniform transition. In the suction type of open-circuit tunnel used for the present measurements, there were no screens in the tunnel contraction, only a honeycomb at the entry being used. The growth of a new boundary layer on the test wall independent of the boundary layer in the contraction, together with the forced transition should ensure that both of the above effects would be minimised in the present experiments. The pitot pressure at the surface, which provides some indication of the constancy of conditions across the span, was measured near the trailing edge and is shown in Fig. 18. The maximum variation was -6.5 per cent of the mean, while for one boundary-layer thickness (a mean value of which is about 0.75 in. at this position) on either side of the line of the velocity traverses, the variation is less than  $\pm 2$  per cent of the mean.

It is interesting to note that the peak in pitot pressure at about 9.5 in. corresponds approximately with the line of the wall static tappings. This effect is most probably due to the local blockage of the injection mass flow at each static tapping resulting in the boundary layer along the line of static tappings having a different behaviour to that away from this line. The peak in pitot-pressure results in a peak in dynamic pressure (if the static pressure is constant) consistent with a boundary layer developing along the line of static tappings under the influence of a locally reduced injection rate. This result provides *a posteriori* justification for the inclination of the supportinggrid to the flow direction mentioned in Section 3.

### 11. Variation of Static Pressure through the Boundary Layer.

Newman<sup>22</sup> has suggested that static-pressure variation through the boundary layer may give rise to a significant term in the momentum integral equation under severe adverse pressure-gradient conditions. He showed that the additional term which must be included in the momentum integral equation is

$$B = -\frac{\partial}{\partial x} \left[ \frac{2}{\rho U_1^2} \int_0^\delta (p-p_1) \, dy \right],$$

where  $p_1$  is the static pressure at the edge of the layer and p the static pressure at height y.

Such a variation of static pressure may also occur in zero pressure gradient layers with suction or injection if the acceleration term  $\frac{\partial v}{\partial x}$  is significant, as can be seen from the y-momentum equation,

$$u\frac{\partial v}{\partial x} + v\frac{\partial v}{\partial y} = \frac{1}{\rho}\frac{\partial p}{\partial y} + \frac{1}{\rho}\frac{\partial \tau}{\partial x} + \frac{normal}{stress}$$
terms.

Even if the effect of the normal stresses is negligible, the static-pressure gradient could still be significant

because of the term  $u \frac{\partial v}{\partial x}$ . The severest possible condition was chosen to determine experimentally whether such gradients were appreciable. Measurements were made in a layer with a sudden discontinuity in the injection velocity distribution, the injection rate  $v_0/U_1$  changing from about 0.003 to very nearly zero at x = 17.5 in. Static-pressure profiles were measured both upstream and downstream of the discontinuity and the integral in the expression for *B* evaluated. The variation of the integral with x is shown in Fig. 19. While local gradients are appreciable, the overall contribution to momentumthickness growth for any choice of smooth curve through the scattered data would be negligible. The considerable scatter in Fig. 19 represents a quite small error in the measurement of static pressure.

A typical static-pressure profile is shown in Fig. 20. The maximum deviation from the wall static pressure  $p_0$  is only about -0.35 per cent of the free-stream dynamic pressure. The profile shown was measured at 3 in. (about 8 boundary-layer thicknesses) upstream of the discontinuity. All the profiles measured are of the same shape and with variations of much the same magnitude as that shown. Thus, even though the condition which could give rise to a static-pressure variation was much more severe than would be encountered normally, the measured variations were found to be very small, and their effects are consequently neglected.\*

The static-pressure profiles measured in this test were also used to determine the magnitude of the error in local velocity  $u/U_1$  arising from assuming that the static pressure is constant and equal to the wall static pressure  $p_0$  throughout the layer, as was done in all the velocity-profile measurements. The effect is shown in Fig. 20 as the resultant percentage error in local  $u/U_1$  for the velocity profile 3 in. upstream of the discontinuity. This error is generally within the likely error in the actual measurement of  $u/U_1$  and is consequently neglected.

The static pressures indicated by the probe resting on the wall and in the free stream are compared with those indicated by the wall tappings in Fig. 21, for both parts of the layer. The agreement between the three pressures is generally better than 0.2 per cent of the reference pressure. It might be possible that neither a static probe resting on the wall nor a wall static tapping would indicate the correct static pressure when injection is taking place. However, the close correspondence between these two pressures and that measured at the edge of the boundary layer (for that part of the layer with injection) suggest that both do indicate the true static pressure.

It is concluded that the method of measuring velocity profiles, taking the static pressure to be constant and equal to that indicated by the adjacent wall tapping, is likely to result in negligible errors in the mean velocity profiles.

### 12. Skin-Friction Coefficients.

Using the two-dimensional momentum integral equation i.e.

$$\frac{c_f}{2} = \frac{d\theta}{dx} - \frac{v_0}{U_1} + (H+2)\frac{\theta}{U_1/U_{\rm ref}} \cdot \frac{d(U_1/U_{\rm ref})}{dx}$$

the distributions of  $c_f/2$  have been calculated for each of the boundary layers and are tabulated in Table V. Only the values for the measuring stations after x = 11.5 in. are quoted.

The gradient term,  $d\theta/dx$ , was determined from fitting the curves of  $\theta$  vers. x by hand. This determination is based on a purely subjective assessment of the 'best' curve to be fitted to the experimental data. The resultant gradients are sensitive to this choice of curve, and from experience it is reasonable, even with quite well-defined curves, to expect differences of at least 4 per cent of  $d\theta/dx$  from different operators using the same techniques on the same data. Differences of the same order are also easily obtainable from numerically fitting different types of analytical curve (for example, polynomials of different order).

<sup>\*</sup>These static-pressure measurements were made with a standard type of 4-hole ellipsoidal nose static tube. Hinze<sup>11</sup> states that such a tube is unlikely to indicate the correct static pressure in a turbulent flow and that no systematic investigation has been made which would give the magnitude of the effect of turbulence on the tube reading. He suggests, however, that such tubes are likely to read too low a pressure.

Additional errors in  $d\theta/dx$  will arise due to lack of two-dimensionality and inaccurate measurement of the injection rate.

It is not possible to quote a meaningful overall estimate of the accuracy of the skin friction results given in Table V. Rather, the value of 4 per cent of  $d\theta/dx$  is given in each case, since it is the precision of the determination of this quantity which will determine the precision of  $c_f/2$ . This estimate of the precision is accepted as reasonable (if not optimistic) in view of the possible errors mentioned above.

For the layers with pressure gradient where  $d\theta/dx$  varied significantly along the layer, an average value has been accepted in obtaining this estimate. The estimate in these cases should be accepted with caution since, in addition to the previously mentioned effects, the local value of  $c_f$  is now dependent also on the accuracy of determination of the local pressure gradient and considerable fluctuations about the mean value of  $c_f$  will occur. This is most clearly seen in Pressure Distribution II, where, because of the large injection rate, the  $c_f$  would be expected to be small. The quoted values of  $c_f/2$  are seen to fluctuate between -0005 and +0013 and the quoted estimate of the accuracy has little meaning. However, the overall

# average value of the skin-friction coefficient (i.e. $\frac{1}{L} \int_{0}^{L} c_{f} dx$ , where L is the chord) is small in agreement

with expectation.

In view of the considerable errors in the values of  $c_f$ , the direct use of these for testing any new velocityprofile law is not recommended. The better procedure in such cases is to determine the  $c_f$  from the velocity profiles (using an analogue of the Clauser plot based on the new law) and then to calculate the development of  $\theta$  with x using this  $c_f$ . This is the method which has been used in the analysis of the present data (McQuaid<sup>19</sup>).

# 13. Experiment on a Boundary Layer with a Discontinuity in the Injection Velocity Distribution.

For simplicity, the experimental arrangement which had been used for the previous measurements was now only slightly modified to allow for this experiment. The plenum chamber (shown in Fig. 1) was now divided by a partition, so that the injection mass flow was confined to the front part of the test wall. The boundary layer with injection was continued to x = 17.5 in. and thereafter, the injection velocity was intended to be zero. The arrangement did, however, have a number of disadvantages which gave rise to several difficulties in the measurements.

Firstly, in order to obtain a precise position for the end of injection, a  $\frac{1}{2}$  in. wide 'Sellotape' strip was attached to the wall, giving x = 17.5 in. as the end of the injection surface. The thickness of the strip was 0.0015 in. and it should therefore affect the velocity profile only very close to the wall. That this was the case is seen from Fig. 22 where velocity profiles measured immediately upstream and immediately downstream of the trailing edge of the strip are compared. For wall distances greater than about 0.01 in., no effect is discernible. The strip was nevertheless at the position where extraneous influences should be excluded and the proper arrangement would have been to have a true solid surface following the porous surface. (It was not convenient to mask the whole surface over the zero injection part, since then the wall static-pressure tappings would not be available, making adjustment of the pressure gradient very difficult.)

Secondly, complete sealing of the partition in the plenum chamber was not achieved, due principally to the difficult joint between the partition and the grid supporting the porous wall. Even a small residual injection velocity over the nominally zero injection part of the surface has an effect which is significant compared to the skin-friction coefficient. This effect cannot accurately be taken into account, since the leakage flow rate cannot be measured directly.

Initially, a complete boundary-layer development was measured, with the injection rate nominally changing from 0.0032 to zero. It appeared, however, that the injection rate over the nominally zero injection part of the layer was of the order of 0.0004. Elaborate precautions could not reduce this residual injection rate to less than about 0.0001 to 0.0002, as indicated approximately by the pressure differential across the porous wall. This uncertainty of 0.0001 in the injection rate gives rise to an average uncertainty of 10 per cent in the skin-friction coefficient. The measurements were repeated with an injection rate of 0.0034 and this reduced leakage flow and it is this layer which is discussed here and tabulated in Table

III\*. The injection rate over the latter part of the layer is there given as 0.0001, but this figure could be in error by 100 per cent. Two of the velocity profiles were measured on the Sellotape strip mentioned above, so that the injection velocity was zero, these profiles being at x = 17.6 in. and x = 17.85 in.

Thirdly, the velocity distribution along the test wall could not be adjusted to a constant value to the same precision as in the main experiments. The experimental velocity distribution is shown in Fig. 23, together with the mean curve accepted. Although the velocity was constant to within  $\pm 0.5$  per cent of the mean over the greater part of the test wall, the gradients present were sustained over significant portions of the layer and must therefore be taken into account. The gradients cannot, however, be accurately obtained and the mean curve used considerably smooths the measurements, the sharp peak at the discontinuity being completely ignored.

The combination of these two uncertainties (residual injection rate and pressure gradient) rendered the determination of  $c_f$  from the measured growth of  $\theta$  very inaccurate. The values of  $c_f$  over the latter part of the layer given in Table V are probably no more accurate than about  $\pm 15$  to 20 per cent and are thus of little use from the point of view of testing velocity profile laws in these nominally zero pressure gradient, solid surface conditions. This experiment can therefore be regarded as no more than preliminary in nature. However, detailed velocity profiles at closely spaced intervals after the discontinuity have been measured and they can be used to describe qualitatively the progress of the layer from one fully developed condition to the other.

#### 14. Conclusions.

(i) Calculations using the present measurements have shown that variations in the injection rate of  $\pm 10$  per cent of the mean have an effect on the general scatter on the momentum-thickness development no greater than that due to variations in the velocity distribution of a magnitude of  $\pm 0.2$  per cent of the mean and a wavelength of a few boundary-layer thicknesses. The variations in injection rate of about  $\pm 10$  per cent of the mean in the present experiments did not produce discernible effects on the velocity near the surface.

(ii) It has been shown that the local blockage of injection mass flow produced by wall static tappings have a measurable effect on the surface pitot pressure distribution across the span. It is therefore recommended that velocity profiles should be measured away from the line of wall static tappings and that the method of surface support should be such that succeeding joints or supporting members are not aligned with the flow direction.

(iii) Measurements have shown that static-pressure variations through the boundary layer with injection are small and do not introduce significant errors either in the momentum integral equation or in velocity profiles obtained using the static pressure at the wall tapping as reference.

(iv) In any programme of experiments with injection, it is recommended that measurements should be made without injection on the same surface in the same experimental conditions. These measurements will then provide a means of checking whether the surface is aerodynamically smooth. It has been shown that a surface which is aerodynamically smooth without injection will remain so with injection. Experiments without injection also serve to determine the value of the Karman constant,  $\kappa$ , to be used in any mixing length treatment for the inner part of the velocity profile with injection.

Finally, it can be mentioned that the measurements have proved sufficiently consistent and reliable to allow the difference between the theories of Black and Sarnecki, and Stevenson mentioned in Section 1 to be resolved and this is described in Ref. 19. The measurements have also been used to verify the intermittency hypothesis of Sarnecki<sup>25</sup> for injection and a skin-friction law in terms of H,  $R_{\theta}$  and  $v_0/U_1$  has been obtained<sup>20</sup>.

#### 15. Acknowledgements.

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<sup>\*</sup>The static pressure profiles discussed in Section 11 were, however, measured with the first boundary layer. They were not repeated for the second boundary layer, since the original measurements had shown that the effects of static-pressure variation normal to the wall were not important.

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# NOTATION

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A,B	Constants in the semi-logarithmic inner law for solid surfaces ( $A = \frac{1}{\kappa} \log_e 10$ )
C <sub>f</sub>	Local value of the skin friction coefficient $\left( = \frac{\tau_0}{\frac{1}{2}\rho U_1^2} \right)$
Н	Profile shape-factor $=\frac{\delta^*}{\theta}$
р	Static pressure
Р	Pitot pressure
$R_{ heta}$	Reynolds number based on momentum thickness $=\frac{U_1\theta}{v}$
u,v,w	Components of velocity in the boundary layer in the $x$ , $y$ and $z$ directions respectively
$U_1$	Free-stream velocity
$\frac{U_1}{v}$	Local free-stream Reynolds number per unit length
$U_{ m ref}$	Value of $U_1$ at reference position
${U}_{ au}$	Wall shear velocity $\left( = \left(\frac{\tau_0}{\rho}\right)^{\frac{1}{2}} \right)$
$v_0$	Transpiration velocity at the wall (positive for injection)
<i>x</i> , <i>y</i> , <i>z</i>	Space co-ordinates along, normal to, and across the surface
$x_0$	Distance from the origin of the local effective radial flow
$\delta^*$	Displacement thickness = $\int_0^\infty (1 - \frac{u}{U_1}) dy$
heta	Momentum-loss thickness = $\int_0^\infty (1 - \frac{u}{U_1}) \frac{u}{U_1} dy$
к	Mixing-length constant
λ	Parameter in the bilogarithmic law of Black and Sarnecki <sup>1</sup>
v	Kinematic viscosity
ρ	Fluid density
$\tau_0$	Wall shear stress
Further ident	ification of parameters in Table III
L.E.	Leading Edge

U-ONE	$U_1$
RE NUMBER PER INCH	$U_1/v$
INJECTION RATE	$v_0/U_1$

.

# NOTATION—continued

DELTA STAR	$\delta^*$
THETA	θ
RE-THETA	$R_{ heta}$
U/U <sub>1</sub>	$u/U_1$

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### TABLE I

### Summarised Details of Measurements.

Pressure Gradient	Nominal $U_1$ ft/sec	Nominal $v_0/U_1$		
	50	0		
	50	•0017		
	50	•0032		
Nominally Zero	50	•0046		
	50	-008		
	150	0		
	150	•0032		
	150	·008		
Adverse; Pressure Distribution I	55 to 47	·002		
Favourable; Pressure Distribution II	44 to 55	·008		
Favourable; Pressure Distribution III	60 to 112	·0027 to ·007		
Nominally Zero	150	Discontinuous: $x < 17.5'', v_0/U_1 = .0034,$ $x > 17.5'', v_0/U_1 = 0$		

In addition to the above complete boundary layers, measurements were also made of single velocity profiles at x = 31.0 in. for  $U_1 = 30$  and 50 ft/sec and  $v_0/U_1$  from 0.003 to 0.015 in zero pressure gradient.

### TABLE II

x Inches from Leading	$U_1/U_{ref}$ Distributions for First Series											
Edge	(i)	(ii)	(iii)	(iv)	(v)	(vi)	(vii)	(viii)				
5.56	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000				
6.75	1.013	1.009	1.011	1.013	1.013	1.016	1.020	1.021				
8·13	1.012	1.009	1.011	1.014	1.014	1.019	1.023	1.030				
9∙50	1.010	1.006	1.011	1.016	1.016	1.023	1.025	1.044				
10.81	1.007	1.004	1.010	1.016	1.015	1.024	1.026	1.054				
12.06	1.010	1.006	1.010	1.016	1.015	1.025	1.023	1.067				
13.38	1.012	1.008	1.011	1.016	1.015	1.025	1.018	1.076				
14.63	1.016	1.013	1.014	1.020	1.018	1.025	1.012	1.090				
15.88	1.014	1.008	1.012	1.018	1.016	1.025	1.000	1.101				
17.25	1.015	1.011	1.013	1.018	1.017	1.024	.991	1.113				
18.56	1.014	1.010	1.011	1.016	1.015	1.023	-980	1.124				
19.88	1.013	1.009	1.011	1.016	1.017	1.025	.968	1.139				
21.31	1.014	1.009	1.011	1.016	1.014	1:024	.956	1.150				
22.50	1.015	1.010	1.011	1.017	1.017	1.025	.949	1.163				
24.00	1.016	1.009	1.011	1.017	1.017	1.025	.942	1.176				
25.13	1.018	1.011	1.012	1.018	1.018	1.025	.934	1.188				
26.69	1.018	1.013	1.011	1.016	1.019	1.024	.925	1.199				
27.69	1.015	1.005	1.009	1.016	1.018	1.025	.916	1.206				
28.81	1.018	1.008	1.012	1.018	1 019	1.026	·911	1.212				
30.38	1.015	1.006	1.010	1.016	1.019	1.025	904	1.221				
31.63	1.016	1.009	1.010	1.018	1.020	1.025	-904	1.228				
32.94	1.017	1.006	1.012	1.020	1.024	1.029	·896	1.232				
34.19	1.011	1.003	1.006	1.017	1.022	1.028	·888	1.228				

## Velocity and Velocity Gradient Distributions.

(i)  $U_1 = 50, V_0/U_1 = 0;$ 

(ii) 
$$U_1 = 150, V_0/U_1 = 0;$$

- (iii)  $U_1 = 50, V_0/U_1 = 0.0017;$
- (iv)  $U_1 = 50, V_0/U_1 = 0.0032;$
- (v)  $U_1 = 50, V_0/U_1 = 0.0046;$
- (vi)  $U_1 = 50, V_0/U_1 = 0.008;$
- (vii) Pressure Distribution I;
- (viii) Pressure Distribution II.

x Inches	$U_1/U_{\rm ref}$	Distributio	ns for Secon	d Series
Tooding	-		ľ	
Edgo	(i)	<b>6</b> 0	(;;;)	(in)
Euge	(1)	(11)	(111)	(17)
5.43	1.000	1.000	1.000	1.000
6.73	1.007	1.011	1.005	1.009
8.13	1.013	1.021	1.011	1.016
9.58	1.013	1.025	1.013	1.015
11.04	1.011	1.026	1.013	1.014
11.95	1.012	1.028	1.016	1.016
13.37	1.013	1.029	1.029	1.019
14.69	1.014	1.030	1.045	1.022
16.01	1.014	1.032	1.063	1.024
17.35	1.014	1.034	1.091	1.030
18.65	1.013	1.035	1.120	1.022
19.45	1.011	1.034	1.137	1.020
20.41	1.011	1.032	1.149	1.017
21.25	1.011	1.032	1.196	1.017
21.93	1.010	1.031	1.213	1.017
22.53	1.010	1.031	1.238	1.017
23.23	1.011	1.030	1.266	1.018
24.08	1.011	1.031	1.306	1.019
24.73	1.013	1.032	1.343	1.020
25.43	1.013	1.032	1.375	1.019
25.88	1.013	1.032	1.401	1.018
26.78	1.013	1.031	1.452	1.019
27.43	1.013	1.032	1.489	1.018
28.23	1.011	1.032	1.529	1.016
28.63	1.011	1.033	1.564	1.015
29.58	1.012	1.033	1.637	1.018
30.18	1.011	1.032	1.674	1.014
31.03	1.011	1.032	1.732	1.015
31.43	1.014	1.032	1.764	1.017
32.53	1.011	1.034	1.818	1.017
33-28	1.007	1.034	1.827	1.007
34.13	1.007	1.035	1.839	1.004
1	1	1	1	1

## Velocity and Velocity Gradient Distributions.

(i)  $U_1 = 150, V_0/U_1 = 0.0032;$ 

(ii)  $U_1 = 150, V_0/U_1 = 0.008;$ 

(iii) Pressure Distribution III;

(iv) Discontinuity in  $V_0$ .

### TABLE II-concluded

x Inches from Leading	Smoothed Distributions of $d(U_1/U_{ref})/dx$										
Edge	(i)	(ii)	(iii)	(iv)	(v)						
10	0	0	+.0104	+.0025	+.0003						
11	0	0015	+.0101	+.0042	+.0007						
12	0	0036	+ 0097	+.0063	+.0011						
13	0	0050	+ 0093	+.0090	+.0016						
14	0		+ •0090	+.0123	+.0021						
15	0	- 0069	+ .0088	+.0153	+0018						
16	0	0076	+ 0086	+ 0182	+.0010						
17	0	0082	+ 0087	+.0210	0						
18	0 .	• 0086	+ .0089	+.0240	- 0016						
19	0	0089	+.0092	+.0265	- 0025						
20	0	- 0086	+ 0096	+.0297	0020						
21	0	•0076	+ 0099	+.0333	- 0012						
22	+.0004		+.0101	+.0373							
23	+.0004	<i>−</i> ·0058	+.0101	+.0418	+ .0011						
24	+ .0004	• 0055	+.0098	+ 0467	+.0014						
25	+.0004	•0059	+.0091	+.0515	+.0005						
26	+.0004	0062	+.0082	+.0560	0006						
27	+.0004	• 0063	+ 0068	+.0602							
28	+.0004	- 0059	+.0060	+.0647							
29	+.0004	<i>−</i> ·0053	+.0056	+.0700							
30	+ 0004	0044	+.0055	+.0730							
31	+.0005		+.0055	+.0710							
32	+.0006	- 0029	+.0055	+.0440							
33	+ .0007	•0026	0005	+.0220	- 0020						
34	+ .0008	0023	0037	+.0065	0020						

### Velocity and Velocity Gradient Distributions.

(i)  $U_1 = 50$ ,  $V_0/U_1 = 0.0046$  (Nominally zero pressure gradient);

- (ii) Pressure Distribution I;
- (iii) Pressure Distribution II;
- (iv) Pressure Distribution III;
- (v) Discontinuity in  $V_0$  (Nominally zero pressure gradient).

Note: Velocity gradients are per inch.

# TABLE III

Velocity Profile Data for Layer with  $\frac{V_0}{U_1} = 0$ ,  $U_1 = 50$  ft/sec, Zero Pressure Gradient.

X IN	CHES	3 PROM	L.E.	5.6		8.3	1	1.5	14.	5	17.4		21.5	25.	.0	28.4		31.0	34	.2
U-ONE (FT./SEC.)		51.	14	5 <b>0.</b> 96		51.68		.54	51.6	7	51.77	51	1.32	51.2	29	51 <b>.0</b> 9	5	1.14		
re n	UMBE	er per	INCH	26480		26434	2	26109		26035		26067		26466		26453		26496	26	397
INJE	CTI	DH RA	TE	o		0		0	0		o		0	c	0	o		o		0
delt	'A 91	PAR (IN	Ches)	.025	ю	.0331		<b>0</b> 438	.05	02	.0594		.0694	.0	775	.0873	\$	.0924	. 1	<b>0</b> 36
THEI	A(II	CHES)		.015	9	.0218	•	0295	.03	41	.0410	1	<b>.0</b> 484	.05	544	.0615	;	.0649		734
Ħ				1.57	1	1.515	1	. 484	1.4	69	1.450	I	1.433	1.4	425	1.421	I	1.423	1.	412
re-1	HET/	A		Ļع	1	577		770	8	89	1069	,	1264	11	440	1626	<b>.</b>	1720	1	937
		- /		• •																
х 	•	5.0	X =	8.3	X =	11.5	X =	14.5	Χ =	17.4	X =	21.5	X =	25.0	X =	28.4	Х =	31.0	X = (	34.2
Y		0/01	Y	U/01	Y	U/U1	Y	U/UI	Y	บ/บา	Y	U/UI	Y	ប/បា	Y	U/UI	Y	ប/បា	Y	<b>U/UI</b>
.00	)8 No	.517	.008	.470	.008	.429	.008	.412	.008	• 399	.008	391	.008	.380	.008	.375	.008	• 373	.005	.295
.01	10	.558	.009	.508	.010	.440	.009	424	.009	. 404	.009	.400	.009	. 390	.009	. 300	.009	-378	.005	.308
.01	ii .	. 582	.011	.536	.011	.501	.011	.469	.011	.459	.011	.447	.011	434	.011	424	.011	.407	.008	.338
.01	12 .	. 605	.012	.562	.013	. 550	.012	. 493	.012	.478	.012	.469	.012	. 460	.012	. 447	.012	421	.009	.363
.01	13 .	.628	.013	.585	.015	.587	.013	.518	.013	.502	.013	.488	.013	.483	.013	.466	.013	.440	.010	.390
.0	4.	.040	.014	.608	.017	.609	.014	.538	.014	.522	.014	.503	.014	.505	.014	. 485	.014	.461	.011	. 414
.0	16	675	.015	.027	.019	.030	.010	•714	.015	-540	.015	• > 39	.015	.522	.015	.503	.015	.482	.012	•436
.0	17	.685	.017	.652	.029	.683	.020	.622	.018	.584	.019	.585	.017	• 733 - 547	.019	- 231	.017	•490 516	.013	. 470 h70
.0	8	. 695	.018	. 661	.034	. 696	.022	.633	.020	. 604	.025	.616	.019	568	.021	.565	.018	.532	.016	.493
.01	19 .	. 702	.019	. 670	.044	. 722	.024	. 647	.022	.617	.030	.638	.021	.586	.023	.578	.019	.542	.017	. 506
.0	21	.715	.020	.677	.054	.744	.028	. 666	.024	.631	.035	.654	.023	•599	.025	• 591	.021	• 559	.018	.517
.0	23	-725	.021	.004	.074	.781	.033	.003	.028	.048	.040	. 666	.025	.608	.030	.612	.023	• 574	.019	.526
.0	27	-134 -247	.022	. 704	.114	.844	.050	. 721	.055	.676	.047	686	.030	.029 6hh	-035	.020	.025	• 504 50h	.021	• 543
.0	29	.750	.026	.709	.134	.875	.058	737	.048	<b>.6</b> 98	.060	.702	.040	.655	.045	.650	.029	.602	.025	.568
.0	31	. 758	.028	.717	.154	. 904	.068	.752	.058	.716	.070	.716	.045	.665	.050	.658	.031	.609	.027	.575
.0	33	.765	.030	.724	.174	.928	.078	.770	.068	•733	.080	.729	.050	.674	.060	.674	.033	.617	.030	.588
.0	57 10	-771	.035	.741	.194	• 949 of 8	.098	.800	.078	-747	.090	.741	.050	.689	.070	.688	.035	.624	.035	.605
.0	45	.801	.045	.766	.234	.979	.138	. 854	.108	.789	.110	.767	.080	.716	.000	.713	.045	.644	.040	.628
.0	50	.815	.050	775	.254	.991	158	.879	128	. 813	.130	.790	.090	.729	.100	.725	.050	.652	.050	.636
.0	55	. 829	.055	.787	.274	.996	.178	.903	.148	.836	.150	.813	.100	.741	.125	.752	.060	.668	.060	.655
.0	60	.844	.060	.798	.294	1.00	.198	.924	.168	.857	.170	.832	.125	.771	.150	.777	.070	.683	.070	.667
.0	70	870	.005	.009	• 314 ววh	1.00	.210	.941	208	.0// 807	.190	- 051	175	.794	- 175	•799	.080	·095	.080	.070
.ŏ	75	.883	.075	.829	.350	1.00	.258	.974	.228	.917	.230	.889	.200	.840	.225	.840	.100	.721	.100	.700
.0	Βó –	. 894	.080	. 839			.278	. 984	.248	. 933	.250	.902	.225	.861	.250	. 859	.125	744	.120	.723
.0	85	. 905	.085	. 847			.298	• 994	.268	.948	.270	.916	.250	.881	.275	.877	.150	.766	.140	.742
.0	90	.916	.090	.856			-318	•999	.288	.962	.290	.932	.275	.899	.300	. 895	.175	.789	.160	.758
-0	97 M	. 920	100	-005 875			• 330 358	1.00	- 300	•973 08b	.330	· 959	. 300	.910	350	.911	.200	.009	. 100	.790
	05	.945	.105	.883			.375	1.00	.348	.990	.410	.990	.350	.947	.375	.937	.250	.847	.220	.804
.1	1Ó	953	.110	. 893					. 368	• 997	. 450	. 999	•375	.961	400	.949	275	.863	.240	. 820
1	15	.961	.120	.908					.408	1.00	. 490	1.00	.400	.971	.425	.959	. 300	. 881	.260	.832
!	20	.967	.130	.923					.448	1.00	. 530	1.00	.425	.981	.450	. 971	.325	.897	.280	.845
	27 25	.982	.140	. 939					• 4 ( >	1.00	•717	1.00	. 470	.909	.500	. 988	.375	.926	. 320	.871
.1	45	.989	.160	.961									.525	.998	.525	.993	.400	.939	.340	.885
.1	55	.992	.170	.974									.575	1.00	.575	997	. 425	.950	.360	.895
.1	65	996	.180	. 981									. 650	1.00	. 625	1.00	450	. 960	. 380	.906
.1	85	1.00	.190	.989									.700	1.00	.675	1.00	. 475	.972	. 400	.918
.2	05	1.00	.210	.998											. 725	1.00	. 500	• 979	.440	•937
•2	27	1.00	-230	1.00											.000	1.00	.600	1.00	.520	.960
			.270	1.00													.650	1.00	.560	.980
			1210														.700	1.00	.600	. 992
																	.750	1.00	. 640	. 996
																	.800	1.00	.680	1.00
																				1 ^^

.680 .720 .760

.00

# Velocity Profile Data for Layer with $\frac{V_0}{U_1} = 0.0017$ , $U_1 = 50$ ft/sec, Zero Pressure Gradient.

X INCH	ES FROM	L.E.	5.6	0	8;3	1	1.5	14.	5	17.4		21.5	25.	25.0			31.0	34	•2
RE NIM	(FI./0		2626	2 31	26201	,	6205	26400		21.14			91.31		71.27		50.99 50.99		• 99 1.02
TNIECT			001	70	00171	5	00171	204	171	20204		20095	200	171	20102	•	20424	20	424
DELMORET		unne)	.001	ι <u>ε</u> δ	.00171	•	0565	.00	70	.0017	1	.00171	.00	4 7 1 1-12	1000	1	1000	.0	
	THOUSE	ioneo /	.020	~	.0300	•	0707	.00	19 55	.0032		.0900		4(	.12(3		.1370	. 1	470
TUPLE (	INCRES )	,	.017	0 .c	.0290	•	0313	.04	77 	.0555		.0055	.07	.70	.0859		.0929	.0	999
			1.72	20	1.506	1	.510	1.4	93	1.500		1.476	1.4	.88	1,482		1.475	1.	471
RE-THE	TA		44	•7	010		980	12	01	1458		1710	20	10	2248		2454		640
X =	5.6	X =	8.3	X =	11.5	X =	14.5	X =	X = 17.4		21.5	X =	25.0	X =	28.4	X =	31.0	X =	34.2
Y	ប/ហ	Y	ប/បា	Y	<b>บ/บ</b> 1	Y	u/uI	Y	ប/បា	Y	U/UI	Y	บ/บา	Y	υ/υΙ	Y	บ <b>/บา</b>	Y	ប/បា
.005 .006 .007 .008 .009 .011 .012 .013 .014 .015 .017 .021 .023 .033 .038 .048 .058 .048 .058 .063 .058 .063 .058 .058 .058 .058 .058 .058 .058 .058	45542388505435085848858585845885997644482581580000	.005 .006 .007 .008 .009 .010 .012 .013 .014 .015 .017 .023 .025 .030 .035 .040 .055 .055 .055 .055 .055 .055 .05	01440367711487556666691289388285420162276119866800000	$\begin{array}{c} .005\\ .007\\ .008\\ .009\\ .011\\ .012\\ .013\\ .014\\ .015\\ .0167\\ .025\\ .035\\ .045\\ .0555\\ .065\\ .065\\ .070\\ .080\\ .0110\\ .1100\\ .1100\\ .220\\ .2340\\ .255\\ .268\\ .340\\$	.3354569261135012216677988824466688799964430885150056991455531999900000	$\begin{array}{c} .005 \\ .006 \\ .007 \\ .008 \\ .009 \\ .011 \\ .012 \\ .013 \\ .015 \\ .016 \\ .017 \\ .019 \\ .023 \\ .025 \\ .035 \\ .040 \\ .075 \\ .035 \\ .040 \\ .075 \\ .050 \\ .060 \\ .070 \\ .075 \\ .040 \\ .075 \\ .040 \\ .075 \\ .040 \\ .075 \\ .040 \\ .075 \\ .040 \\ .075 \\ .040 \\ .075 \\ .040 \\ .075 \\ .040 \\ .075 \\ .040 \\ .075 \\ .040 \\ .075 \\ .040 \\ .075 \\ .040 \\ .075 \\ .040 \\ .075 \\ .040 \\ .075 \\ .040 \\ .075 \\ .040 \\ .075 \\ .040 \\ .075 \\ .040 \\ .075 \\ .040 \\ .075 \\ .050 \\ .075 \\ .015 \\ .0$	31386159161477226665584655641733066848257880133455556598999990000 31386915916147722666658846556417330688482578801334555565999999990000	$\begin{array}{c} .005\\ .006\\ .007\\ .008\\ .009\\ .010\\ .012\\ .013\\ .014\\ .015\\ .016\\ .017\\ .023\\ .035\\ .040\\ .055\\ .060\\ .070\\ .080\\ .090\\ .110\\ .120\\ .210\\ .230\\ .240\\ .250\\ .200\\$	29974224271888244448441235826888774948881772578888888557777776666633195567753370000	$\begin{array}{c} .005\\ .007\\ .008\\ .009\\ .010\\ .012\\ .013\\ .014\\ .015\\ .017\\ .025\\ .030\\ .045\\ .056\\$	27544 3142 3342 3342 3342 3342 3342 3342 33	.005 .006 .007 .008 .009 .011 .012 .013 .014 .015 .019 .023 .025 .030 .025 .030 .025 .030 .025 .030 .025 .035 .045 .056 .056 .056 .057 .045 .056 .056 .057 .045 .057 .045 .056 .056 .057 .045 .057 .045 .057 .045 .056 .057 .045 .057 .045 .057 .045 .057 .045 .056 .057 .045 .057 .045 .056 .057 .045 .057 .045 .056 .045 .056 .057 .045 .056 .045 .056 .056 .056 .056 .057 .045 .056 .056 .056 .057 .045 .056 .056 .056 .057 .045 .056 .056 .056 .056 .057 .045 .056 .056 .056 .056 .056 .056 .056 .05	266821154443731198835096222800605567702119774052882971138999988663960000	.005 .006 .007 .008 .009 .011 .012 .013 .015 .017 .019 .025 .040 .035 .040 .035 .040 .035 .040 .035 .040 .035 .040 .050 .05	26772 29211 33251 33853 3442 35534 35534 35554 355777 38848 383777 38848 3885 357777 38944 35577772 24444 359999999000000	.005 .006 .007 .008 .009 .010 .011 .012 .013 .015 .010 .025 .030 .040 .035 .040 .045 .055 .040 .055 .050 .040 .055 .050 .040 .055 .050 .05500 .0550 .0550 .05500 .0550 .0550 .0550 .05500 .0550	2678739444 3329444 33389600333486705788867648835666488372996247726016724477811244454430088295990000 	.005 .006 .007 .008 .009 .010 .011 .012 .013 .014 .015 .017 .025 .030 .040 .045 .050 .040 .045 .050 .040 .04	2576633322233340431103752444555555566778255757566778255755667782557575667782557575667782557575667782557575667782557575667782557575667782557575667782557575667782557575667782557575667782557575667782557575667782557575667782557575667782556677825575756677825566778255757566778255667782557575667782556677825575756677825566778255757578667866786678667826677825577782585868589599745586678266778255777782658687886889599745586678266778257778265868788688959974556678266778257778265868786678267782577782658687866768667826777825777826586878667777827868588959782858888888888888888888888888888

# Velocity Profile Data for Layer with $\frac{V_0}{U_1} = 0.0032$ , $U_1 = 50$ ft/sec, Zero Pressure Gradient.

X INCHES FROM L.E. 5.6	8.3	11.5	14.5	17.4	21.5	25.0	28,4	31.0	34.2	
U-ONE (FT./SEC.) 49.83	50.64	51.30	51.49	51.33	51.17	51,12	51,22	51.09	51.06	
RE NUMBER PER INCH 25878	26347	26217	26317	26312	26389	26447	26498	26464	26368	
INJECTION RATE .00335	.00330	.00326	.00324	.00325	.00326	.00327	.00326	.00327	.00327	
DELTA STAR(INCHES) .0302	.0493	.0739	•0900 '	.1095	.1356	.1569	.1817	.1937	.2085	
THETA(INCHES) .0191	.0309	.0464	.0576	.0695	.0860	.0992	.1155	. 1236	.1334	
н 1.583	1.595	1.592	1.563	1.576	1.577	1.581	1.572	1.567	1.564	
RE-THETA 494	814	1217	1515	1829	2270	2624	3061	3271	3516	
X = 5.0 $X = 8.3$ $X =$	· 11.5	X = 14.5	X = 17.4	X = 21.5	Χ =	25.0 X	= 28.4	X = 31.0	X = 34.2	
	0/01	Y U/UI	Y U/U1	Y U/UI	Y	י∪/טז צ	U/UI	Y U/U1	Y U/U1	
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	i       .265         i       .265         i       .265         i       .306         i       .418         i       .430         i       .430         i       .530         i       .550         i       .566         i       .582         i       .618         i       .679         i       .773         i       .770         i       .887         i       .887         i       .896 <td< th=""><th><math display="block">\begin{array}{cccccccccccccccccccccccccccccccccccc</math></th><th>.005         .240           .006         .248           .007         .265           .008         .284           .009         .302           .010         .321           .011         .341           .012         .368           .013         .368           .014         .394           .017         .414           .019         .432           .021         .447           .023         .454           .030         .451           .025         .468           .030         .451           .025         .468           .030         .451           .025         .468           .030         .519           .045         .532           .050         .545           .060         .503           .050         .545           .060         .600           .090         .616           .100         .631           .100         .643           .120         .660           .120         .660           .120         .660           .200<th>.005 .219 .006 .226 .007 .240 .008 .260 .009 .278 .010 .294 .011 .310 .12 .328 .013 .346 .014 .357 .015 .369 .017 .309 .019 .408 .021 .428 .023 .437 .025 .449 .025 .449 .025 .449 .025 .449 .025 .507 .030 .472 .030 .588 .040 .588 .040 .588 .040 .597 .050 .518 .040 .588 .040 .588 .040 .588 .040 .588 .040 .588 .040 .588 .040 .588 .000 .000 .000 .000 .000 .000 .000 .0</th><th>.005 .006 .007 .008 .009 .010 .011 .013 .014 .013 .014 .016 .016 .016 .016 .016 .020 .035 .040 .045 .050 .050</th><th><math display="block">\begin{array}{cccccccccccccccccccccccccccccccccccc</math></th><th><math display="block">\begin{array}{cccccccccccccccccccccccccccccccccccc</math></th><th>.005 .224 .006 .238 .007 .246 .008 .262 .009 .274 .010 .291 .011 .303 .012 .315 .014 .340 .016 .358 .018 .374 .025 .415 .030 .431 .035 .449 .040 .460 .050 .483 .060 .500 .070 .513 .080 .528 .100 .553 .120 .574 .140 .592 .160 .608 .240 .674 .220 .660 .240 .674 .220 .660 .240 .674 .220 .660 .240 .674 .220 .660 .240 .674 .220 .643 .220 .660 .240 .674 .260 .885 .280 .702 .300 .716 .340 .744 .380 .774 .420 .953 .580 .895 .500 .849 .540 .873 .580 .994 .700 .953 .740 .968 .780 .994 .850 .994</th><th>.005         .201           .006         .220           .007         .228           .008         .243           .009         .266           .010         .276           .011         .332           .014         .332           .014         .332           .014         .332           .020         .387           .020         .387           .030         .411           .035         .4459           .040         .459           .050         .450           .060         .521           .050         .453           .060         .521           .050         .452           .060         .521           .060         .521           .060         .521           .060         .521           .120         .563           .140         .582           .140         .766           .280         .668           .320         .716           .280         .668           .290         .931           .520         .835           .600<!--</th--></th></th></td<>	$\begin{array}{cccccccccccccccccccccccccccccccccccc$	.005         .240           .006         .248           .007         .265           .008         .284           .009         .302           .010         .321           .011         .341           .012         .368           .013         .368           .014         .394           .017         .414           .019         .432           .021         .447           .023         .454           .030         .451           .025         .468           .030         .451           .025         .468           .030         .451           .025         .468           .030         .519           .045         .532           .050         .545           .060         .503           .050         .545           .060         .600           .090         .616           .100         .631           .100         .643           .120         .660           .120         .660           .120         .660           .200 <th>.005 .219 .006 .226 .007 .240 .008 .260 .009 .278 .010 .294 .011 .310 .12 .328 .013 .346 .014 .357 .015 .369 .017 .309 .019 .408 .021 .428 .023 .437 .025 .449 .025 .449 .025 .449 .025 .449 .025 .507 .030 .472 .030 .588 .040 .588 .040 .588 .040 .597 .050 .518 .040 .588 .040 .588 .040 .588 .040 .588 .040 .588 .040 .588 .040 .588 .000 .000 .000 .000 .000 .000 .000 .0</th> <th>.005 .006 .007 .008 .009 .010 .011 .013 .014 .013 .014 .016 .016 .016 .016 .016 .020 .035 .040 .045 .050 .050</th> <th><math display="block">\begin{array}{cccccccccccccccccccccccccccccccccccc</math></th> <th><math display="block">\begin{array}{cccccccccccccccccccccccccccccccccccc</math></th> <th>.005 .224 .006 .238 .007 .246 .008 .262 .009 .274 .010 .291 .011 .303 .012 .315 .014 .340 .016 .358 .018 .374 .025 .415 .030 .431 .035 .449 .040 .460 .050 .483 .060 .500 .070 .513 .080 .528 .100 .553 .120 .574 .140 .592 .160 .608 .240 .674 .220 .660 .240 .674 .220 .660 .240 .674 .220 .660 .240 .674 .220 .660 .240 .674 .220 .643 .220 .660 .240 .674 .260 .885 .280 .702 .300 .716 .340 .744 .380 .774 .420 .953 .580 .895 .500 .849 .540 .873 .580 .994 .700 .953 .740 .968 .780 .994 .850 .994</th> <th>.005         .201           .006         .220           .007         .228           .008         .243           .009         .266           .010         .276           .011         .332           .014         .332           .014         .332           .014         .332           .020         .387           .020         .387           .030         .411           .035         .4459           .040         .459           .050         .450           .060         .521           .050         .453           .060         .521           .050         .452           .060         .521           .060         .521           .060         .521           .060         .521           .120         .563           .140         .582           .140         .766           .280         .668           .320         .716           .280         .668           .290         .931           .520         .835           .600<!--</th--></th>	.005 .219 .006 .226 .007 .240 .008 .260 .009 .278 .010 .294 .011 .310 .12 .328 .013 .346 .014 .357 .015 .369 .017 .309 .019 .408 .021 .428 .023 .437 .025 .449 .025 .449 .025 .449 .025 .449 .025 .507 .030 .472 .030 .588 .040 .588 .040 .588 .040 .597 .050 .518 .040 .588 .040 .588 .040 .588 .040 .588 .040 .588 .040 .588 .040 .588 .000 .000 .000 .000 .000 .000 .000 .0	.005 .006 .007 .008 .009 .010 .011 .013 .014 .013 .014 .016 .016 .016 .016 .016 .020 .035 .040 .045 .050 .050	$\begin{array}{cccccccccccccccccccccccccccccccccccc$	$\begin{array}{cccccccccccccccccccccccccccccccccccc$	.005 .224 .006 .238 .007 .246 .008 .262 .009 .274 .010 .291 .011 .303 .012 .315 .014 .340 .016 .358 .018 .374 .025 .415 .030 .431 .035 .449 .040 .460 .050 .483 .060 .500 .070 .513 .080 .528 .100 .553 .120 .574 .140 .592 .160 .608 .240 .674 .220 .660 .240 .674 .220 .660 .240 .674 .220 .660 .240 .674 .220 .660 .240 .674 .220 .643 .220 .660 .240 .674 .260 .885 .280 .702 .300 .716 .340 .744 .380 .774 .420 .953 .580 .895 .500 .849 .540 .873 .580 .994 .700 .953 .740 .968 .780 .994 .850 .994	.005         .201           .006         .220           .007         .228           .008         .243           .009         .266           .010         .276           .011         .332           .014         .332           .014         .332           .014         .332           .020         .387           .020         .387           .030         .411           .035         .4459           .040         .459           .050         .450           .060         .521           .050         .453           .060         .521           .050         .452           .060         .521           .060         .521           .060         .521           .060         .521           .120         .563           .140         .582           .140         .766           .280         .668           .320         .716           .280         .668           .290         .931           .520         .835           .600 </th	

# Velocity Profile Data for Layer with $\frac{V_0}{U_1} = 0.0046$ , $U_1 = 50$ ft/sec, Zero Pressure Gradient.

INCHES FROM L.E.	5.6	8.3	11.5	14.5	17.4	21.5	25.0	28.4	31.0	34.2
U-ONE (FT./SEC.)	50.84	51.79	51.40	51.30	51.36	51.46	51.36	51.40	51.35	51.34
RE NUMBER PER INCH	25778	26376	26567	26517	26501	26468	26418	26473	26531	26771
INJECTION RATE	.00468	.00460	.00463	.00464	.00463	.00463	.00463	.00463	.00463	.00464
DELTA STAR (INCHES)	.0330	.0559	.0869	.1111	.1377	.1701	•1933	.2235	.2371	.2560
THETA(INCHES)	.0203	.0339	.0523	.0670	.0824	.1024	.1172	.1348	.1449	.1572
H	1.631	1,648	1.662	1.658	1.672	1.661	1.648	1.657	1.636	1.628
RE-THETA	522	895	1389	1776	2183	2711	3097	3570	3845	4208
x = 5.6 x =	8.3 X =	11.5	X = 14.5	X = 17.4	X = 21.5	X =	25.0 X =	28.4	X = 31.0	X = 34.2
צ ט/טו צ	u/ut Y	ប/បា	Y U/UI	ייע ע	Y U/UI	Y	ע/טז צ	u/uI	Y U/U1	Y U/U1
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	.265       .005         .290       .006         .310       .007         .328       .006         .352       .009         .352       .009         .352       .009         .352       .001         .404       .014         .418       .014         .418       .014         .443       .033         .500       .033         .513       .044         .559       .056         .569       .066         .569       .066         .567       .076         .560       .100         .650       .100         .650       .100         .650       .20         .707       .146         .733       .166         .763       .166         .763       .160         .773       .166         .793       .224         .930       .266         .930       .266         .993       .32         .993       .32         .993       .32         .993       .32         .993	233         243         243         243         243         2575         288         233         2575         288         233         2433         2575         288         2333         2433         2575         288         2933         2934         2935         2940         2940         2940         2940         2940 <t< td=""><td><math display="block">\begin{array}{cccccccccccccccccccccccccccccccccccc</math></td><td><math display="block">\begin{array}{cccccccccccccccccccccccccccccccccccc</math></td><td>.005 .172 .006 .175 .007 .191 .008 .203 .009 .221 .010 .237 .012 .262 .014 .292 .014 .292 .014 .292 .014 .292 .014 .334 .020 .352 .020 .352 .035 .420 .035 .420 .045 .441 .050 .451 .050 .500 .500 .500</td><td>2 .005 .006 .007 .008 .009 .010 .012 .014 .016 .025 .025 .035 .040 .025 .035 .040 .040 .035 .040 .035 .040 .040 .050 .035 .040 .040 .050 .035 .040 .040 .050 .035 .040 .040 .050 .055 .050 .050 .050 .055 .050 .050 .055 .050 .050 .055 .050</td><td><math display="block">\begin{array}{cccccccccccccccccccccccccccccccccccc</math></td><td><math display="block">\begin{array}{cccccccccccccccccccccccccccccccccccc</math></td><td><math display="block">\begin{array}{cccccccccccccccccccccccccccccccccccc</math></td><td><math display="block">\begin{array}{cccccccccccccccccccccccccccccccccccc</math></td></t<>	$\begin{array}{cccccccccccccccccccccccccccccccccccc$	$\begin{array}{cccccccccccccccccccccccccccccccccccc$	.005 .172 .006 .175 .007 .191 .008 .203 .009 .221 .010 .237 .012 .262 .014 .292 .014 .292 .014 .292 .014 .292 .014 .334 .020 .352 .020 .352 .035 .420 .035 .420 .045 .441 .050 .451 .050 .500 .500 .500	2 .005 .006 .007 .008 .009 .010 .012 .014 .016 .025 .025 .035 .040 .025 .035 .040 .040 .035 .040 .035 .040 .040 .050 .035 .040 .040 .050 .035 .040 .040 .050 .035 .040 .040 .050 .055 .050 .050 .050 .055 .050 .050 .055 .050 .050 .055 .050	$\begin{array}{cccccccccccccccccccccccccccccccccccc$	$\begin{array}{cccccccccccccccccccccccccccccccccccc$	$\begin{array}{cccccccccccccccccccccccccccccccccccc$	$\begin{array}{cccccccccccccccccccccccccccccccccccc$

# Velocity Profile Data for Layer with $\frac{V_0}{U_1} = 0.008$ , $U_1 = 50$ ft/sec, Zero Pressure Gradient.

X MORES FROM L.E.         5.6         8.3         11.5         14.5         17.4         21.5         25.0         28.4         31.0         34.2           U-CIRE (FT, /SEC.)         49.46         50.59         50.57         50.59         51.25         51.30         51.24         51.28         51.32         26.467         26.499         26.697         26.699         26.697         26.693         26.697         26.999         26.697         26.993         26.697         26.993         26.697         2.699         26.697         2.699         2.607         2.6083         2.6014         2.779         .3175         .3755         .4447         .4767         .5101           THELM STRUM (TRUERS)         0.607         0.663         1.796         1.976         .2175         .2117         .2201         .2211         .2419         .2515           R         1.721         1.669         1.596         1.592         1.994         2.014         2.005         2.601         1.991         6.695           X         V/U         Y         V/U         Y         V/U         Y         V/U         Y         V/U         Y         Y         Y         Y         Y         Y         Y         Y																				
U-CIRE (FT, /ERC.) 49.46 50.50 50.57 50.57 51.22 51.25 51.30 51.24 51.28 51.52 51.30 51.24 51.28 51.52 51.50 51.24 51.28 51.52 51.50 51.24 51.28 51.52 51.50 51.24 51.28 51.52 51.50 51.52 51.50 51.52 51.50 51.52 51.50 51.52 51.50 51.52 51.50 51.52 51.50 51.52 51.50 51.52 51.50 51.52 51.50 51.52 51.50 51.52 51.50	X INCHI	es from	I L.E.	5.6	;	8.3	1	1.5	14.	5	17.4		21.5	25.	.0	28.4		31.0	34	.2
NE RUMBER PER LINER         25330         26467         26712         26784         26477         2699         26007         26693         26071         26793           RUMCTION FARE         .00053         .00056         .00050         .00054         .00050         .00054         .00050         .0005         .000	U-ONE	(FT./S	EC.)	49.4	6	50.50	5	<b>0.</b> 97	50.	95	51.22		51.25	51.	30	51.24	ŧ	51.32	51	•57
ENDERTION         FAURE         .00833         .00816         .00809         .00809         .00803         .00804         .00803         .00803         .0080	RE NUM	BER PER	INCH	2553	0	26467	2	6712	267	84	26487		26499	268	307	26853	}	26651	26	5748
DELCA STARTINGTHES         .0407         .0863         .1470         .1925         .2479         .3175         .3775         .1447         .1777         .1777           THEEA(INGRES)         .0027         .0661         .0750         .0966         .1249         .1576         .1673         .2201         .2419         .2615           R         .1721         1.669         1.960         1.952         1.984         2.014         2.005         2.020         1.979         1.950           X = 5.6         X = 8.3         X = 11.5         X = 11.5         X = 11.4         X = 21.5         X = 25.0         X = 28.4         X = 31.0         X = 34.2           Y         U/UT         Y	INJECT	ION RA	TE	.008	33	<b>.0</b> 0816	•	<b>0080</b> 8	.00	809	.0080	4	.00804	.00	0803	.0080	)4	.00803	.0	0799
THEMA (INGURDES)         .0237         .0461         .0790         .0966         .1249         .1576         .1673         .2201         .2419         .2615           R         1.721         1.669         1.950         1.952         1.984         2.014         2.005         2.020         1.979         1.990           NE-THERM         604         1221         2003         2641         3308         4177         5021         5911         6448         6995           X = 5.6         X = 8.3         X = 11.5         X = 17.4         X = 21.5         X = 25.0         X = 28.4         X = 31.0         X = 94.2           Y         U/UT         Y	DELTA	STAR(IN	CHES)	.040	7	.0863		1470	.19	25	.2479	,	.3175	•3'	755	, կկկ-	,	. 4787	.5	101
R         1.721         1.869         1.960         1.952         1.994         2.014         2.005         2.020         1.979         1.990           RE-THERA         604         1221         2003         2641         3308         4177         5021         5911         6448         6995           X = 5.6         X = 8.3         X = 11.5         X = 11.5         X = 11.5         X = 11.7         X = 21.0         X = 28.4         X = 31.0         X = 34.2           Y         U/U1         Y         U/U1 </td <td>THETA(</td> <td>inches)</td> <td>)</td> <td>.023</td> <td>7</td> <td>.0461</td> <td></td> <td>0750</td> <td>.09</td> <td>86</td> <td>.1249</td> <td>,</td> <td>.1576</td> <td>.18</td> <td>373</td> <td>.2201</td> <td></td> <td>.2419</td> <td>.2</td> <td>615</td>	THETA(	inches)	)	.023	7	.0461		0750	.09	86	.1249	,	.1576	.18	373	.2201		.2419	.2	615
<b>FE-THEFA</b> <b>604 1221</b> 2003 2641 3306 <b>1</b> 177 5021 5911 6448 66995 <b>x - 5.6 x = 6.3 x = 11.5 x = 14.5 x = 17.4 x = 21.5 x = 25.0 x = 26.4 x = 31.0 x = 34.2</b> <b>x U/U1 x U</b>	Ħ			1.72	1	1.869	1	. 960	1.9	52	1.984		2.014	2.0	005	2.020	,	1.979	1.	950
$ \begin{array}{c} x = 5.6 \\ x = 8.3 \\ y = 11.5 \\ y = 1$	RE-THE	TA		60	<u>)4</u>	1221		2003	26	41	33 <b>0</b> 8	3	4177	50	021	5911		6448	6	995
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$																			-	
Y         U/U1         Y	X =	5.6	X =	8.3	X =	11.5	X =	14.5	X =	17.4	X =	21.5	Х ≖	25.0	X =	28.4	X =	31.0	X =	34.2
.005 289 .007 174 .007 180 .016 128 .007 131 .007 108 .017 .009 .017 .007 .007 .009 .007 082	Y	ប/ហ	Y	ប/បា	Y	บ/บ1	Y	υ/υΙ	Y	ບ/ບາ	Y	U/UI	Y	U/U1	Y	U/UI	' Y	บ/บ <b>1</b>	Y	U/U1
1.35 .976 1.60 .993 1.40 .984 1.70 .997 1.50 .964 1.70 .997	x .005 .006 .009 .011 .012 .014 .015 .014 .015 .014 .015 .025 .030 .040 .055 .040 .055 .055 .060 .055 .060 .055 .060 .055 .060 .055 .055	0 2904 33247 33402 4348 2904 4348 2904 4348 2907 33402 4348 2907 33402 4348 2907 33402 4348 2907 33402 4348 2907 33402 4348 2907 33402 4348 2907 33402 4348 2907 33402 4348 2907 33402 4348 2907 33402 4348 2907 35702 6668 888 8999 9958 99958 99958 10000 1000 1000 1000 1000 1000	Y .005 .007 .011 .013 .015 .025 .029 .031 .035 .025 .029 .031 .035 .025 .029 .040 .045 .055 .060 .045 .055 .055 .060 .045 .055 .055 .045 .055 .055 .055 .045 .055 .05	U/U 1405885266117778665222266646498420773988345994859900000	Y .005.010 .025.035 .040.055 .055.040 .0555.040 .0400 .1400 .1400 .1400 .2400 .2400 .3400 .4400 .5560 .4400 .5560 .4400 .5560 .4400 .5560 .4400 .5560 .4400 .4400 .5560 .4400 .4400 .5560 .44000 .4400 .4400 .4400 .44000 .4400 .4400 .44000 .44000 .44000 .44000 .44000 .440000	U/U1 1282 22808 33241 33680 33241 35680 33241 35680 33241 35680 33241 35680 33241 35680 33241 35680 33241 35680 33241 35680 3241 35776966 329900 3000 329000 329000 329000 329000 329000 329000 329000 329000 329000000 329000000000000000000000000000000000000	Y .005 .010 .025 .026 .025 .040 .040	U 135514032003555376214686606028473666606288572557788899390400000 333333333341488606600284736666062885725577888999999900000	Y .005.010 .025.035 .040.050 .050.060 .050.000 .050.000 .050.000 .050.000 .050.000 .050.000 .050.000 .050.0000 .050.0000 .050.0000 .050.0000 .050.0000 .050.00000 .050.00000 .050.00000 .050.00000000	U 128735815573288246959781133662258883135585332214468433700000	Y .005.025 .025.0305 .0405.0500 .0450.0500 .0450.0500 .0450.0500 .0500.0500	U/UI 88884 161 1912225222 225322229148 33263355535572996 5555572996 55555729667775244451 55555729667775244451 55555729667775244451 55555729667775244451 55555729667775244451 55555729667775244451 55555729667775244451 55555729667775244451 55555729667775244451 55555729667775244451 55555729667775244451 55555729667775244451 55555729667775244451 555557296775244451 555557296775244451 555557296775244451 555557296775244451 555557296775244451 555557296775244451 555557296775244451 55555729677775244451 55555729677775244451 555557299757294451 555557299757294451 555557299757294451 555557299757294451 555557299757294451 555557299757294451 555557299757294451 555557299757294451 555557299757294451 555557299757294451 555557299757294451 555557299757294451 555557299757294451 555557299757294451 555557299757294451 555557299757294451 555557299757294455 555557299757294455 555557299757294 555557299757294455 555557299757294 555557299757294 55557299757294 55557299757294 55557299757294 55557299757294 55557299757294 55557299757294 555572997577777777777777777777777777777	Y .0055 .010 .0150 .0255 .0305 .040 .0455 .0500 .0455 .0500 .0500 .0500 .0500 .0500 .1200 .1400 .2400 .2400 .2400 .2400 .3200 .3200 .3200 .3200 .3200 .3200 .3200 .3200 .3200 .2400 .2550 .2000 .1000 .1000 .2000 .1000 .2000 .1000 .2000 .1000 .2000 .1000 .2000 .1000 .2000 .1000 .2000 .2000 .0000 .0000 .20000 .2000 .2000 .2000 .2000 .2000	U 87298724338882741295519633927517777809887084065388999990000 U 872987232578333333333344346272755555556658775788835891440557559990000	Y .005 .025 .030 .045 .050 .050 .045 .050 .05	UI 829251511668779902339904117743327188211799336689644998154458729226131146999999990000	Y 0055 0079 0011 0133 0155 0225 0305 0255 025	U/U 662 307 58 11 38 77 53 37 59 30 66 44 15 59 71 96 30 55 55 55 55 55 55 55 55 55 55 55 55 55	Y .005 .010 .025 .035 .035 .040 .045 .035 .040 .045 .035 .040 .045 .035 .040 .045 .035 .040 .045 .035 .040 .045 .035 .040 .045 .035 .040 .045 .035 .040 .045 .040 .045 .040 .045 .040 .045 .040 .045 .040 .045 .040 .045 .040 .045 .040 .045 .040 .045 .040 .045 .040 .045 .040 .045 .040 .045 .040 .045 .040 .045 .040 .045 .040 .045 .040 .040 .040 .045 .040 .050 .040 .050 .040 .050 .040 .050	U/U1 -075 -092 -1111 -148 -1891 -2234 -27588 -27578 -27588 -275788

.997 1.00 1.00 1.00

# Vzelocity Profile Data for Layer with $\frac{V_0}{U_1} = 0$ , $U_1 = 150$ ft/sec, Zero Pressure Gradient.

X INCHES FROM L.E. 5.6	8.3	11.5	14.5	17.4	21.5	25.0	28.4	31.0	34.2
U-DNE (FT./SEC.) 146.04	145.77	145.28	145.10	145.36	145.75	144.87	144.59	144.89	- 145.91
RE NUMBER PER INCH 75188	75475	76142	76751	76149	75890	76621	77277	76495	75812
INJECTION RATE O	o	0	0	0	o	0	o	0	0
DELTA STAR(INCHES) .0216	.0274	.0369	.0453	.0499	.0599	.0670	.0744	<b>.0</b> 788	.0888
THETA(INCHES) .0152	.0196	.0264	.0325	.0357	.0430	.0484	.0530	.0565	.0645
H 1.425	1.397	1.400	1.393	1.400	1.394	1.385	1.404	1.395	1.377
RE-THETA 1142	1481	2 <b>0</b> 08	<b>24</b> 93	2717	3263	3 <b>70</b> 8	4095	4321	4889
x = 5.6 x = 8.3 x =	11.5	X = 14.5	X = 17.4	X = 21.5	X = 2	5.0 X =	28.4 X=	31.0	X = 34.2
Y U/UI Y U/UI Y	ប/បា	¥ U/UI	Y U/U1	Y U/UI	Y	U/U1 Y	U/UI Y	บ/บา	Y U/U1
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	$\begin{array}{c} 449\\ -470\\ -504\\ -578\\ -576\\ -598\\ -576\\ -585\\ -595\\ -603\\ -614\\ -676\\ -636\\ -664\\ -672\\ -773\\ -775\\ $	.003 .432 .004 .467 .005 .491 .006 .521 .007 .538 .009 .565 .010 .575 .011 .583 .012 .591 .013 .597 .015 .608 .017 .618 .017 .618 .017 .618 .019 .662 .025 .642 .030 .665 .725 .648 .030 .665 .725 .648 .030 .665 .728 .046 .775 .765 .728 .066 .779 .065 .746 .075 .765 .085 .746 .085 .746 .085 .746 .085 .789 .085 .789 .085 .789 .085 .789 .085 .789 .090 .991 .090 .991 .180 .822 .220 .944 .210 .955 .220 .944 .210 .955 .220 .944 .210 .955 .220 .944 .210 .975 .220 .944 .210 .955 .220 .944 .210 .975 .220 .994 .210 .975 .220 .994 .200 .994 .200 .997 .220 .994 .200 .997 .220 .994 .200 .997 .220 .994 .200 .997 .220 .994 .200 .997 .220 .994 .200 .997 .220 .994 .100 .005 .300 .000 .300 .000	$\begin{array}{cccccccccccccccccccccccccccccccccccc$	.005 .466 .006 .474 .007 .497 .008 .511 .009 .529 .010 .541 .011 .554 .013 .576 .013 .576 .013 .576 .015 .591 .017 .602 .019 .610 .025 .632 .030 .648 .035 .662 .040 .674 .045 .633 .055 .703 .060 .710 .065 .719 .070 .728 .075 .734 .080 .739 .100 .769 .110 .782 .120 .793 .130 .807 .140 .819 .170 .850 .180 .839 .170 .850 .180 .823 .200 .822 .210 .894 .220 .904 .230 .911 .240 .929 .270 .945 .310 .970 .330 .981 .350 .989 .370 .994 .390 .971 .00	.005 .006 .007 .008 .007 .011 .013 .015 .019 .021 .021 .021 .021 .021 .021 .021 .021	.459         .008           .473         .009           .493         .010           .508         .011           .529         .012           .542         .013           .553         .015           .563         .016           .570         .018           .573         .021           .602         .025           .610         .030           .626         .035           .641         .040           .653         .045           .647         .055           .648         .045           .667         .055           .648         .060           .704         .080           .705         .260           .695         .070           .738         .120           .741         .100           .776         .160           .816         .200           .910         .300           .927         .320           .940         .340           .997         .420           .000         .520           .000         .520           .000 <td>482         .008           494         .009           510         .010           523         .011           540         .012           552         .013           577         .015           588         .016           577         .015           588         .016           .577         .015           .605         .020           .617         .022           .630         .024           .643         .045           .657         .030           .667         .030           .667         .030           .684         .045           .692         .050           .708         .060           .719         .070           .734         .080           .767         .100           .826         .130           .846         .140           .807         .200           .947         .260           .958         .280           .948         .360           .977         .200           .948         .360           .998</td> <td>. 460 . 490 . 510 . 530 . 5559 . 5675 . 5695 . 5795 . 5695 . 7777 . 77790 . 8162 . 8847 . 8895 . 9929 . 9413 . 9988 . 9997 . 9988 . 9997 . 9988 . 9997 . 1000 . 10000 . 100000 . 100000 . 100000 . 100000 . 100000 . 1000000 . 10000000000</td> <td></td>	482         .008           494         .009           510         .010           523         .011           540         .012           552         .013           577         .015           588         .016           577         .015           588         .016           .577         .015           .605         .020           .617         .022           .630         .024           .643         .045           .657         .030           .667         .030           .667         .030           .684         .045           .692         .050           .708         .060           .719         .070           .734         .080           .767         .100           .826         .130           .846         .140           .807         .200           .947         .260           .958         .280           .948         .360           .977         .200           .948         .360           .998	. 460 . 490 . 510 . 530 . 5559 . 5675 . 5695 . 5795 . 5695 . 7777 . 77790 . 8162 . 8847 . 8895 . 9929 . 9413 . 9988 . 9997 . 9988 . 9997 . 9988 . 9997 . 1000 . 10000 . 100000 . 100000 . 100000 . 100000 . 100000 . 1000000 . 10000000000	

31

1.1

# Velocity Profile Data for Layer with $\frac{V_0}{U_1} = 0.0032$ , $U_1 = 150$ ft/sec, Zero Pressure Gradient.

X INCHES FROM L.E. 5.6	8.5	11.5	14.5	17.4	21.5	25.0	28.4	31.0	34.2
U-ONE (FT./SEC.) 146.59	148.49	148.13	149.34	148.89	148.13	148.34	147.99	148.57	147.64
RE NUMBER PER INCH 74479	75572	75651	75242	75573	75753	75238	75620	7578 <del>5</del>	75903
INJECTION RATE .00321	.00317	.00317	.00315	.00316	.00317	.00317	.00318	.00316	.00318
DELTA STAR(INCHES) .0251	.0386	.0599	.0783	.0958	.1230	.1383	.1636	.1777	.1972
THETA(INCHES) .0164	.0251	.0380	.0494	.0605	.0771	.0878	.1030	.1129	1258
н 1.536	1.540	1.579	1.584	1,585	1.595	1.575	1.588	1.574	1.567
RE-THETA 1218	1894	2872	3718	4569	5842	6609	7791	8554	9552
x = 5.6 x = 8.5 x =	11.5	X = 14.5	X = 17.4	X = 21.5	X =	25.0 X =	28.4	X = 31.0	X = 34.2
Y U/UI Y U/UI Y	บ/บ1	Y U/UI	Y U/U1	Y U/U	IY	u/u1 צ	υ/υΙ	Y U/U1	Y U/U1
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	.341 .352 .370 .4478 .4788 .4778 .4778 .4778 .4778 .4778 .5534 .5518 .5572 .5562 .7425 .6617 .6655 .7425 .6617 .5864 .8927 .9927 .9927 .9927 .000 1.000	.005 .327 .006 .332 .007 .343 .008 .357 .009 .369 .010 .382 .011 .399 .012 .412 .013 .425 .014 .436 .015 .446 .016 .455 .018 .467 .020 .478 .026 .506 .016 .455 .018 .467 .026 .506 .016 .455 .018 .467 .026 .506 .016 .455 .018 .467 .026 .506 .006 .599 .028 .514 .030 .552 .040 .555 .589 .050 .5777 .055 .589 .050 .5777 .050 .5777 .050 .5770 .050 .5777 .050 .500 .000 .848 .250 .918 .225 .984 .350 .903 .325 .984	$\begin{array}{cccccccccccccccccccccccccccccccccccc$	$\begin{array}{cccccccccccccccccccccccccccccccccccc$	$\begin{array}{cccccccccccccccccccccccccccccccccccc$	$\begin{array}{cccccccccccccccccccccccccccccccccccc$	.258         .269         .289         .318         .3343         .354         .3702         .3892         .418         .437         .463         .473         .495         .535         .617         .613         .734         .495         .535         .617         .633         .485         .554         .575         .617         .613         .756         .613         .998         .9997         .000         .001	005         .253           006         .263           007         .276           008         .291           009         .307           010         .322           011         .335           012         .346           013         .357           014         .365           023         .414           .025         .422           030         .438           .023         .414           .025         .422           .030         .438           .045         .465           .055         .494           .060         .502           .070         .518           .080         .525           .090         .545           .100         .558           .500         .652           .300         .712           .400         .809           .450         .809           .450         .809           .650         .909           .650         .909           .650         .909           .650         .908      .800         .995	.005 .261 .006 .270 .007 .2777 .008 .288 .009 .302 .010 .313 .011 .326 .012 .337 .013 .347 .014 .355 .015 .363 .017 .376 .019 .367 .021 .395 .023 .403 .025 .410 .030 .425 .035 .438 .040 .450 .035 .438 .040 .450 .055 .479 .050 .519 .050 .519 .070 .504 .080 .519 .070 .504 .080 .519 .070 .504 .480 .783 .450 .874 .500 .814 .500 .814 .550 .874 .550 .814 .550 .981 .450 .993 .770 .966 .800 .999 .100 .998 .900 .945

1.20 1.00

# Velocity Profile Data for Layer with $\frac{V_0}{U_1} = 0.008$ , $U_1 = 150$ ft/sec, Zero Pressure Gradient.

X INC	ies fr	OM L.E.	5.	.6	8.3		11.5	14	•5	17.4		21.5	25	5.0	28.4		31.0	31	4.2
U-ONE	(FT.	/sec.)	142,	.83	146.02	: 1	46.95	147	• 39	148.0	4	148.50	148	3.02	147.7	8	148.13	14	7.47
RE NUI	BER P	ER INCH	740	017	75435	;	75684	76	280	7604	8	75817	76	5268	7598	0	75699	76	6654
INJECT	LION 1	RATE	.00	0812	.0079	14	.00787	.0	<b>07</b> 88	.007	85	.00783		0787	.007	86	.00784		00783
DELTA	STAR (	INCHES)	.02	299	.0625		.1161	.1	583	.213	8	.2811	•3	3258	. 384	3	.4180		+442
THETA	(INCHE:	s)	.01	84	.0353		0594	.0	817	.104	в	.1393	.1	661	. 193	1	.2165	.2	2385
н			1.6	627	1.769		1.953	1.	937	2.04	D	2,018	1.	961	1.99	D	1.931	۱.	863
RE-THI	sta.		13	62	2666		4499	6	234	79 <b>7</b> 3	3	10560	12	2669	1467	3.	16387	18	3280
X =	5.6	X =	8.3	X =	11.5	X =	14.5	X =	17.4	X =	21.5	X =	25.0	¥ =	98 Ji	¥ -	21.0	¥ _	<b>a</b> k <b>a</b>
Y	ប/ហ	Y	ប/បា	Y	ប/បា	Y	U/UI	Y	บ/บา	Y	υ/υΙ	Y	U/U1	Y Y	U/UI	Y Y	ט/ט <b>ו</b>	х = Y	34•2 U/U
.005	• 390	.005	.258	.005	.159	.005	.145	.005	.086	.005	.104	.005	.106	.005	.069	.005	.088	.005	.104
.008	• 397	.005	283	.005	.161	.005	.154	.006	•090	.006	.107	.006	.109	.006	.074	.006	.092	.006	. 107
.008	432	.008	.301	.008	.171	.008	.177	.007	.094	-007	116	.007	.113	.007	-078 08h	.007	.097	.007	.112
.009	. 451	.009	.316	.010	.194	.010	.200	.009	.104	.009	.122	.009	.127	.000	.004	.008	.116	.000	. 120
.010	.471	.010	• 331	.012	.220	.012	.218	.010	.113	.010	.130	.010	.135	.010	.096	.015	.152	.015	.168
.012	-400	.011	.345	.014	.241	.014	.236	.012	.130	.012	.142	.012	.149	.012	.110	. 020	.174	.020	.192
.013	.515	.012	.367	.018	.270	.018	.250	.014	162	.014	.158	.014	.164	.014	.125	.030	.213	.030	.226
.014	. 528	.014	.377	.020	.283	.020	.271	.018	.178	.018	.180	.018	.184	.018	.130 145	.040	.238	.040	.254
.015	- 541	.015	.384	.025	. 309	.025	.291	.020	.187	.020	.191	.020	.193	.020	.152	.060	.275	.060	.201
.017	.560	.017	.400	.030	•333	.030	.308	.025	.213	.025	.214	.025	.213	.030	188	.070	.289	.080	. 320
.021	.596	.019	. 414	-035	.350	.035	• 324	.030	•232	.030	.229	.030	.228	.040	.218	.080	. 305	.100	. 344
.023	.611	.023	438	.045	.382	.040	.351	.035	.240	.035	.244	.035	.242	.050	.238	.100	.329	.120	.365
. 025	.625	.025	. 449	.050	•397	.050	361	.045	.278	.050	.277	.040	.275	.000	.271	120	- 351	.140	- 385
.030	•658	.030	. 471	.055	.410	•060	.383	.050	.292	.060	.296	.060	.294	.080	292	.160	. 386	.180	.402
.035	-007	.035	.493	.060	• 423	.070	402	.060	.316	.070	•313	.070	.314	.090	.306	.180	. 403	.200	.431
.045	742	.045	.534	.0070	.430	.000	•425 .hhh	0,0	.338	.080	· 326	.080	• 329	.100	.321	.200	.419	.250	.464
. 050	766	.050	.552	.075	463	.100	.460	.000	. 375	.100	.352	.100	• 343 .35h	.120 110	• 345 268	·220	• 433	.300	.492
755	.789	.055	.570	•080	• 477	.120	.496	.100	.391	.120	.378	.120	.376	.160	. 388	.260	461	. 400	-219
	.809	.060	•589	.090	.503	.140	. 530	.120	.421	.140	.400	.140	397	.180	. 405	.280	474	.450	574
.070	.846	.080	.661	.110	- 520 55h	180	• 502	.140	.450	.160	• 423	.160	.419	.200	. 421	.300	. 486	. 500	. 602
.080	.877	.090	.691	.120	.575	.200	.627	.180	.508	.200	.444 263	.100	.430 Jugh	.220	.438	.350	.519	.550	.630
.090	.904	.100	.722	.140	.620	.220	.661	.200	.537	.220	.484	.250	494	.260	.470	.450	. 581	.650	.679
.100	•929	.110	• 754	•160 1Po	.667	.240	.694	.240	. 592	.240	. 506	.300	532	.280	484	. 500	. 613	.700	.705
.120	.963	.120	. 811	.200	.710	.260	•727 758	.280	•645	.260	. 526	. 350	.574	.300	.499	. 550	. 644	.750	.730
.130	.975	.140	.837	.220	.792	.300	.787	.360	.748	.200	- 547	.400	.014	.350	-533	.600	. 675	.800	•755
.140	.985	.150	.863	.240	. 831	.320	.819	. 400	794	.350	.620	.500	.694	.400	.601	. 700	. 733	1.00	.856
.150	•993	-160	.888	•260	.867	.340	.847	.440	.840	.400	.672	. 550	.737	. 500	.638	. 750	.763	1.10	. 899
.180	1.00	.180	.909	.200	.901	- 300	.679	.480	.883	. 450	. 721	.600	.775	.550	.674	.800	• 792	1,20	. 935
.200	1.00	.190	.945	.320	958	.400	.925	.560	.924	.550	813	. 050	.813 859	.600	.709 7b2	.850	.822	1.30	• 966
.220	1.00	.200	.960	.340	975	. 420	946	. 600	. 980	.600	.859	.750	.888	.700	.774	.900	.874	1.50	. 900
.250	1.00	.210	•974	.360	• 989	.440	.964	. 640	. 991	.650	901	. 800	.921	.750	806	1.00	.897	1.60	1.00
		.220	. 905	. 100	1.00	.460	•977	.680	.999	.700	•937	.850	• 947	.800	. 836	1.05	.919	1.70	1.00
		.260	.999	.460	1.00	.540	.998	. 760	1.00	-750	900	.900	.970	.850	.870	1.10	.941	1.80	1.00
		.280	1.00	. 500	1.00	.580	1.00	.800	1.00	.850	.997	1.00	.902	.900	.900	1.20	. 900		
		. 320	1.00			.620	1.00			. 900	997	1.10	. 998	1.00	.949	1.40	.997		
		• 400	1.00			.700	1.00			1.00	1.00	1.20	1.00	1,05	.968	1.50	1.00		
										1.10	1.00	1.30	1.00	1.10	• 979	1.60	1.00		
					•					1.20	1.00	1.40	1.00	1.20	.994	1.70	1.00		
														1.40	1.00				

# Velocity Profile Data for Layer with Pressure Distribution I.

X INCHES FROM L.E.	5.6	8.3	11.5	14.5	17.4	21.5	25.0	28.4	31.0	ah o
U-ONE (FT./SEC.)	53 <b>.6</b> 8	54.97	54.71	54.36	53.07	51.35	50,10	LB.88	51.0 58 51	)4.2 h7 57
RE NUMBER PER INCH	28325	29097	29086	28897	27871	26964	26517	25857	25506	4(+))
INJECTION RATE	.00182	.00178	.00179	.00180	.00184	.00190	00105	00000	£7790	29400
DELTA STAR(INCHES)	.0271	.0402	.0565	.0758	.0968	. 1291	. 1531	1820	.00202	.00205
THETA(INCHES)	.0174	.0262	.0373	.0498	0620	0817	0076	11052	.2023	.2225
Н	1,560	1, 533	1,516	1 522	1 569	1 570	1 560	. 1154	.1284	.1404
RE-THETA	492	763	1084	1440	1727	220%	0589	1.507	1.575	1.584
		1.5			. 12 (	2204	2900	2904	3207	3567
X = 5.6 X =	8.3 X =	11.5	X = 14.5	X = 17.4	X = 21.5	X =	25.0 X =	• 28.4 X =	31.0	X = 34.2
Y U/U1 Y	ע/טו צ	ប/បា	Y U/UI	¥ U/U1	Y U/UI	Y	ע/טז צ	υ/υι Υ	U/U1	¥ U/U1
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	$\begin{array}{cccccccccccccccccccccccccccccccccccc$	.220 .336 .395 .4463 .4463 .55228 .5567 .5503 .66728 .6680 .7724 .8093 .9955 .8094 .9955 .8094 .9955 .8094 .9955 .8094 .9955 .8094 .9955 .9956 .00000 .000000	$\begin{array}{cccccccccccccccccccccccccccccccccccc$	$\begin{array}{rrrrrrrrrrrrrrrrrrrrrrrrrrrrrrrrrrrr$	$\begin{array}{cccccccccccccccccccccccccccccccccccc$	$\begin{array}{c} .005\\ .007\\ .009\\ .013\\ .013\\ .015\\ .019\\ .025\\ .030\\ .050\\$	.229 .005 .255 .007 .290 .009 .332 .011 .365 .013 .387 .015 .407 .017 .421 .019 .432 .021 .444 .025 .472 .030 .4454 .025 .472 .030 .514 .050 .514 .050 .578 .005 .578 .100 .557 .080 .578 .100 .557 .080 .578 .100 .621 .140 .643 .166 .679 .200 .643 .160 .679 .200 .643 .160 .643 .160 .679 .200 .643 .160 .679 .200 .643 .160 .679 .200 .758 .400 .775 .320 .775 .320 .775 .320 .775 .400 .788 .440 .848 .560 .938 .680 .993 .640 .938 .680 .995 .850 .995 .850 .995 .850 .995 .001 .00 .001 .00	.209 .005 .236 .007 .272 .009 .304 .011 .334 .013 .355 .015 .378 .017 .392 .019 .406 .021 .417 .023 .429 .025 .445 .035 .468 .040 .486 .050 .505 .060 .517 .070 .527 .080 .552 .100 .551 .120 .590 .140 .642 .220 .642 .220 .642 .220 .642 .220 .642 .220 .642 .220 .642 .220 .642 .220 .644 .220 .645 .180 .645 .180 .645 .180 .645 .200 .671 .520 .798 .320 .798 .320 .798 .360 .523 .600 .593 .600 .993 .600 .996 .640 .997 .720 .996 .640 .997 .720 .997 .720 .998 .640 .997 .720 .997 .720 .997 .720 .998 .640 .997 .720 .997 .720 .990 .720 .997 .720 .720 .997 .720 .720 .720 .720 .720 .720 .720 .72	.223 .243 .275 .3031 .3575 .3750 .402 .444 .4569 .5026 .5776 .5626 .6415 .7796 .7796 .7796 .88472 .8977 .99588 .9958 .9958 .9958 .9958 .9957 .0000 1.000	.005 .188 .007 .207 .009 .231 .011 .255 .013 .294 .015 .323 .017 .344 .019 .367 .021 .362 .023 .396 .025 .404 .030 .424 .030 .424 .030 .424 .030 .452 .040 .452 .050 .474 .050 .474 .050 .474 .050 .452 .120 .551 .120 .555 .140 .550 .400 .550 .551 .120 .555 .1400 .5555 .5555 .5555 .5555 .5555 .55555 .55555 .55555 .55555 .555555

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# Velocity Profile Data for Layer with Pressure Distribution II.

X INCH	es froi	4 L.E.	5.6	5	8.3	1	1.5	14.	5	17.4		21.5	25.	.0	28.4	:	31.0	34.	.2
UONE	(FT./8	SEC.)	44.3	38	46.12	4	7.59	48.	86	49.96		51.79	53-	ւ կեր	54.75	1	55.44	55	.41
RE NUM	BER PER	R INCH	2346	53	24158	2	4857	256	52	26151		26945	27	467	28099	:	28454	28	528
INJECT	ION R/	TE	.008	350	.00826	•	00815	.00	804	.0079	7	.00786	.0	0775	.0076	9	.00767	.0	0763
DELTA	STAR(II	iches)	.040	8	.07 <b>99</b>		1273	.15	36	.1770		.2065	.2	208	.2479		.2684	• 3	052
THETA(	INCHES	}	.022	29	.0436		0691	.08	154	.0994		.1185	. 1:	287	.1443		. 1569	.1	741
н			1.77	79	1.834	1	.843	1.7	98	1.782		1.742	1.1	716	1.719		1.711	۱.	753
RE-THE	TA		53	8	1052		1716	21	92	2598		3193	3	535	4053		4463	4	968
X =	5.6	X =	8.3	X =	11.5	X =	14.5	X =	17.4	X =	21.5	X =	25.0	Х =	28.4	X =	31.0	X =	34.2
Y	ប/បា	Y	บ/บ <b>า</b>	Y	บ/บา	Y	υ/υΙ	Y	ប/ប1	Y	υ/υτ	Y	ប/ប1	Y	υ/υι	Y	U/U1	Y	U/U1
$\begin{array}{c} .005\\ .007\\ .009\\ .013\\ .015\\ .017\\ .023\\ .025\\ .025\\ .025\\ .0335\\ .055\\ .0605\\ .070\\ .090\\ .1120\\ .130\\ .220\\ .2400\\ .300\\ .300\\ .300\\ .300\\ .300\\ .220\\ .2400\\ .300\\ $	6577377735922828240152256904775109999900000	$\begin{array}{c} .005\\ .009\\ .013\\ .015\\ .019\\ .025\\ .035\\ .045\\ .055\\ .065\\ .060\\ .090\\ .1120\\ .150\\ .246\\ .246\\ .246\\ .246\\ .346\\ .450$	191799986896812498873355154921438718586088888500000	.005 .007 .009 .011 .013 .015 .020 .025 .030 .040 .035 .050 .050 .050 .050 .050 .050 .05	159 1166 1179 1215 229 3357 4247 5576 5576 5576 4616 9920 129 5576 5576 5576 5576 5576 5576 5576 557	.005 .010 .017 .019 .023 .025 .040 .025 .040 .055 .040 .055 .050 .055 .050 .055 .060 .055 .070 .080 .100 .110 .120 .120 .110 .120 .220 .22	1784254033386806137999738864274288639418594778993686660000 333333334444457555568668589478893689368660000	.005 .010 .017 .019 .021 .025 .030 .040 .035 .040 .055 .050 .055 .060 .070 .055 .050 .070 .055 .050 .070 .07	155 17321 225792 334650 334016554594 55555794669357775000671004429270000 33401655455455555560669735777500067009999991110	$\begin{array}{c} .005\\ .010\\ .017\\ .019\\ .023\\ .025\\ .030\\ .040\\ .035\\ .050\\$	$\begin{array}{c} 150\\ .167\\ .2245\\ .285\\ .285\\ .354\\ .354\\ .430\\ .435\\ .435\\ .555\\ .575\\ .555\\ .575\\ .555\\ .575\\ .575\\ .584\\ .436\\ .436\\ .436\\ .446\\ .4495\\ .555\\ .575$	.005 .017 .017 .017 .023 .025 .035 .040 .035 .050 .040 .050 .050 .050 .050 .050 .05	$\begin{array}{c} 143\\ 2244\\ 307\\ 2246\\ 307\\ 3365\\ 33$	.005 .010 .025 .020 .025 .035 .040 .050 .050 .050 .050 .050 .050 .05	151 162260 23133468 337468 34747 34748 34744	.005 .010 .020 .025 .035 .040 .045 .050 .060 .06	$\begin{array}{c} .55\\ .177\\ .226\\ .2901\\ .3244\\ .33902\\ .4437\\ .447915\\ .5577\\ .55787\\ .647731551\\ .8848\\ .911\\ .99278\\ .9978\\ .9988\\ .9979\\ .9988\\ .9979\\ .9988\\ .000$	.005 .010 .015 .020 .025 .040 .035 .040 .050 .040 .050 .040 .060 .160 .140 .140 .140 .140 .240 .240 .240 .240 .240 .240 .240 .2	.111 .144 .230 .255 .276 .299 .313 .358 .377 .388 .357 .357 .357 .357 .357 .357 .357 .357

# Velocity Profile Data for Layer with Pressure Distribution III.

X INCHI	es fro	M L.E.	5.	3	7.9	1	1.2	14.	2	17.0		21.8	24	.8	28.2		30.8	2).	
U-ONE	(FT./:	SEC.)	59.	82	60.43	e	60.50	62.	52	65.42	2	73.43	82	.03	03.22			بدر ۱۱۱	
RE NUM	BER PEI	R INCH	310	69	31386	3	1518	322	27	33678	3	37867	ь <u>т</u>	718	67616	-	F2005		. yz
INJECT	ION RA	ATE	.00	274	.00271		00289	.00	201	.0038	21	00373		0.62	4/015	, 	23295	51	(091
DELTA S	TAR (II	NCHES)	.02	52	.0399		0568	. 06	72	0707	,	.00312	.0	0403 6=6	.005	13	.00655	•0	0702
THETA()	INCHES	)	.01	65	.0261		0372	. 04	47	01.80		0095	.0	070 1.4e	.0041	-	.0632	.0	0891
н			1.5	24	1.526	1	. 525	1.5	202	1 1/20		1 407	.0	407	.044	r	.0438	.0	0561
RE-THEN	<b>'A</b>		5	14	820		1174	16	цо	1617	,	19-92		411 olut	1.43:	5	1.441	1.	589
									- <b>16.</b> .	1017		1050	1	941	2130	)	2337	3	202
X =	5.3	X =	7.9	X =	11.2	X =	14.2	X =	17.0	X =	21.8	X =	24.8	X =	28.2	X =	30.8	X =	34.2
Y	U/U1	Y	ប/បា	Y	ប/ហ	Y	<b>บ/บ</b> า	Y	ប/បា	Y	U/UI	Y	ប/បា	Y	ע/UI <sup>``</sup>	Y	<b>บ/บ</b> า	Y	U/U1
.005 .006 .007 .008 .009 .012 .014 .018 .025 .045 .035 .045 .050 .045 .050 .045 .050 .045 .050 .045 .050 .060 .110 .120 .120 .120 .300	-4397 -457 -485 -518 -548 -569 -662 -668 -668 -668 -668 -668 -773 -775 -668 -668 -668 -773 -775 -775 -810 -840 -917 -939 -995 -996 -1000 -100 -1000 -1	$\begin{array}{c} .005\\ .006\\ .007\\ .008\\ .009\\ .010\\ .011\\ .012\\ .015\\ .017\\ .019\\ .025\\ .030\\ .040\\ .035\\ .040\\ .050\\ .050\\ .050\\ .050\\ .050\\ .060\\ .100\\ .110\\ .150\\ .160\\ .170\\ .180\\ .220\\ .240\\ .300\\ \end{array}$	•3816 •3816 •447235 •55556 •666877777881836830186 •999999999999999999999999999999999999	.005 .006 .007 .008 .009 .010 .011 .012 .013 .014 .015 .019 .021 .023 .025 .030 .025 .030 .045 .050 .045 .050 .050 .050 .050 .05	3288 3386 3386 3420 3420 3514 5540 5550 5500 5550 5500 50000 5000 5000 5000 5000 5000	.005 .005 .007 .008 .010 .012 .014 .016 .025 .035 .040 .025 .240 .045 .220 .045 .220 .045 .220 .240 .220 .240 .220 .240 .220 .240 .220 .240 .220 .240 .220 .240 .220 .240 .220 .240 .2200 .240 .2200 .240 .2200 .240 .2200 .2400 .2400 .2400 .2400 .2400 .2500 .2400 .2500 .2400 .25000 .2500 .2500 .2500 .25000 .25000 .25000 .25000 .25000 .25000 .25000 .25000 .25000 .25000 .25000 .25000 .25000 .250000 .250000 .250000 .250000000000	.314 3248 3371 .4480 .5556 .6668 .771 .7792 .8889 .9996 .5999 .000 	$\begin{array}{c} .005\\ .006\\ .007\\ .008\\ .010\\ .014\\ .016\\ .025\\ .030\\ .045\\ .050\\ .045\\ .050\\ .045\\ .050\\ .045\\ .050\\ .045\\ .050\\ .045\\ .050\\ .045\\ .050\\ .045\\ .050\\ .045\\ .050\\ .040\\ .025\\ .040\\ .040\\ .025\\ .040\\ .040\\ .025\\ .040\\ .040\\ .025\\ .040\\ .040\\ .040\\ .020\\ .040\\ .020\\ .040\\ .020\\ .040\\ .020\\ .040\\ .020\\ .040\\ .020\\ .040\\ .020\\ .040\\ .020\\ .040\\ .020\\ .040\\ .020\\ .040\\ .020\\ .040\\ .040\\ .040\\ .040\\ .040\\ .050\\$	.319 .33573 .4497 .5545 .5557 .5567 .5567 .5567 .5567 .5567 .5567 .5567 .5567 .5567 .5567 .5567 .5567 .5567 .5668 .5773 .88581 .9921 .9999 .9999000 .1000	$\begin{array}{c} .005\\ .006\\ .007\\ .008\\ .010\\ .014\\ .016\\ .025\\ .030\\ .045\\ .030\\ .045\\ .050\\ .040\\ .025\\ .040\\ .025\\ .040\\ .045\\ .050\\ .040\\ .045\\ .050\\ .040\\ .045\\ .050\\ .040\\ .040\\ .040\\ .020\\ .020\\$	. 359 . 361 . 407 . 500 . 522 . 567 . 588 . 609 . 624 . 663 . 663 . 703 . 720 . 737 . 752 . 886 . 669 . 663 . 703 . 720 . 804 . 825 . 889 . 914 . 825 . 976 . 989 . 916 . 100 1.00	.005 .006 .008 .012 .014 .018 .025 .030 .049 .045 .050 .050 .049 .045 .050 .050 .050 .049 .045 .050 .050 .050 .050 .055 .049 .055 .050 .055 .050 .055 .050 .0555 .055 .055 .055 .055 .055 .055 .055 .055 .055 .055 .055 .055 .055	.3744 .3797599399935 .55555555555555555555555555555	$\begin{array}{c} .005\\ .006\\ .007\\ .008\\ .010\\ .012\\ .014\\ .016\\ .025\\ .030\\ .045\\ .050\\ .045\\ .050\\ .045\\ .050\\ .045\\ .050\\ .045\\ .050\\ .045\\ .050\\ .045\\ .050\\ .045\\ .050\\ .045\\ .050\\ .040\\ .120\\ .240\\$	.357 378 .4022 .4489 .55241 .5583 .6653 .6699 .7757 .88250 .9900 .9900 .9900 .9900 1.000	.005 .006 .007 .008 .010 .012 .016 .016 .016 .025 .030 .040 .040 .040 .045 .050 .040 .045 .050 .040 .04	37332 3802398 442398 552888 557565 663884 6690355777738 8857644487 8924879999 99927999000 1.000	$\begin{array}{c} .005\\ .006\\ .007\\ .008\\ .010\\ .012\\ .016\\ .025\\ .050\\ .045\\ .050\\ .060\\ .000\\ .012\\ .016\\ .025\\ .050\\ .045\\ .050\\ .000\\ .000\\ .120\\ .022\\ .020\\$	.256 .265 .305 .338 .305 .384 .401 .414 .453 .513 .545 .513 .545 .573 .505 .573 .505 .573 .505 .573 .515 .573 .505 .573 .515 .573 .505 .573 .515 .573 .515 .573 .505 .573 .515 .573 .515 .573 .515 .573 .555 .573 .555 .573 .555 .573 .555 .573 .555 .575 .57

# Velocity Profile Data for Layer with Wall Position Determined Electrically; $U_1 = 30 \text{ ft/sec.}$

X INCH	es fro	DM L.E.	31	.0	31.	.0	31.0	0	31.0		31.0		31.C	3.	1.0	31.	0	31.0	I	31.0		31.0	3	
U-ONE	(FT.,	/sec.)	31	.25	31.	36	31.6	53	32.19	5	31.38	:	30.71	31	1.23	31.	02	31.6	7	31.06		31.06	30	0.95
RE NUN	BER PI	ER INCI	E 16	600 JL	160	96	1642	20	1658	5	16450		16020	16	6410	162	51	1649	8	16130		16105	10	5043
INJECT	ION P	RATE		0312	.00	404	• 002	176	.0051	1	.00664	<b>.</b> .	.00798		00905	.01	019	.011	11	.0122	7	.01336		01428
DELTA	STAR()	(NCHES)	).1	921	.23	50	.255	3	• 301 <sup>1</sup>	ŀ	.3332		4787	•:	5448	.64	73	.706	7	.8036		.8934	•	9650
THETA(	INCHES	5)	.1	205	.14	36	.152	20	.1724		.1849		2357	.2	2570	.28	55	. 302	0	. 7230		. 3413		3557
н			1.	594	1.6	37	1.68	80	1.748	3	1.602		2.031	2.	120	2.2	67	2.34	0	2.488		2.618	2	713
RE-THE	TA		1	976	23	11	249	5	2859	,	3042		3776	1	e18	کیل	ш1	209	- h	5210		5.06	-	: 706
								-			<b>3</b>		5175		2.0			490	0	1210		J490		5700
Y	ប/បា	Y	ប/បា	Y	ប/បា	Y	ບ/ຫ	Y	U/U1	Y	ប/បា	Y	ប/បា	Y	U/U1	Y	U/U1	Y	บ/บา	Y	U/U1	Y	ប/ហ	
.005	.177	.005	.150	.005	.138	.005	.120	.005	.109	.005	.068	.005	.067	.005	*	.005	*	.005	*	.005	*	.005	*	
.015	.273	.015	.245	.015	.214	.020	181	.015	.159	.020	162	.040	.164	.020	.123	. 100	.121	.050	.096	.050	.068	.050	.088	
.020	.341	.020	.295	.020	.266	.025	.262	.020	.204	.040	197	.060	.201	.060	.156	.150	.219	.150	.175	.150	.141	.150	.124	
.030	.411	.030	.367	.030	-339	.040	.334	.040	.298	.060	.240	.100	.253	.100	.206	.250	.240	.200	.207	.200	.199	.200	.152	
.035 .0k0	-432 hho	.035	.387	.035	• 366 280	.050	·359	.050	·324	.070	.255	.120	.273	.120	.220	.300	. 306	. 300	.256	. 300	.224	. 300	.200	
.045	464	.045	424	.045	.393	.070	.396	.000	.344	.100	.207	. 140	.209	.160	.249	.350 .400	. 331	-350 . 400	-282	-350 hoo	.247	· 350	.222	
.050	.476	.050	433	.050	.406	.080	.411	.080	.375	.120	305	.200	.328	.240	.296	450	.386	.450	. 332	.450	.292	.400	.263	
.055	466	+060 -070	.455	.060	.425	.090	-426 haß	.100	.404	.160	.341	.240	.356	.280	.321	.500	.410	. 500	.356	. 500	.317	• 500	.286	
.070	.514	.080	485	.080	455	.120	457	.140	. 421	.200	· 374	.200	.382 . Jun 7	- 320	. 344	-550	.436	• 550	- 383	.550	.338	.550	.306	
•080	530	.090	. 497	.090	. 470	.140	472	160	459	.280	428	.360	430	.400	.389	.650	.494	.650	.433	.650	. 391	. 650	. 355	
.090	.541	.100	.509	.100	.484 Fol	.160	- 490	.180	475	.320	. 452	.400	. 455	. 440	.412	.700	. 524	.700	. 457	.700	. 414	.700	.376	
.120	.573	.140	547	.140	.523	.200	.500	.200	.491	• 360	+477	.440	.478	.480	• 435	.800	.576	.800	.509	.800	.462	. 750	400	
.140	.592	.160	565	.160	540	.220	.537	.280	. 551	.440	.524	.520	.524	.560	480	1.00	.678	1.00	.618	1.20	.660	1.00	.424	
.160	.611	.200	-599	.180	.556	.240	• 553	-320	.577	.480	.548	.560	. 546	.600	. 500	1.20	.783	1.20	.718	1.40	.762	1.20	. 620	
.300	.723	.400	.739	.300	.647	. 300	. 665	.400	.032	+520	•573	.600	.572	.640	• 525	1.40	.875	1.40	.815	1.60	.856	1.40	.718	
.400	792	. 500	. 802	.400	.715	.500	.732	.600	.755	.700	682	,800	.689	.800	.615	1.80	.989	1.80	.904	2.00	. 929	1.80	.809	
.500	.855	.600	.856	.500	· 779	.600	.788	. 700	.816	• 800	.742	• 900	. 751	.900	.669	2.00	1.00	2.00	. 996	2.20	1.00	2.00	.961	
.700	.910	.700	.912	.600	.836	.700	. 841 80k	.800	. 865	.900	• 797	1.00	.806	1.00	•723	2.20	1.00	2.20	1.00	2.40	1.00	2.20	.992	
.800	.987	.900	.979	.800	.939	.900	. 945	1.00	.951	1.10	.054	1.20	. 098	1.20	.826			2,40	1.00			2.40	1.00	
.900	1.00	1.00	• 996	.900	.974	1.00	.975	1.10	. 989	1.20	. 944	1.60	.993	1.60	.973							2.00	1.00	
1.00	1.00	1.10	1.00	1.00	.993	1.10	.989	1.20	1.00	1.30	968	1.80	1.00	1.80	. 996									
		1.30	1.00	1.30	1.00	1.20	· 996	1.30	1.00	1.40	.984	2.00	1.00	2.00	1.00									
				1.50	1.00	1.50	1.00		1.00	1.60	1.00			2,20	1.00									
				•		1.70	1.00			1.70	1.00													

indicates that velocity measurements were uncertain.

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# Velocity Profile Data for Layer with Wall Position Determined Electrically; $U_1 = 50$ ft/sec.

X INCH	es froi	M L.E.	31.0	D C	31.0	3	1.0	31.	0	31.0		31.0	31.	0	31.0		31.0
U-ONE	(FT./	SEC.)	51.	47	52.01	5	1.73	51.	83	51.74	!	51.7B	51.	74	51.85		51.56
RE NUN	ober pei	R INCH	265	+5	26822	2	6632	267	65	26636	:	26499	267	'89	26762		26614
INJECT	ION R	ATE	.00	27 <sup>8</sup>	.00369	, .	00491	.00	544	.0063	4	.00699	.00	951	.0118	8	.01449
DELTA	STAR(I	nches)	.16	B9	.1969	•	2622	.28	22	.3320		. 3695	• 55	16	. 7905		1.2074
THETA	INCHES	)	.10	34	.1221		1514	.15	98	.1796		. 1933	.24	99	.3071		•375 <sup>4</sup>
н			1.5	57	1.613	1	.732	1.7	66	1.849		1.911	2.2	207	2.574		3.216
RE-THE	TA		28	78	3274		4031	42	78	4783		5123	66	95	8219		9991
Y	ប/ប1	Y	บ/บ1	Y	ט/טו	Y	ប/បា	Y	U/U1	Y	U/U1	Y	บ/บ1	Y	<b>บ/บ</b> 1	Y	บ/บ <b>า</b>
$\begin{array}{c} .005 \\ .006 \\ .007 \\ .008 \\ .009 \\ .011 \\ .013 \\ .016 \\ .022 \\ .024 \\ .022 \\ .033 \\ .049 \\ .059 \\ .067 \\ .089 \\ .099 \\ .0$	2051 2211 22375 2912 2912 2912 2912 2912 2912 2912 291	$\begin{array}{c} .005\\ .007\\ .008\\ .009\\ .010\\ .011\\ .012\\ .013\\ .014\\ .015\\ .016\\ .017\\ .019\\ .023\\ .025\\ .035\\ .040\\ .045\\ .055\\ .050\\ .045\\ .055\\ .050\\ .055\\ .050\\ .055\\ .050\\ .050\\ .060\\ .090\\ .100\\ .140\\ .225\\ .300\\ .450\\ .500\\$	18913773773804708850458851111997288145557551302322985018208806689480000	$\begin{array}{c} .005\\ .007\\ .009\\ .011\\ .013\\ .015\\ .017\\ .023\\ .025\\ .030\\ .045\\ .050\\ .040\\ .050\\ .040\\ .050\\$	1386 14576 22465 29333 23335 244798 337798 344244 555556 260746 263097 1099752 2666988 37798 399990000 1000	$\begin{array}{c} .005\\ .007\\ .009\\ .011\\ .013\\ .015\\ .017\\ .019\\ .023\\ .025\\ .035\\ .040\\ .045\\ .050\\ .040\\ .035\\ .040\\ .045\\ .050\\ .040\\ .080\\ .090\\ .045\\ .050\\ .040\\ .080\\ .090\\ .090\\ .080\\ .090\\ .080\\ .090\\ .090\\ .080\\ .090\\ .000\\$	$\begin{array}{c} 126\\ 13499\\ 1952\\ 2267\\ 2003\\ 33350\\ 33350\\ 33350\\ 33350\\ 33350\\ 33350\\ 33350\\ 33350\\ 33350\\ 33350\\ 3355\\ 3555\\ 5575\\ 36641\\ 815\\ 775\\ 8144\\ 301\\ 775\\ 8144\\ 301\\ 755\\ 9999\\ 9990\\ 000\\ 000\\ 000\\ 000\\ 000\\$	.005 .007 .009 .011 .013 .015 .017 .019 .021 .023 .025 .030 .040 .045 .050 .050 .050 .050 .050 .05	$\begin{array}{c} . 103 \\ . 124 \\ . 177 \\ . 223 \\ . 234 \\ . 234 \\ . 234 \\ . 234 \\ . 234 \\ . 334 \\ . 334 \\ . 334 \\ . 445 \\ . 553 \\ . 559 \\ . 669 \\ . 769 \\ 119 \\ . 999 \\ . 999 \\ . 999 \\ . 999 \\ . 000 \\ 0 \end{array}$	$\begin{array}{c} .005\\ .007\\ .009\\ .011\\ .013\\ .015\\ .017\\ .019\\ .023\\ .025\\ .030\\ .045\\ .050\\ .040\\ .045\\ .050\\ .040\\ .045\\ .050\\ .040\\ .045\\ .050\\ .040\\ .045\\ .050\\ .040\\ .045\\ .050\\ .060\\ .070\\ .080\\ .045\\ .050\\$	$\begin{array}{c} .8958\\ .1022\\ .11460\\ .11400\\ .$	.005 .010 .015 .020 .025 .030 .035 .040 .050 .050 .050 .050 .050 .050 .05	* * .0743 .0793 .1237 .1201 .22568 .2309 .3314 .449 .5494 .5494 .5499 .9936 .99576 .99576 .99970.00	.005 .010 .015 .020 .030 .040 .050 .060 .120 .120 .120 .120 .120 .120 .120 .12	* * * .061 .083 .083 .1128 .1455 .2295 .3250 .4272 .5405 .5629 .7792 .8886 .9953 .9993 .9993 .9993 .9991 .000	.005 .020 .060 .100 .250 .350 .400 .450 .400 .450 .400 .450 .400 .450 .400 .450 .400 .450 .400 .450 .400 .40	* * * * * * * * * * * * * * * * * * *

\* indicates that velocity measurements were uncertain.

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# Velocity Profile. Data for Layer with Discontinuous Distribution of Injection.

X INCHES F	ROM L.E.	11.50	14.50	16.40	17.40	17.60	17.85	18.35	19.10	21.50	25.00	28.40	31.00	34.20
U-ONE (FT	./SEC.)	147.90	148.92	149.64	150.44	149 <b>.8</b> 6	149.72	149.23	148.56	148.49	148.88	148.39	148.25	146.30
RE NUMBER	PER INCH	75289	75810	76078	76483	76754	76479	76232	<b>7</b> 5788	75654	75722	75144	75629	74732
INJECTION	RATE	.00341	<b>.0</b> 0339	.00337	.00336	0	0	.00010	.00010	.00010	.00010	.00010	.00010	.00010
DELTA STAR	(INCHES)	.0639	.0805	.0929	.0976	.0979	.0979	.0989	.0995	.1013	. 1033	.1134	.1171	. 1237
THETA (INCH	es)	.0396	.0506	.0580	.0610	.0613	.0618	.0634	.0648	.0685	.0722	.0797	.0833	.0891
н		1.614	1.591	1.601	1.601	1.597	1.583	1.560	1.537	1.480	1.432	1.423	1.406	1.389
RE-THETA		2982	3836	կեր1 ի	4662	4706	4730	4833	4908	5179	5464	5986	6300	6655
¥ -	11 50	14 50	16 ko	17 40	17.60	17	85	18 35	19.10	21.50	25.00	28.10	31.00	sh ou
v ~		14. 50	10.40		1,100		•	1.7.11	1/11	11/m	11/11	11/111	J1100	11/119
1	0/01	0,01	0/01	0/01	0/01	0/0	~	0,01	0/01	0,01	3/01	0/01	0/01	0/01
.005	.320 .326	.321	.288 .296	.278	.200	.30	6	• 335 • 345	• 342 • 350	.301	.309	.357	• 302 • 372	.400
.007 .003	•337 •350	· 339 • 358	.312 .329	• 303 • 322	. 305 . 324	.31	2	•357 •376	.370 .389	.396 .418	.404	. 388	. 417	. 439
.009	-371	.376	• 347	• 338	.344	• 36	4	-395	.410	.442	.453	.436		
.010	.389	.392	. 364	• 356	.362	. 38	4	.411	.429	-459	.472	.459	.466	. 477
.012	- 420	.410	.389	.362	.390	.41	4	- 437	• 455	.485	.501	.480	•495	.502
.014	.444	.439	.409	.402	.409	• 43	2	1,454	+471	.500	.520	.500	• 514	.522
.018	.400 h7h	.450	-423 haß	•41 ( h21	.423	•44 bs	6	• 404 Juzh	-403 hos	.712	• 232 6 li 2	-219	- 221	- 734
.020	• 4 (4 h8s	h75	.430	1000	.434	• 47	3	180	• 495	.722	· 742	· 529	- 550	• 743
.025	.511	496	.473	466	հեր	.19	0	105	515	545	.570	• 557	564	567
.030	.533	.514	491	485	485	. 49	ă –	.509	.528	.557	.581	570	.579	. 580
.035	-552	528	.506	.501	.502	. 50	5 7	.521	540	568	.593	.583	.590	. 591
.040	.567	.543	519	.513	.515	.52	ċ .	.533	548	.579	.603	.596	.601	.602
.045	.582						-		••••			• • • • •		1002
.050	.597	.569	.546	.541	.540	. 54	3	• 553	.566	• 597	.621	.614	.617	.619
.060	. 623	. 592	.569	.561	.562	• 56	4	.570	.582	.612	.636	.630	.633	.635
.070	.651	.614	.590	• 583	. 584	.58	5	.587	- 597	.625	.647	. 644	.646	.651
•080	.677	. 633	.609	. 603	.603	. 60	3	.603	.611	.637	.660	.654	.658	.661
.090	.700	.654	.628	.620	.621	.62	1	.619	.625	.648	.671	.665	.669	.671
.100	. 724	.673	.645	•638	.637	• 63	Ţ	.634	.640	.659	.680	.676	.680	. 681
.125	•779	.718	.687	.078	.678	.67	D 1.	.673	.674			/		
175	- 030 976	- 701	• (21	.710	.110	• 71	4	- 71	• 709	•715	. 728	. 722	- 722	. 722
-200	016	841	. 001 . ·	• 124	- 174	• 15 78	0 2.	770	* (41	768	771	761	760	759
.225	.952	.878	.836	. B22	. 820	. 81		.810	- 175	. 100	• ( ( )	• 101	. 105	• 170
.250	.976	.912	.869	.852	.850	84	ģ.	.840	.833	820	814	700	706	787
.275	.992	941	.897	. 882	.881	.87	à	.869	.863	.020	.0.4	• 199	. 190	• 101
.300	998	.963	925	.910	.909	.90	7	.897	.890	. 870	. 855	834	807	817
.325		.983	.950	. 936	.933	.93	ź	923	.916	1010	,	•••••		1011
.350	1.00	• 993	.971	• 957	.955	. 95	2	.946	. 940	.915	. 893	. 869	. 860	.847
• 375			. 984	• 973	• 973	• 97	1	.965	• 957		,			
.400	1.00	• 999	• 993	•986	.985	.98	4	.980	.975	• 953	. 929	.901	. 890	.874
. 425				• 994	• 994	• 99	3	.990	.986					
• 450	1.00	1.00	• 999	• 997	• 997	• 99	6	. 998	• 993	• 980	. 960	. 931	.918	. 900
.500		1.00	1.00	1.00	1.00	• 99	9	. 999	• 999	• 995	. 981	. 958	• 944	. 924
- 220		1.00	1.00	1.00	1.00	1.0	0	1.00	1.00	• 999	.993	.977	. 965	- 949
.000			1.00	1.00	1.00	1.0	0	1.00	1.00	1.00	. 998	•990	• 980	. 966
.070						1.0	U .	1.00	1.00	1.00	1.00	• 997	. 991	• 980
750										1.00	1.00	• 999	• 997	• 991
- 190											1.00	1.00	• 999	• 997
.850												1.00	1.00	.999
.900												1.00	1 00	1/00

### TABLE IV

### Measurements of Gross Convergence or Divergence Using the Wake-Traverse Method.

$$v_0/U_1 = 0, U_1 = 50 \text{ ft/sec}, \text{ Zero pressure gradient } (h = 3 \text{ in.}):$$

Method calculation (see below)	<i>x</i> <sub>0</sub> ft	α (Angle of convergence or divergence), degrees	$\frac{\theta}{x_0 - x}$	Possible error in $d\theta/dx$ per cent
Α	±120	±0.06	$\pm 3 \times 10^{-5}$	$\pm 1.4$
В	+ 81	+ 0.09	$+7 \times 10^{-5}$	+ 3.8
С	± 280	+0.03	$\pm 2 \times 10^{-5}$	$\pm 1.1$

 $v_0/U_1 = .008, U_1 = 50 \text{ ft/sec}$ , Zero pressure gradient (h = 6 in.):

A	±240	$\pm 0.06$	$\pm 4 \times 10^{-5}$	$\pm 0.5$
В	+ 107	+0.14	$+19 \times 10^{-5}$	+ 2.4
С	+156	+0.09	$+13 \times 10^{-5}$	+1.6

*Pressure distribution III* (h = 6 in.):

А	± 240	$\pm 0.06$	$\pm 1.7 \times 10^{-5}$	<u>+</u> 3·4
В	± 320	$\pm 0.05$	$\pm 1.2 \times 10^{-5}$	$\pm 1.3$
С	± 560	±0.03	$\pm 0.7 \times 10^{-5}$	<u>+</u> 2·4

Notes: A Calculation using wake separations at  $x_1 = 12$  in. and cylinder separation; B Calculation using wake separations at  $x_1 = 12$  in. and  $x_1 = 28$  in.;

- C Calculation using wake separation at  $x_1 = 28$  in. and cylinder separation.

Sign Convention:  $x_0$  (or  $\alpha$ ) positive indicates convergence to a virtual origin downstream with  $d\theta/dx$  greater than that from the two-dimensional momentum integral equation by the indicated amount.

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				_							
x inches from leading edge	11.5	14:	5	17·4	21.5	25.0	28-4	1	31·0	34-2	4 per cent of $d\theta/dx$
$v_0/U_1 = 0, U_1 = 50$ ft/sec Zero pressure gradient	0.0022	0.002	0.0021 0		0.0020	0.0019	0.001	9 0	0019	0.0018	0.00008
$v_0/U_1 = 0, U_1 = 150$ ft/sec Zero pressure gradient	0.0017	0.001	.6 0	·0016	0.0015	0.0015	0.001	4 0	0014	0.0013	0.00006
$v_0/U_1 = .0017, U_1 = .50 \text{ ft/sec}$ Zero pressure gradient	0.0014	0.001	3 0	•0013	0.0012	0.0012	0.001	1 0.	0010	0.0010	0.00012
$v_0/U_1 = 0032$ , $U_1 = 50$ ft/sec Zero pressure gradient	0.0009	0.000	8 0.	0007	0.0007	0.0006	0.000	5 0.0	0005	0.0004	0.00015
$v_0/U_1 = 0046$ , $U_1 = 50$ ft/sec Zero pressure gradient*	0.0006	0.000	0.0005 0.1		0.0004	0.0003	0.000	2 04	0002	0.0003	0.00019
$v_0/U_1 = .008$ , $U_1 = .50$ ft/sec Zero pressure gradient	0.0003	0.000	0.0003 0.000		0.0003	0.0003	0.000	3 0.0	0003	0.0003	0.00034
$v_0/U_1 = 0032$ , $U_1 = 150$ ft/sec Zero pressure gradient	0.0007	0.000	7 0.	0006	0.0006	0.0005	0.000	5 00	0005	0.0004	0.00015
$v_0/U_1 = .008, U_1 = 150$ ft/sec Zero pressure gradient Less than 0.0001 0.00033											
Pressure Distribution I	0.0015	0.001	4 0.	8000	0.0008	0.0008	0.000	5 0.0	8000	0.0004	0.00020
Pressure Distribution II	0.0010	0.000	3 (	0	-0.0003	-0.0005	-0.000	01 0.0	0005	0.0013	0.00022
x inches from leading edge	11-2	14.2	17.0	<b>b</b>	21.8	24.8	24.8 28.2		3	34.2	
Pressure Distribution II	0.0006	0.0008	3 0-0	0008	0.0008	0.0008	0.000	5 0.0	003	0.0007	0.00003
	[······	·	<u> </u>	<del></del>				· · · · · · · · · · · · · · · · · · ·	T		
x inches from leading edge	11.5	14.5	16.4	17.4	19-1	21.5	25.0	28.4	31.0	34.2	0.00010
Layer with Discontinuity in $v_0^*$	0.0003	0.0005	0.0003	0-0002	2 0.0012	0.0010	0.0015	0.0014	0.0012	0.0010	0.00010

\*In both these layers, the small pressure gradients present have been taken into account. For the layer with a discontinuity in  $v_0$ , the values of  $c_f/2$  for x = 17.6 in., 17.85 in. and 18.35 in. are uncertain and are not quoted.



FIG. 1. Sectional Plan of tunnel working section.

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• • •



Test wall before attachment of porous sheet



Detail of adhesive joint

FIG. 2. Supporting arrangement for porous wall.



'Vyon' Sintered Polythene





# 'Porosint' Sintered Bronze





# 'Poroloy' Stainless Steel Wiremesh

0.005 in SCALE 0.05 in HORIZONTAL 0.001 in VERTICAL

FIG. 3. Comparison of 'Vyon' with alternatives.



FIG. 4. Microphotograph of 'Vyon' taken on the Cambridge University scanning electron microscope.



FIG. 5. Apparatus used to measure variation of porosity along porous sheet.



FIG. 6. Variation of  $v_0$  along centreline of test wall.









A = Flow	Rate for Layer wi	ith $V_{0/U_1} = .0017$ , $U_1 = 50$ ft./sec.
B =	do.	Pressure Distribution I
C =	do.	V <sub>0/U1</sub> =·0032, U1=50ft./sec.
D =	do.	Vg( <sub>U1</sub> = ·0046, U1= 50 ft./ sec.
E =	do.	{\V_1=-008, U1=50 ft./ sec. Pressure Distribution II

FIG. 10. Comparison of streamlined entry with orifice plate.



FIG. 11. Examples of velocity distributions.



FIG. 12. A typical result of two-dimensionality tests.



FIG. 13. Comparison of zero injection profiles with inner region profile family (Clauser chart).



FIG. 14. Comparison of calculated momentum developments with experiment.







FIG. 16.  $c_f/2$  vers.  $R_{\theta}$  for zero injection data.



FIG. 17. Variation of sublayer thickness with  $v_0/U_1$  and  $c_f$ .



FIG. 18. Spanwise variation of wall pitot pressure at x = 32 in.







FIG. 22. Effect of sealing strip on velocity profile near the wall.



FIG. 23. Experimental velocity distribution.

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