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Compressible Turbulent Boundary Layers with Combined Air Injection and Pressure Gradient

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Summary

The purpose of the work described in this report was to study the effect of longitudinal pressure gradients upon compressible turbulent boundary layers on a flat plate, with and without air injection. A brief survey of some of the more recent work on pressure gradient flows with and without injection is given. Emphasis is placed upon the effects of the pressure gradients on the velocity and temperature profiles although theoretically predicted developments are indicated on the figures. The use of the razor-blade technique for measuring skin-friction in pressure gradient flows is also shown to be very satisfactory.

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LIST OF CONTENTS

- 1. Introduction
- 2. A Review of Earlier Work
 - 2.1. Pressure Gradient Flows Without Injection
 - 2.2. Pressure Gradient Flows With Air Injection
- 3. Experimental Equipment and Test Procedure
 - 3.1. Wind Tunnel
 - 3.2. The Design of the Pressure Gradients
 - 3.3. Injection
 - 3.4. Probes
 - 3.5. Test Procedure
 - 3.6. The Reduction of the Experimental Data
- 4. The Skin-Friction Coefficient
 - 4.1. The Measurement of Skin-Friction for Zero Injection
 - 4.2. An Estimation of Skin-Friction for Injection
- 5. The Comparison of the Present Results with Two Prediction Methods
- 6. Discussion of the Boundary-Layer Profiles
 - 6.1. The Velocity Profiles
 - 6.2. A Comparison of Velocity Profiles in Pressure Gradients with Injection
 - 6.3. The Temperature Profiles
 - 6.4. Boundary-Layer Relations in the Inner and Outer Layers
 - 6.4.1. The inner region 6.4.2. The outer region
 - 6.5. General Comments
- 7. Concluding Remarks

Acknowledgements

List of Symbols

References

Tables 1 and 2

Illustrations-Figs. 1 to 42

Detachable Abstract Cards

1. Introduction

This report gives the results of a series of experiments to study compressible turbulent boundary layers over porous surfaces with air injection, in the presence of both favourable and adverse pressure gradients. The tests were made in the same tunnel as used by Jeromin,¹ Squire² and Dunbar³ and were made in parallel with work by Marriott⁴ who studied the compressible turbulent boundary layer over a flat plate with discontinuous changes in injection rate.

The present results were obtained on a flat surface with the pressure gradient obtained by modifying the downstream end of a $M_1 = 2.5$ liner, so that a linear increase or decrease in Mach number was produced over the test plate. In each case the region of linear Mach-number gradient was about 150 mm and the initial boundary-layer thickness without injection was about 6 mm. Two favourable gradients where the Mach number increased from about $M_1 = 2.55$ to $M_1 = 3.0$ and 3.2 respectively and an adverse gradient where the Mach number decreased from $M_1 = 2.55$ to 2.2, were obtained. The actual gradients obtained varied slightly when the injection rate changed.

For each gradient, velocity and temperature profiles were measured at 25 mm steps along the test plate for various injection rates. These profiles are tabulated at the end of the report. In addition skin friction, in the absence of injection, was measured by the razor-blade technique.

The purpose of the programme was twofold; firstly to study the effects of pressure gradients on layers with injection and secondly to use the results as test cases for two prediction methods. One was the method of Verma⁵ which used a finite difference scheme to solve the momentum and enthalpy equations using an eddy-viscosity model and a constant turbulent Prandtl number. The other was a direct modification of the Bradshaw–Ferriss^{6,7} method by the present author. This method solves the turbulence energy equation and since it assumes that the temperature profile is related to the velocity profile by a Crocco relation, a supplementary purpose of the work was to check the accuracy of this relationship for the complex flows studied here.

In this report the emphasis will be placed on the effects of the pressure gradients and the velocitytemperature relation. A full comparison with the two prediction methods will be presented in a joint report with P. G. Marriott, where the performance of both methods will be assessed in relation to the non-equilibrium flows studied here and those studied by Marriott. However, many of the experimental results presented here are compared with the two prediction methods in the figures.

2. A Review of Earlier Work

There is very little profile data for boundary layers with fluid injection measured in strong pressure gradients in incompressible flow and to the author's knowledge no previous data for compressible boundary layers, although some boundary layers which have been studied have been influenced by upstream pressure gradients. There are now several reviews available for fluid injection into constant pressure flows and the present review will therefore consider pressure gradient flows without air injection briefly and pressure gradient flows with injection in more detail. A very full review of constant-pressure flows with air injection and pressure-gradient flows with or without injection is given by Thomas.⁸

2.1. Pressure Gradient Flows Without Injection

Many of the pressure gradient data along flat surfaces at low speeds have been analysed by Coles and Hirst⁹ who found that most of the data were well represented by the law of the wall, $u/U_{\tau} = 1/k \log y^+ + B + (\pi/k)w(y/\delta_c)$ and a velocity defect law, $(U_1 - u)/U_{\tau} = f(y/\delta)$. Clauser¹⁰ formed a dimensionless-pressure-gradient parameter $\beta = (\delta_i^*/\tau_w)(dp/dx)$ which was nearly constant along his equilibrium adverse-pressure-gradient flows. The wake parameter π appeared to be closely connected with β .

A method which predicts the velocity defect family throughout the boundary layer for $\beta \ge -0.5$ is that of Mellor and Gibson.¹¹ They also use $U_p = U_{\tau}\beta^{\frac{1}{2}}$ instead of U_{τ} to non-dimensionalise the velocity defect since this gave a better collapse for large β . The predicted velocity defect and shear-stress distributions agree exceptionally well with the profiles of Clauser for $\beta = 1.8$ and 8.0 and those of Herring and Norbury¹² for $\beta = -0.35$ and -0.53.

The zero skin-friction flow of Stratford¹³ did not follow the trend of general agreement with the inner law and velocity-defect law, when analysed by Coles and Hirst. However, when compared with the theory of

Mellor and Gibson the velocity defect is predicted very well when non-dimensionalised by U_p instead of U_r .

Investigations of pressure gradients in compressible flows are often incomplete in their collection of data such as temperature and static-pressure variations through the boundary layers. Pressure gradients produced on ramp models are subject to large static-pressure variations through the boundary layers. Threedimensional influences such as end effects in two-dimensional flows or convergence and divergence along cylindrical flows are often neglected when they should not be.

An investigation of adverse and favourable pressure gradients, where complete measurements were made, was performed by Lewis, Gran and Kubota.¹⁴ The boundary layer grows on the inside of a large radius cylindrical shell with a centre body producing the pressure gradient. The static pressure was constant through the boundary layer to within ± 10 per cent and the Crocco¹⁵ temperature relation was verified to within experimental accuracy. It would appear that except where the boundary layer changes rapidly from $\beta = 1.5$ to -0.8 the velocity profiles are in near equilibrium conditions. The profiles in the adverse gradient show reasonable agreement with the wake function of Coles.¹⁶ The velocity defects for the adverse gradient collapse for the same values of β with the incompressible curves of Coles and Hirst.

Boundary layers under the influence of imposed pressure gradients along flat plates have been studied by Michel, Quemard and Elena;¹⁷ Sivasegaram,¹⁸ and Voisinet, Lee and Yanta.¹⁹

Michel *et al.* produced their favourable pressure gradient with the least magnitude by modifying the rear of a linear in a smooth curve, while the two stronger gradients were caused by a single expansion corner on the liner. The profiles seem to show some signs of relaminarisation and the logarithmic velocity profiles do not bear linear characteristics. There is a large overshoot of velocity in the inner region and negligible wake component if indeed it is not negative.

Both Sivasegaram and Voisinet *et al.* have used flexible tunnel walls to produce their pressure gradients. Sivasegaram's three pressure gradients commence with strong favourable pressure gradients and it was thought that the boundary layers were not fully turbulent at the start of the gradients. The velocity profiles predicted by both the Patankar–Spalding²⁰ and Bradshaw–Ferriss methods do not agree well with the experimental profiles, even in the fully turbulent flow, until the gradient has been reduced almost to zero after 600 mm.

Voisinet *et al.* have taken comprehensive measurements in an adverse-pressure-gradient flow. Staticpressure and total-temperature measurements are taken through the layer. The static pressure variation is less than 5 per cent and often nearly constant. The temperature variation agreed better with that of $Walz^{21}$ than that of $Crocco^{15}$ but a noticeable discrepancy with Walz was the inflection at the edge of the sublayer. There was no observed overshoot in the stagnation temperature at the edge of the boundary layer.

The boundary layers measured were between 40 mm and 80 mm thick, consequently the traverses went well into the sublayer where viscous-flow interaction and probe-wall interference were encountered and allowed for. A velocity-profile family using the sublayer law, $u^+ = y^+$ and inner law with Coles' wake function $u^+ = 1/k \log y^+ + B + (\pi/k)w(y/\delta_c)$, agreed exceptionally well with experiment.

Three theoretical prediction methods which solve the boundary-layer partial-difference equations directly are those of Bradshaw and Ferriss; Patankar and Spalding, and Cebeci and Smith.²²

The theory of Bradshaw and Ferriss has been comprehensively compared with pressure-gradient flows for zero heat transfer by Bradshaw and Ferriss^{6,7} and Sivasegaram and Whitelaw.²³ The theory of Patankar and Spalding has also been compared with experiment in the last reference.

Cebeci²⁴ has published a comparison with the data of Pasiuk, Hastings and Chatham²⁵ for pressure-gradient flow and the overall agreement for velocity and temperature profiles, δ^* and θ is quite reasonable. The predictions of the other two methods mentioned, for this data, are very similar to that of Cebeci and Smith.

From the previous comparisons it is clear that there is very little data in pressure-gradient flows which is suitable for a comprehensive comparison with two-dimensional theories. The majority of experimental flows at the present time is subject to:

(1) A lack of complete experimental measurement; noticeably the static pressure and temperature traverses through the boundary layer, and unreliable skin-friction coefficients.

(2) Considerable three-dimensional effects, such as end effects, longitudinal curvature or lateral convergence and often a combination of two or more.

(3) The presence of laminar characteristics or influence of upstream pressure gradients persisting along the measured development.

For boundary layers not subject to the above, or only mildly so, the theories in general predict developments which agree very well with experiment.

2.2. Pressure Gradient Flows with Air Injection

The first thorough investigation was performed by McQuaid²⁶ who measured boundary-layer velocity profiles in both favourable and adverse pressure gradients, for incompressible flow. He also showed that a velocity defect law could be formed to include both injection and pressure gradient.

Similar work has been repeated by Julien²⁷ and Loyd²⁸ for stronger favourable pressure gradients. Whereas the injection rates of McQuaid varied along the pressure gradients, those of the above two studies were supposed to be constant. In practice the blowing rates were not kept constant and asymptotic flows with constant R_{θ} and C_{f} could not be achieved. Neither of the two investigations measured enough profiles to calculate the corrections to C_{f} . The boundary layers of Julien tended towards full development at the end of the pressure gradient whereas those of Loyd were at no time close to developed conditions. In practice the best estimates of C_{f} , for all the flows, were obtained by either fitting velocity profiles to sublayer laws which depends upon the smoothness of data near the wall, or by using a logarithmic region method. Neither of these methods provided values of C_{f} better than ± 20 per cent.

The comparison between the theoretical predictions using the Patankar-Spalding method, and the experiments of Julien shows that although there is considerable scatter in C_f the probable discrepancy is on the whole not as large as ± 20 per cent in the pressure gradient region. In the developing flow to and from the pressure gradient larger discrepancies occur. For the relaxing flow after the strongest pressure gradient, the θ development is consistently over-predicted by the order of 25 per cent, whereas the H development is reasonably predicted. It is therefore probable that, for the experimental values of R_{θ} given, the theory would predict considerably lower values of C_f in the relaxation development. It also implies that the velocity profiles are poorly predicted in this flow.

For the predictions of the data of Loyd, a constant value of F is assumed and in the pressure-gradient region departures up to 10 per cent occur between the assumed and experimental value. The clear emphasis has been upon predicting H correctly for all the flows. Again the R_{θ} development is over-predicted for all the flows by as much as 20 per cent and since the C_f predictions for three of the four developments shown under-predicted by as much as 15 per cent, there is clear evidence of the profiles not reaching a state of full development under local conditions.

The skin friction is clearly increased for all blowing rates in the pressure gradients of Julien over the upstream constant-pressure level. However, for the much stronger gradients of Loyd there is no increase in C_f in the pressure-gradient region within experimental accuracy for all blowing rates. It is also significant that in the constant-pressure region, upstream of the pressure gradients, for the same conditions of f, H and R_{θ} , Loyd consistently calculates values of C_f higher than Julien by as much as 10 per cent.

Baker²⁹ has also studied the effects of both favourable and adverse pressure gradients upon the transpired low-speed boundary layer. Density variations through the layer have also been considered by using Freon injection as well as air injection. The transition from constant-pressure flow to pressure-gradient flow was not measured as measurements were started downstream of the start of the pressure gradient.

For the largest blowing rates in the adverse pressure gradient the downstream stations were susceptible to three-dimensional effects and were on the point of separation. The pitot pressure close to the wall, for these stations, was equal to the static pressure. Baker also calibrated Preston tubes in channel flow with differing pressure gradients and mass-flow rates. For zero blowing the calibration was within 5 per cent of that of Patel.³⁰

Baker has used the Prandtl mixing length with a constant value in the outer layer. The Van Driest damping function has been modified for blowing in a similar manner as that of Julien and Loyd. For air injection, the prediction of velocity profiles, H and R_{θ} is very good for all three pressure-gradient flows. The proposed model for the eddy-viscosity distribution was successful for the favourable pressure gradients and for moderate adverse pressure gradients with moderate blowing rates. The model became inadequate for severe blowing rates and adverse pressure gradient and it was necessary to adjust the constant value of L_{max} in the outer layer from $0.09\delta_{995}$ down to between $0.065\delta_{995}$ and $0.07\delta_{995}$ to correct the shape factor developments. When density variation is introduced through the boundary layer the discrepancies are magnified.

Using this model, Baker has also predicted the pressure gradient transpired boundary-layer flows of McQuaid, Julien and Loyd. The agreement with the results of McQuaid, other than the C_f distribution which is not shown, is very good. The agreement with the results of Julien are overall better than that of the methods of Julien himself since R_{θ} is correctly predicted and the same scatter observed for C_f . Similarly, for the results of Loyd, R_{θ} is correctly predicted with the result that Baker's model predicts an increase in C_f in the pressure-gradient region which was neither calculated by Loyd nor predicted by the eddy-viscosity model which was adopted.

It would seem that prediction methods can be used successfully in favourable pressure gradients and in mild adverse pressure gradients with moderate blowing rates, for low-speed incompressible flow.

3. Experimental Equipment and Test Procedure

The experimental equipment used was basically the same as that of Jeromin,¹ Squire² and Dunbar³ since the present work and theirs has all been concerned with the development of injection into the compressible boundary layer along a flat porous plate. Changes in the nature of the experiments so far have needed little adjustment, if any, to the test equipment. Since the present experiments involved the production of pressure-gradient flows along the test section, which is the lower surface of the wind-tunnel cross-section, it was easiest to modify the roof of the tunnel to produce the pressure gradients. Therefore the experimental description will be concentrated upon the production of the pressure gradient and will contain only the important features of the injection apparatus and design of the wind tunnel (*See* Fig. 1).

3.1. Wind Tunnel

The tunnel in the Cambridge University Engineering Department is an intermittent blow-down tunnel using air stored at 7×10^6 N/m². The air pressure is then reduced to provide a maximum running stagnation pressure, P_0 , in the tunnel of about 10^6 N/m². There is no temperature control over the tunnel stagnation temperature; however, during a run the stagnation temperature, T_0 , varies by only 2 K whilst the mean stagnation temperature for any one particular run may vary from 290 K to 300 K depending upon the amount of use of the tunnel and the external room temperature. The tunnel cannot be run in steady-state conditions due to the short running time and there will be small variable heat-transfer rates present.

3.2. The Design of the Pressure Gradients

Since it was possible to extend the traverse-gear platform so as to traverse the rear 250 mm of the test plate (*see* Fig. 1) it seemed reasonable to commence the pressure gradients about 200 mm upstream of the traverse gear. It was hoped that this would give a length of about 150 mm which was subjected to the pressure gradient and which could be traversed before the traverse gear affected the flow.

The three pressure gradients which were produced will be referred to as Gradients A, B and C. Gradients A and C are favourable gradients; C being the stronger; and Gradient B is an adverse gradient.

The pressure gradients were produced by modifying the rear section of an Araldite, M = 2.5, wind-tunnel liner which was cast specifically for the purpose.

Gradient A was designed by the method of characteristics to increase the Mach number from 2.5 to 3.0 over the required range of 150 mm on the test plate. The rear of the wind-tunnel liner was machined to a smooth curve producing an expansion fan of 5 degrees on the tunnel liner, so that as near as possible a linear variation of Mach number was produced over the test section (*see* Fig. 2).

Gradient C was formed in an attempt to increase the favourable gradient so that a final Mach number of the order of 3.5 could be obtained with a linear change of Mach number. This could have been achieved by an expansion fan of 10 degrees on the linear surface. In practice, the effect of the last part of the expansion fan was downstream of the test section and a final Mach number of 3.25 was reached on the test section. It was not thought advisable to produce the gradient by a single turn of 10 degrees as used by Michel *et al.*,¹⁷ since the lack of agreement between these results and prediction methods was explained by a possible relaminarisation of the boundary layers due to the large magnitude of the pressure gradients.

The severity of the Gradients A and C was determined to a large extent by the small dimension of the tunnel cross-section, since it was impossible to turn the flow back gradually enough after the initial 10 degree expansion to avoid forming a compression shock. It was therefore important to remove this compression far enough downstream so that the reflected compression shock off the test section did not occur over the test region. The design of the compression corner proved very difficult since the tunnel could not be started if the corner was too gradual and the cross-sectional area became too large. For Gradient A, a tunnel wall shape was eventually achieved which matched with the diffuser throat and removed the compression downstream from the test section. The tunnel could then be started at a stagnation pressure of 3.7×10^5 N/m² instead of 3×10^5 N/m² as for a constant pressure flow at a Mach number of 2.5. When the flow was tested with injection through a porous test plate it was found necessary to increase the running stagnation pressure to 5×10^5 N/m² to maintain the compression shock system behind the test section in a stable condition. It was extremely important to operate the tunnel at a stagnation pressure as low as possible so that a sufficiently long run could be obtained to complete the temperature traverses, since the temperature probe has a small time lag.

A similar tunnel-wall shape was used for Gradient C downstream of the expansion fan but a stagnation pressure of 5.8×10^5 N/m² was needed to obtain the required injection rate with a stable shock system behind the test section.

Gradient B was produced by fitting a dural plate to the rear of the liner. The plate was rolled to an approximate shape and machined underneath at various positions to reduce its thickness so that it could be wedged to produce a sufficiently flexible wall. The upstream shape of the wall was then adjusted to produce the start of a linear variation of Mach number reducing from 2.5 to 2.2 over the test section. The plate was systematically adjusted further downstream until the Mach number variation was achieved. The tunnel-wall shape after the compression was a gradual expansion to match to the diffuser throat and caused no problems since no shocks were formed and the influence fell behind the test section. The presence of injection modified the pressure gradient so that the Mach number fell to 2.1 for the downstream stations. This is caused by the boundary layer being under the influence of more of the compression fan due to the thicker boundary layer. The tunnel could be operated at a stagnation pressure of 3×10^5 N/m² for all injection rates in this pressure gradient.

3.3. Probes

Four boundary-layer probes were used; the design of which can be seen in Fig. 3. Two pitot tubes were used for the calculation of the local Mach number profile; a temperature probe for the calculation of the static temperature through the boundary layer; and a static-pressure probe which was used to check that there was negligible transverse pressure gradients through the boundary layer and that the static pressure correlated with the free-stream Mach number determined by the pitot. The reason two pitot probes were used was that the initial probe was damaged during a tunnel run.

The pitot probes were made from hypodermic tubing of outside diameter 1 mm which was flattened and filed to give half heights from the wall to the centre line of the mouths of 0.053 mm and 0.061 mm. The probes were not symmetrical above and below the mouth due to the manufacture and also due to wear upon the lower surface of the initial probe which had been used for several years.

The temperature probe was made from a stainless steel cone of 5 degrees half angle and maximum diameter 1.65 mm which had a copper-constantan thermocouple hard-soldered inside. The cone was fitted to a piece of ceramic tubing 2.5 mm in length which in turn was fitted to hypodermic tubing which carried the insulated wires away to a switching device to which all the other wall thermocouples were connected. Previous temperature probes have used as much as 25 mm of ceramic tubing as insulation and have been strengthened by wedges of brass, but it is impossible to strengthen the ceramic tubing without adding too much to its outside diameter. This length of ceramic proved too fragile for the most upstream traverses during the large loads experienced in the tunnel starting process. Reducing the length of ceramic made no difference to the temperature profile recorded and consequently the stronger type with very little ceramic was adopted.

The static pressure probe was made with a 5 degree whole angle cone which was soldered into a hypodermic tube of outside diameter 1 mm. Two holes of diameter 0.4 mm were drilled through the top and lower sides of the tube at a position 20 mm from the tip of the cone.

3.4. Injection

The injection test area is 85.8 mm across stream and 396 mm downstream and has 32 copper-constantan thermocouples fitted into the surface so that the wall temperature can be interpolated for individual traverses. The boundary layer has been under the influence of injection for about 200 mm so that the boundary layer is characteristic of equilibrium conditions in the constant-pressure flow before the pressure gradients are imposed. The porous test plate is made of porosint Grade A which enables a relatively large pressure difference across the surface to exist for low blowing rates in comparison with the change in wall static pressure along the designed pressure gradients. Therefore the local mass-injection rate varied by only 5 per cent of the mean value along the porous plate under the pressure gradient.

When referring to a particular flow development, the injection rate is then referred to by the variable $m = \rho_w v_w/(\rho_1 U_1)_{ref}$ which only exhibits this small variation along the pressure gradient. The reference conditions refer to a mean value of $\rho_1 U_1$ upstream of the designed pressure gradient where the flow is nominally at a Mach number of 2.5, whereas $\rho_w v_w$ refer to the local conditions. The significant injection parameter, however, is $F = \rho_w v_w/\rho_1 U_1$ where all the variables are evaluated locally and hence the variation of F along the gradient is dependent upon $\rho_1 U_1$ which varies by as much as 100 per cent along the pressure gradient.

Since a change in static-pressure distribution anywhere over the plate will affect the local injection rate and hence the injection rate all over the plate, it is necessary to consider the static-pressure distribution behind the probe and under the probe-holder extension. Except for a small disturbance caused by the compression shock from the front of the probe and minor ones from edges on the extension, the designed pressure gradients were not affected and the effect on the quoted values of *m* was negligible.

Spanwise variations of static pressure were shown to be small by Jeromin³¹ who traversed 25 mm either side of the centre line of the test section when making sure that negligible three-dimensional effects existed. By comparing the static pressure distributions with and without the probe holder extension in position it would appear that the effect of the designed expansions upon the test section is almost unaffected by the presence of the holder.

For Gradients A and C, there occurs a severe adverse pressure gradient after the induced reflected shock which separates the boundary layer on the test section for the highest blowing rates. The position and nature of this adverse gradient were taken into account when calculating the local mass-injection rates.

The above factors can only influence the injection rate by changing the static-pressure distribution. Since measurements through the boundary layer must be performed using a porous plate without static-pressure holes so as not to disturb the local injection rate, the static-pressure distributions produced were recorded during runs using another plate containing pressure tappings. It is estimated that all the combined effects mentioned above produce only a change of less than ± 1 per cent of the mean injection rate whereas the change due to the designed gradients is of the order of ± 5 per cent. The variations of local mass-injection rate *m* and the blowing parameter *F* as a function of streamwise station are shown in Fig. 4.

The temperature of the air supply upon entering the plenum chamber under the porous test plate was just below room temperature and since the test plate normally cools below this temperature during a tunnel run with zero blowing, there will be heat transfer from the injected air to the porous plate and from the porous plate to the free stream. In practice these small-heat transfer rates balance so that the porous plate has a steady wall temperature for positive injection.

The maximum injection rates were fixed by safety limits on the injection equipment. Besides the zero-injection developments, it was possible to obtain:

- (a) two blowing rates for Gradient A, namely m = 0.001 and 0.002,
- (b) three blowing rates for Gradient B, namely m = 0.001, 0.002 and 0.003, and
- (c) only one blowing rate for Gradient C, that of m = 0.001.

3.5. Test Procedure

The first upstream traverse was made 145 mm downstream of the start of injection which was thought sufficient for the boundary-layer profiles to be characteristic of fully developed profiles in zero pressure gradient. This leaves 220 mm of boundary layer development for the measurements, of which the first 50 mm are still in a nominally zero pressure gradient.

The pressure traverses were conducted away from the wall to the free stream and then reversed since the probe was sufficiently flexible to be wound 'into' the wall to record the wall position. This also allowed the temperature of the air in the pitot system to adjust to the running conditions on the outward traverse whilst measurements were taken on the inward traverse. This was possible during the length of running time because of the quick response of the system used. This was not the case for the temperature traverses where there was an obvious time lag if an outward and inward traverse were carried out. The time lag per Kelvin for the metal cone for the range of temperature used was calculated of the order of 4 to 6 seconds. Thus a continuous X–Y plot would be meaningless without taking this lag into account on the scale. It was decided to produce a series of readings at intervals through the boundary layer which were clustered near the wall where the laminar recovery-temperature drop on the cone is largest. By this method it was possible to obtain a traverse as accurate as the error involved in reading the X–Y traces.

Because the temperature probe is much larger than the pressure probe, it is necessary to extrapolate the temperature trace to the local wall temperature.

Boundary-layer traverses were conducted at intervals of 12.7 mm downstream until the boundary layer was either influenced by the reflection of the compression shock or by the presence of the traverse gear. Such an influence can be detected on the X-Y pressure traces when blow-off or unsteadiness may occur through the boundary layer making it difficult to interpret the trace.

For Gradients A and B the pressure gradient can be regarded as commencing between stations 3 and 4. For Gradient C traverses start an extra station upstream and the pressure gradient starts between stations 4 and 5.

With increasing injection rates causing an increase in the boundary-layer thickness, the influence of the pressure gradients is felt further upstream.

For the case of Gradient B, m = 0, traverses were carried out at intervals of 6.35 mm instead of the usual 12.7 mm so that any disturbances would be exposed from the bulk of data measurements. For injection, it was found that with the general increase in boundary-layer growth the effect of these disturbances upon the pressure traces was considerably reduced. For the two highest blowing rates no distortion of the traces could be detected. It is clear, however, that non-linearity in the pressure gradient is magnified by increased injection as can be seen from the Mach number distribution.

3.6. The Reduction of the Experimental Data

The raw data collected from the wind tunnel comprise the X-Y recorder traces through the boundary layer of:

(a) the pitot pressure; behind a normal shock in the case of supersonic flow,

(b) the laminar recovery temperature on a 5 degree cone which is used to determine the local static temperature,

and

(c) the tunnel stagnation pressure, temperature and the wall temperature.

With certain assumptions, the above form a complete set of data with which to determine the velocity and temperature profiles and parameters.

Since the imposed pressure gradients produced neither a measurable transverse-static-pressure gradient nor any shocks in the adverse pressure gradient in the boundary layer itself, the assumption that the flow is isentropic and has constant static pressure through the boundary layer does not appear to be violated when the results are examined. Consequently a data-reduction program similar to that described by Dunbar³ can be used.

The behaviour of the local air density at any point through the boundary layer was calculated using the perfect-gas-state equation which reduces to $\rho/\rho_1 = T_1/T$. The distribution of viscosity through the boundary layer was determined using Sutherland's formula in the form $\mu = \mu_{273}(T/273)^{\frac{3}{2}}(383 \cdot 2/T + 110 \cdot 2)$ where $\mu_{273} = 0.551$ centi poises. A laminar Prandtl number of 0.72 was assumed for the determination of static temperatures from the laminar recovery temperature as measured by the probe.

Probably the largest uncertainty in the evaluation of the collected data is the determination of the free-stream total pressure for the adverse pressure gradient B. The adverse pressure gradient is produced by many weak compression disturbances imposed onto the boundary layer. When a slightly stronger disturbance coincides with the edge of the boundary layer at a traverse station then a distorted pressure trace is recorded on the X-Y recorder. Luckily, this happened at only three or four out of twenty-eight traverse sections in Gradient B, m = 0 and such disturbances were less marked with the presence of air injection.

Fig. 5 demonstrates a normal pressure traverse and two types of trace deformed in the outer part of the layer. The dashed line represents the estimated profile used to describe the boundary layer at that station. The estimated profile is that with which the inner part of the layer would appear compatible if the disturbance had not been present. Since the disturbances do not propagate far into the boundary layer perpendicularly to the wall, it was found that only the outer 20 per cent of the boundary layer was affected at the disturbed stations. No effect of disturbances was noticeable at the adjacent downstream station since the boundary layer had already adjusted to the conditions downstream of the disturbance. The change of profile shape from that of constant pressure equilibrium to the developed profile in the pressure gradient was always systematic so that a profile in between stations could be predicted with little error. The estimated profile can be tested by plotting u/U_1 against y/δ and observing that the profile fits the local trend of profile development. Clearly an unsuitable choice for the free-stream total pressure would result in a disturbed value for the free-stream Mach number, M_1 , and hence an unsatisfactory value of U_1 with which to scale the local velocity.

Rapid changes in the boundary layer parameters, however, are more commonly caused by a rapid change in the boundary layer thickness, δ itself, rather than a disturbed velocity profile. The effect of having to estimate the free-stream velocity produces smaller changes in boundary-layer parameters than those caused by the disturbances in the boundary-layer thickness. These profiles appear similar when plotted u/U_1 against y/δ and only exhibit disturbed profile shapes when plotted u/U_1 against y. Fortunately such traverse stations exhibiting either of these disturbances were few compared with the number performed for Gradient B.

4. The Skin Friction Coefficient

One of the purposes of investigating the present layers was to determine the validity of various forms of the inner law under these circumstances. For this purpose some degree of knowledge is required of the wall shear stress. An absolutely accurate value of the skin-friction coefficient C_f is often not essential. For uniform flows with small disturbance a mean value obtained from the momentum equation is quite adequate. Unfortunately it was difficult to use this equation over various ranges of the present developments without further knowledge of the expected variation of C_f in pressure gradients of this order of magnitude.

Over a range of boundary layer near the start of the pressure gradients, rapid change in the measured momentum thickness θ were recorded. These usually diminished to leave some range of the pressure-gradient flow with a smooth variation where a momentum balance could be attempted. However, the nature of the continuous change from the upstream constant-pressure flow to such reasonably smooth portions could not be estimated through the disturbed region of rapid change. It was therefore clear that other means of determining C_f was essential in analysing the changeover between the two regions of the flow. Apart from this, extremely large percentage errors are incurred when the momentum integral equation is used for blowing rates when the value of C_f is very small.

For mild pressure gradients, where the magnitude does not vary rapidly, and for low blowing rates, the skin friction appears to be satisfactorily predicted by fitting the velocity profile to some appropriate form of inner law. Direct measurement of C_f in a pressure gradient flow using a floating element balance is difficult since secondary forces on the element must be calculated. Usually the accuracy of these results is worse than using Preston or Stanton tubes, provided that an accurate calibration, which takes into account any normal pressure gradient, is used. Sivasegaram¹⁸ has noted that the floating element cannot be used reliably in pressure gradients with magnitudes similar to those of the present experiments.

4.1. The Measurement of Skin Friction for Zero Injection

The variation of wall shear stress along the test plate for zero injection was found using the razor-blade technique devised by Smith, Gaudet and Winter.³² This method requires a calibration of the razor blades against skin-friction coefficient. However, in the present investigation a skin-friction balance was not available so that neither a direct measurement of C_f nor a calibration of the razor blades in pressure gradients was possible.

The calibration used by Smith *et al.* could not be used in the present experiments since the size of the static pressure holes in the test section was only a third of that used by Smith *et al.* This meant that the geometry of the blades above the static-pressure holes would be different unless both faces of the razor blades were machined to produce much thinner razor blades. This usually caused the razor blades to bow, rendering them useless for the purpose required.

Differences in razor-blade calibrations have been shown by Hopkins and Keener³³ when the position of the blade relative to the wall tapping was varied, and by East³⁴ when the chamfer height on top of the razor blade and the position of the leading edge were varied. It was therefore decided to place the front of the razor blades over the leading edge of the wall tapping and remove the chamfer from the top surface of the blades so that only 10 per cent remained (*see* Fig. 6). This would ensure that the boundary layer recovered as quickly as possible so that closer spacing of the blades could be used. To calibrate the razor blades it was decided to use the Spalding–Chi values for constant-pressure flows since several experimental uniform flows of Squire² and Jeromin¹ had demonstrated a very close agreement between these values and those obtained from the momentum growth.

The calibration reached by a dimensional argument for such blades is of the form

$$\frac{\tau_w \rho_w h^2}{\mu_w^2} = F\left(\frac{\Delta P \rho_w h^2}{\mu_w^2}\right).$$

That of Smith et al. originally took the form of:

$$\frac{\tau_{w}\rho_{w}h^{2}}{\mu_{w}^{2}} = 0.207 \left(\frac{\Delta P\rho_{w}h^{2}}{\mu_{w}^{2}}\right)^{0.764}.$$

To check that this form of the calibration did not apply to the present arrangement it was necessary to vary at least two of the variables in the calibration. The simplest manner seemed to be the use of a constant-Machnumber flow at different stagnation pressures. Several razor blades could be mounted along the test plate and

used for the various runs. Since the individual heights of the razor blades should remain constant and the local wall temperatures remain constant, a calibration of the form

$$\frac{\tau_w \rho_w h^2}{\mu_w^2} = a \left(\frac{\Delta P \rho_w h^2}{\mu_w^2}\right)^b \text{ reduces to } \frac{(\tau_w \rho_w)}{(\tau_w \rho_w)} \frac{\text{ref. 1}}{\text{ref. 2}} = \left(\frac{(\Delta P \rho_w)}{(\Delta P \rho_w)} \frac{\text{ref. 1}}{\text{ref. 2}}\right)^b.$$

The different reference conditions apply to any of the different stagnation pressures.

From the experiments of Squire and Jeromin, the values of C_f expected for certain of the tests were known from the momentum growth. These agreed with the values predicted using the Spalding-Chi calibration.³⁵ Therefore the ratio of $(\tau_w \rho_w)$ ref. $1/(\tau_w \rho_w)$ ref. 2 was well known; for example for M = 2.5 at $P_0 = 3 \times 10^5$ N/m² and $P_0 = 5 \times 10^5$ N/m². The calculated value of b obtained did not agree with the value of 0.764 quoted by Smith *et al.* and was consistently higher than this value for all the razor blades.

The value of b found from the present readings which gave reasonable values of (C_f) ref. $1/(C_f)$ ref. 2 as predicted by the Spalding-Chi calibration was b = 0.794. This was representative of all the razor blades, for the three Mach numbers of 1.8, 2.5 and 3.6 for their ranges of stagnation pressure, to within ±4 per cent of 0.794. If however, only the results where $\log (\Delta P \rho_w)$ ref. 1 and $\log (\Delta P \rho_w)$ ref. 2 differ by more than 1 per cent are used, the calculated values of b are clustered to within ±2 per cent of b = 0.794. If this difference is much smaller than 1 per cent then the solutions for b are not so reliable.

By finding the value of b in this manner there is as yet no reliance upon absolute values of C_f . The ratio of skin-friction coefficients for the relevant values of R_{θ} is probably better known than their absolute values, for compressible flow. The mean values obtained from the momentum growth agree with the Spalding-Chi values. The values of C_f produced by the method of Winter and Gaudet³⁶ are generally of the order of 1 or 2 per cent below the values of Spalding and Chi, but produce the same ratio of (C_f) ref. $1/(C_f)$ ref. 2 for the range used here.

The value of the constant a in the calibration depends upon the absolute value of C_f used and upon the effective height h of the Stanton tube, which depends upon the height of the leading edge from the test plate and to a lesser extent upon the chamfer height on the top surface of the blade. Since the chamfer heights used here are relatively small, the effective heights of the razor blades were taken as the height of the leading edge from the surface of the test plate. The small error involved due to the neglect of the chamfer height is automatically compensated for in the calculated value of a in the calibration. The value of a which gave the best mean fit with the Spalding-Chi values of C_f , for all the razor blades, was 0.151. The scatter about this value was within the experimental error involved in measuring the heights of the razor blades. These were measured using tallysurf traverses to an accuracy of approximately ± 1.5 per cent. The shadowgraph and travelling microscope verified the heights with a lower accuracy of ± 4 per cent.

If the heights of the razor blades could be measured more accurately then a better method would have been to calibrate each razor blade individually to account for differences in the individual geometries which must exist. The accuracy of the calibration would then depend mainly upon the error in obtaining the required values of C_t to determine the constant a.

The calibration obtained to represent Mach numbers between 1.8 and 3.6 for stagnation pressures from 2×10^5 N/m² to 10^6 N/m² for zero pressure gradient is then:

$$\frac{\tau_{w}\rho_{w}h^{2}}{\mu_{w}^{2}} = 0.151 \left(\frac{\Delta P\rho_{w}h^{2}}{\mu_{w}^{2}}\right)^{0.794}.$$

The three sets of authors previously mentioned who have used razor blades have shown that calibrations of the form $\log \tau_w \rho_w h^2 / \mu_w^2$ against $\log \Delta P \rho_w h^2 / \mu_w^2$ are in fact non-linear, but over the limited range of $\Delta P \rho_w h^2 / \mu_w^2$ used in the present experiments, the calibration may be taken as linear, well within the bounds of experimental error. Over the same range, the calibration of Hopkins and Keener³³ can be approximated by a linear calibration with b = 0.833 as opposed to that of b = 0.764 by Smith *et al.* The value of 0.794 for *b* in the present experiments is therefore reasonable since the geometry of the razor blade relative to the wall tapping also lies between that of the above two sets of authors.

In the present experiments it was found that the static pressure in the boundary layer had readjusted to the undisturbed value within 25 mm downstream of a razor blade. The razor blades for the calibration at different Mach numbers and stagnation pressures were positioned at approximately 50 mm intervals along the plate. The series was then repeated with the razor blades shifted by 25 mm. In each case the first run was repeated at the end of the series to check whether a razor blade had shifted. The tallysurf traverse was also repeated.

Although the razor blade technique of determining wall shear stress has already been used in pressure gradients, the effect of pressure gradient upon the calibration cannot be evaluated at present because of a lack

of reliable skin friction data in pressure gradients. Consequently the calibration as found above, was used to determine the skin friction distribution of Gradients B and C. The readings were taken in two stages so that the shear stress could be evaluated at intervals of 25 mm along the test section.

If the calibration holds for pressure gradients, this would then produce skin friction measurements in the pressure gradients as accurate as those predicted by the Spalding-Chi calibration for zero pressure gradient.

4.2. An Estimation of Skin Friction for Injection

Measurements similar to those upon the solid plate could not be made for the porous plate because of the inevitable disturbance of the local mass-injection rate. Consequently some means of transforming the skin-friction results for zero injection, incorporating the effect of injection, had to be used. Some evidence for such a correlation in zero pressure gradient does exist. For example, it would be possible to estimate the effect of an injection rate at a particular Mach number between 1.8 and 3.6 by interpolating upon the figure of C_f/C_{f0} against $2F/C_{f0}$ in Ref. 37.

Some similar type of interpolation could be used for flows in pressure gradients if C_{f0} were taken to be the measured skin friction in the pressure gradient without injection. This would by no means be rigorous but would serve as an estimate for finding C_f in injected pressure gradients. For example, the assumption that C_f/C_{f0} or $C_{f0} - C_f$ remained the same value as for the equivalent constant pressure flow at that Mach number and Reynolds number, may produce C_f to the required accuracy if the use of theoretical prediction methods cannot be used. Any interpolation or extrapolation method has obvious flaws. For example, if C_f/C_{f0} for the pressure-gradient flow were assumed to remain the same as for the equivalent constant-pressure flow at that Mach number then separation caused by injection in the constant-pressure flow gives $C_f/C_{f0} = 0$. If this value is used for the pressure-gradient flow it prevents a favourable pressure gradient delaying separation. For an adverse pressure gradient, where an equivalent value in constant-pressure flow at C_f/C_{f0} is non-zero, then if C_{f0} tends to zero in the adverse pressure gradient, C_f must also tend to zero for any injection rate, and separation must occur at the same position with and without injection. This is illogical since injection is observed to accelerate the onset of separation. Assuming that C_f/C_{f0} remains constant is therefore inaccurate close to separation. From a comparison of the predicted developments with the estimated values of C_f , in Figs. 8 to 10, using this assumption, it is clear that the estimation holds reasonably well for the two favourable pressure gradients but overestimates the predicted values in the adverse pressure gradient and does not show the separation indicated by the predicted developments. Since C_f/C_{f0} is non-zero for the constant-pressure flow equivalent to a station in Gradient B, and since C_{f0} is non-zero along Gradient B, then the estimation cannot produce a zero value for C_f and the estimation must overestimate C_f for adverse pressure gradients with low skin-friction values. The errors produced by this method of estimating C_f seem to be much larger in adverse pressure gradients than in favourable pressure gradients as conditions move away from separation.

Similar limitations exist if $C_{f0} - C_f$ is assumed to remain constant, for $C_{f0} - C_f$ can be non-zero in the constant-pressure flow whereas both C_{f0} and C_f can be zero in a strong adverse-pressure gradient. This assumption seemed likely to produce much larger errors in the estimation of C_f and was therefore not considered.

The estimates of C_f for the injected flows, assuming that C_f/C_{f0} remains constant, and the measured values for zero injection are shown with other boundary-layer parameters in Table II. A rigorous correlation between skin-friction coefficients in pressure gradient and constant-pressure flows for various injection rates does not seem worthwhile when so little experimental data exists and when satisfactory results can be obtained from theoretical boundary-layer-prediction methods.

5. The Comparison of the Present Results with Two Prediction Methods

This aspect of the work is to be covered in greater detail by Marriott and Thomas but a brief explanation of the theoretical developments which appear in the Figures is necessary.

One theory is that of Verma⁵ which was written for compressible flow with injection. Verma solves the enthalpy and momentum equations with the aid of an eddy-viscosity model and the hypothesis used was basically the same as that of Cebeci and Smith.²² Differences between the two methods exist in the manner of solving the finite difference equations.

The other theory is the author's extension of the Bradshaw-Ferriss method for compressible flow with zero heat transfer to include injection. The program was modified in a similar manner to that suggested by Ferriss and Bradshaw³⁸ for incompressible flow with injection. Before this modification was made it was necessary to change the length scale, L_{max} , from $0.096\delta_{995}$ as used by Bradshaw to $0.075\delta_{995}$, and also to increase the value of the mixing length constant k to 0.418 from 0.4. As the program originally stood, it predicted the

developments of displacement and momentum thickness and skin friction satisfactorily. However it could not produce the non-dimensional equilibrium velocity profiles for constant-pressure flows measured in the Cambridge University Engineering Department wind tunnels and those of the present experiments for zero injection. For similar Mach numbers and Reynolds numbers these profiles are almost identical to those of Coles;³⁹ Rubesin, Maydew and Varga;⁴⁰ Peake, Brakmann and Romeskie;⁴¹ Michel;⁴² Sivasegaram⁴³ and Baker.²⁹ However, the profiles of Winter and Gaudet³⁶ at much higher Reynolds numbers and those of Adcock, Peterson and McRee⁴⁴ at much higher Mach numbers are predicted better by a value of $0.096\delta_{995}$ for L_{max} . Another way in which the difference in profile shapes between the data of Winter and Gaudet and those mentioned is shown in the relation between the incompressible and compressible momentum thicknesses as a function of Mach number. Winter and Gaudet propose a relation of the form,

$$\theta_i/\theta = 1 + \alpha M_1^2$$

with $\alpha = 0.056$, whereas the value of α should be increased by the order of 20 per cent for the parameters measured by other authors. A detailed comparison between the present experimental profiles and much of the existing constant pressure and pressure-gradient flows with and without injection is given by Thomas.⁸

With a value of $0.096\delta_{995}$ for L_{max} in the Bradshaw-Ferriss method the predicted velocities were too high in the inner region and slightly too low in the outer region of the boundary layer, thus compensating for the displacement thickness. With a value of $0.075\delta_{995}$ for L_{max} the profiles were very similar to those measured at Mach numbers and Reynolds numbers in the same range as the present experiments without a noticeable change in displacement and momentum thicknesses. With a value of 0.4 for k the skin friction development was now underestimated and the value of 0.418, which is characteristic of the boundary layers in the Cambridge University Engineering Department supersonic wind tunnel, returned the development in close agreement with the Spalding-Chi development which in turn agreed with the skin friction values obtained from the experimental momentum growth.

To incorporate injection, the form of the inner law proposed by Bradshaw and Ferriss

$$\frac{2}{V_{w}}[(uV_{w}+U_{\tau}^{2})^{\frac{1}{2}}-U_{\tau}]=\frac{1}{k}\log\frac{U_{\tau}y}{\nu w}+A$$

where A is now a function of Mach number and V_w/U_τ was finally chosen as giving best agreement with experiment with minimum computing time.

These are then the two methods used to produce the theoretical developments which appear in the Figures.

6. Discussion of the Boundary Layer Profiles

The basic experimental results are tabulated in Tables 1 and 2. The smoothed Mach-number distributions used for the theoretical predictions are shown in Fig. 7. Similar presentations of each gradient follow for C_f , δ^* and θ in Figs. 8 to 12. Typical temperature profiles in the zero pressure gradient region, at X = 0 mm, and downstream, at X = 127 mm, where the profiles are typical of the pressure gradient are shown in Figs. 26 to 28. The full boundary-layer developments for the flows are shown in the form of velocity profiles at intervals of 25.4 mm in Figs. 13 to 21.

The inner law is considered in the form

$$G(u) = \int_0^u \frac{(\rho)^{\frac{1}{2}} du'}{(\tau_w + \rho_w v_w u')^{\frac{1}{2}}}$$

versus log y^+ for some of the developments in Figs. 30 to 35. The outer law is also considered in the form $(U_{\tau}-u)/U^*$ versus y/δ for typical profiles in Figs. 39 and 40.

6.1. The Velocity Profiles

When the velocity profiles are plotted in non-dimensional form all three pressure gradients demonstrate the increase in fullness associated with the presence of injection and it is clear that the adverse pressure gradient deforms the profile in the same manner as injection. The shape of the profiles for the two highest blowing rates in Gradient B is similar to those of Jeromin¹ and Marriott⁴ for high blowing rates at a Mach number of 3.6 towards the last test stations of the developments. In these cases there was an upstream history of an adverse pressure gradient. For all these flows the skin-friction is very low so that the logarithmic region may be so small as to be immeasurable and the profiles are dominated by the wake component. This behaviour is very similar to that of the profiles measured by Stratford¹³ with a nominally zero skin-friction coefficient. Neither of the

prediction methods show this kind of behaviour when approaching separation although both methods predict a gradual fall in skin friction until separation is predicted.

The change in the profile shape close to the wall, between that in a constant-pressure flow and that in a favourable pressure gradient, indicates an increase in wall shear stress with the presence of a favourable pressure gradient. In pressure Gradient C there is a trace of an inflection in the profiles close to the wall, as in the profiles of Michel *et al.*¹⁷ This is not shown by either of the two prediction methods.

With the addition of injection the profiles become fuller and the wall shear stress reduces with an increase in injection rate. The injection profiles for favourable pressure gradients resemble those for lower injection rates in constant-pressure flows or still lower injection rates in adverse-pressure gradients. For example, for m = 0.001 the velocity profiles in Gradient A resemble zero-pressure-gradient profiles for zero injection.

6.2. A Comparison of Velocity profiles in Pressure Gradients with Injection

When a comparison of velocity profiles is made it is essential to know the immediate history of the boundary layer upstream. Although local conditions of two profiles may be similar their immediate upstream histories may differ greatly so that the profile shapes also differ noticeably. The profile shapes with which the present profiles are compared are taken after as long a development as was measured in the particular pressure gradient. In some cases the local conditions vary continually along the flow and the state of the flow is mentioned when considering the profile shape.

The adverse-pressure-gradient profiles are shown in Figs. 22 and 23. The profile shape, onto which the present measurements along each flow collapse, represents a pressure-gradient parameter β of between 0.5 and 0.6. The injection rate is considered in the form V_w/U_1 so that both compressible and incompressible data can be considered. The profiles are plotted versus y/θ_i for the same reason.

In Fig. 22 the profiles of Ludwieg and Tillman⁴⁵ and Sivasegaram¹⁸ for $\beta \approx 0.5$ are very similar to those of the present experiments. The profile for $\beta = 0.235$ of Sivasegaram is still influenced by the upstream favourable pressure gradient and resembles a zero-pressure-gradient profile. All the other profiles are at nominally higher values of β . The profiles of Schubauer and Klebanoff⁴⁶ represent profiles at lower values of β than shown since the pressure gradient starts only 50 mm upstream of that for $\beta = 1.74$ and follows a favourable pressure gradient. The later profile represents a lower value of β than $\beta = 12$ since the flow causes a rapid increase in β and does not adjust to local conditions. The profile for Baker²⁹ for $\beta = 1.18$ is similarly affected but that for $\beta = 0.98$ is characteristic of local conditions. The flow of Stratford¹³ has a rapid β variation and only close to the wall does the profile show the fullness associated with a very low skin friction. All the profiles of Peake, Brakmann and Romeskie⁴ appear under-developed which is associated with the under-developed flow in the constant-pressure region upstream of this pressure gradient. The profiles of Voisinet *et al.*¹⁹ also represent lower values of β than calculated since the flow follows a strong favourable pressure gradient and β increases rapidly.

For injection in Fig. 23 the profiles of McQuaid²⁶ are characteristic of local conditions and the profiles for $V_w/U_1 = 0.002$ are almost identical with the present experiments. The developed profiles of Baker for $\beta = 0.98$ agree with the present profiles, except close to the wall, where the present profiles demonstrate higher velocities, associated with the onset of separation. Baker's profiles for $\beta = 1.18$ again seem representative of lower values of β .

Figs. 24 and 25 show the profiles for favourable pressure gradients. For zero injection the profile of Herring and Norbury¹² is very similar to those of Gradient A and only varies slightly close to the wall. The profiles of Sivasegaram are representative of a value of $-\beta$ less than 0.6 as indicated and the profile for $-\beta = +0.16$ probably corresponds to a value higher than this, since full development in the constant-pressure flow does not occur until after this station. The profile of Baker for $-\beta + 0.47$ is similar to that for Gradient A except near the wall. The profile for $-\beta = +0.78$ again corresponds to a higher value of $-\beta$ due to the stronger pressure gradient upstream. The profiles of Michel *et al.*¹⁷ are taken from the downstream stations of the developments D1, D2 and D3 but all the profiles demonstrate the influence of the stronger pressure gradients upstream, which are respectively $-\beta = 1.4$, +1.6 and +1.8. The profile shapes of both Loyd²⁸ and Julien²⁷ seem characteristic of stronger pressure gradients, but unlike the flows of Michel *et al.* there is no stronger pressure gradient upstream. Instead, the boundary layer in the constant-pressure region upstream of the test pressure gradients is not in equilibrium and is considerably under-developed and resembles that in a mild favourable pressure gradient.

A comparison between profiles for injection into favourable pressure gradients is not as simple as that for adverse pressure gradients since the effects of injection and a favourable pressure gradient on the profile shape are in opposite senses. Injection tends to make the profile fuller with lower velocities for a given value of y/θ_i

whereas the favourable pressure gradient has the opposite effect. This holds through the inner half of the boundary layer, but as can be seen in the figures the profile shapes cross and the reverse is true in the outer region of the layer. Nevertheless, the profiles of Loyd and Julien are under-developed for the local values of β . The profiles of Baker and McQuaid, for similar values of β and V_w/U_1 resemble the present profiles.

The profiles of Baker for freon injection show that close to the wall the profiles are similar to those of air injection into boundary layers with very low skin-friction coefficients, since the profiles approach the u/U_1 axis steeply close to the wall. In general the profiles show higher velocities for a given value of y/θ_i than for air injection, since the free-stream value of y/θ_i is less than that for the equivalent flow with air injection.

It is concluded that the present experimental flows are substantially developed under the influence of the pressure gradients. Similarly the flows of McQuaid and Baker for either favourable or adverse pressure gradients are also developed but the favourable-adverse pressure gradient of Baker and the flows of Loyd and Julien do not attain a developed state under local conditions.

For developed flows theoretical methods can predict profile shapes quite adequately but when the flow is under-developed and influenced by upstream conditions which are different from the local conditions, differences between theory and measurement will exist unless the upstream history is also considered in the theory.

6.3. The Temperature Profiles

For compressible flow with zero heat transfer one would expect that the flux of total energy would remain constant through the boundary layer. Since the wall temperature under these conditions would be below the stagnation temperature, T_0 , this implies that T_0 is not constant through the boundary layer and that there is an overshoot in T_0 near to the edge of the boundary layer, since u = 0 at the wall. In the present experiments, for zero blowing the measured wall temperatures were generally slightly higher than the calculated wall recovery temperature using a recovery factor of r = 0.89. The reduction of the wall temperature usually attributed to the effect of injection is not noticed, as can be seen from Table 2, since the heat transfer from the injected air supply to the wall maintains the wall temperature very close to the room temperature. For zero blowing the heat transfer is from the wall to the boundary layer and an observed cooling of the wall is noticed.

The variation of static temperature in the zero pressure gradient and in the pressure gradient for stations X = 0 mm and X = 127 mm respectively are shown in Figs. 26 to 28. The effect of the pressure gradient upon these is not so marked as upon the velocity profiles but the same tendency to be fuller with blowing and adverse pressure gradients exists. The obvious change upon the profiles is caused by the change in the scaling factor T_1 due to the variation in M_1 along the pressure gradient.

From a theoretical analysis with a range of turbulent Prandtl numbers, Spence⁴⁷ found that a good approximation to his results was given by

$$\frac{T}{T_1} = \frac{T_w}{T_1} + \frac{T_r - T}{T_1} \cdot \frac{u}{U_1} - \frac{T_r - T_1}{T_1} \cdot \left(\frac{u}{U}\right)^2$$

where r refers to adiabatic wall recovery conditions. The recovery factor used in this equation for the case of injection profiles was evaluated using the empirical relation

$$\frac{r}{r_0} = \left(1 + 0.83 \frac{2F}{C_{f0}}\right)^{-0.04}$$

as used by Dunbar³ and a value of $r_0 = 0.89$ was used.

Except for the case of the two blowing rates of m = 0.002, 0.003 for Gradient B, the agreement of Spence's equation with measured temperature profiles is remarkably good in all three pressure gradients. It is in general slightly better than the temperature distribution produced by solving the energy equation from the theory of Verma. The measured temperature profile is very similar to the velocity profile for the two cases exempted above. The particular shape is also produced by Spence's equation. The same feature of rapid change between wall conditions and the first experimental values is evident, since the velocity and temperature are interrelated.

The assumption of constant T_0 through the boundary layer is clearly not true when the measured distribution is calculated. Typical distributions for the three gradients are shown plotted in Fig. 29 since interest has been shown lately in these, concerning the existence of the temperature overshoot in the outer part of the boundary layer. This is not noticed in these experiments to a significant extent although very small overshoots are indicated. However, the rapid changes close to the wall are very interesting.

6.4. Boundary Layer Relations in the Inner and Outer Layers

It is generally held that the boundary layer can be sub-divided into three distinct regions: (1) the region nearest the wall being the viscous sublayer, (2) the region known as the inner region which is influenced largely by the imposed boundary conditions of the wall, and (3) the outer region where the effect of the wall is small and the flow bears the characteristics of a 'wake' region.

Although pitot pressure probes with an outside diameter of less than 0.1 mm were made, it was found impossible to obtain sufficient satisfactory data in the sublayer region of the present boundary layers to be able to consider comparisons between theory and experiment in this region. Consequently, such comparisons will be concerned only with the inner and outer regions.

(a) The inner region

For compressible flow with combined pressure gradient and injection, the boundary-layer equations can be integrated with the usual assumptions to produce an inner law of the form:

$$G(u) = \int_0^u \frac{\rho^{\frac{1}{2}} du'}{(\rho_w v_w u' + \tau_w + (dp/dx)y)^{\frac{1}{2}}} = \frac{1}{k} \log \frac{U_\tau y}{v_w} + B.$$

For large pressure gradients, the dominant term in the expression $\rho_w v_w u' + \tau_w + dp/dx \cdot y$ is the last component. For severe adverse pressure gradients a plot of G(u) versus log y^+ produces little region where the slope is as large as 1/k and removes any sign of a wake region where one might expect a very large wake component. For severe favourable gradients there will occur a value of y through the boundary layer where $\tau_w + \rho_w v_w u + (dp/dx)y$ is zero so that any linearity of the plot existing initially is quickly destroyed. Fig. 36 shows typical plots of this form of G(u) versus log y^+ for the present experiments when G(u) is calculated using linear interpolation with small step changes in u'.

At present there appears little to be gained from such plots and one could argue that where the linearity and slope differ from 1/k, then the equation $\tau = \tau_w + \rho_w v_w u + (dp/dx)y$ no longer holds and that second order terms cannot be neglected in the boundary-layer equations. If, however, the term (dp/dx)y is neglected, the resulting plots of G(u) versus log y^+ bear similar characteristics to the usual inner law especially for favourable pressure gradients where one might expect the inner law to hold further through the boundary layer due to the much smaller wake components associated with favourable pressure gradients. Since the more logical equation to produce an inner law should include the pressure gradient term it is difficult to justify the removal of this term to produce plots which do exhibit a linear region.

For adverse pressure gradients the inner law holds only very close to the wall and it is here that experimental scatter can occur in the velocity profiles so that the law does not produce a significant linear region at all.

The amount of scatter in the G(u) plots as shown in the initial pressure gradient region in Figs. 30 and 34 is observed by most experimenters (e.g. Michel *et al.*¹⁷ and Sivasegaram¹⁸) but towards the end of the pressure gradients A and C, some of the profiles bear remarkably linear characteristics although the slopes may vary considerably. For Gradient C, it can be seen that the inner region describes nearly all the boundary layer and this effect is more pronounced for the blown profiles which is contrary to some characteristics of blown profiles which bear similarities to adverse-pressure-gradient profiles.

In the figures of the G(u) profiles (Figs. 30 to 35), Coles¹⁶ wake function is shown to describe the wake exceptionally well. In Figs. 37 and 38 the variations of π and the law of the wall constant *B* are shown along the flows for the different injection parameters. The possible error in *B* due to the uncertainty in C_f is shown on Fig. 38 by the side of each flow. With the onset of separation at the highest injection rates in Gradient B the constant *B* falls rapidly along the flows and becomes negative. In the favourable pressure gradients the value of *B* increased slightly over the initial pressure-gradient region and settled to a constant value along the flows.

The value of π increased more rapidly along the adverse pressure gradient for increasing injection. For the favourable pressure gradients the value dropped and remained virtually unchanged for increasing injection up to the maximum used in these experiments. The value of π did not reach zero and increased in the last one or two stations when the magnitudes of the pressure gradients were reduced.

(b) The outer region

It has been shown by McQuaid⁴⁸ and Squire² that the law in the form $(U_1 - u)/U_\tau = g(y/\delta)$ can be transformed to account for the compressible flow with injection and pressure gradient by using it in the form:

$$\frac{U_1 - u}{U^*} = g(y/\delta) \quad \text{where} \quad U^* = U_1 \left(\frac{T_w}{T_1} \frac{d\theta}{dx}\right)^{\frac{1}{2}}$$

The present experiments are compared with the transformed velocity defect law in Figs. 39 and 40. For zero and adverse pressure-gradient profiles, the collapse is excellent for all blowing rates while the velocity defects for the favourable gradients show vast differences. This is to be expected since it has already been shown that these profiles are satisfied by the inner law almost to the edge of the boundary layer.

It is noticeable that the velocity defects of the theories in Fig. 41 are very similar to the experimental defects. This is significant for the case of Gradient B, m = 0.002 and 0.003 where the overall developments are poorly predicted.

In Fig. 42 the range of velocity defects of the present flows in Gradient B is compared against other data. Apart from the defect profiles of Voisinet *et al.*¹⁹ the rest of the data shown agrees with the range found in Gradient B. The defects of Voisinet *et al.* show the influence of the strong favourable pressure gradient upstream.

6.5. General Comments

The experiments of many authors have shown that the collapse of non-dimensional velocity profiles for all blowing rates in zero pressure gradient is good, as would be expected for equilibrium profiles. Small deviations from such profiles occur when small pressure gradients are present. To the same degree of accuracy, the initial profiles of the present experiments collapse onto similar shaped profiles. The profiles then undergo a transition from this equilibrium profile shape when the boundary layer experiences the initial pressure gradient and rapidly tend towards a new shape characteristic of the particular gradient even though it is impossible for it to have reattained equilibrium conditions in a constant pressure gradient since the blowing rate varies from station to station along the gradient.

The initial profiles of Gradient C show signs of the presence of a mild favourable gradient upstream of the first station which would account for the increase in Mach number from the start of Gradient A. This increase was caused by attempts to smooth the Araldite-Dural join on the rear of the liner when forming Gradient B. This produced a small expansion which could not easily be removed later, and the effect upon Gradient C is to change the initial Mach number from 2.55 to 2.58.

Similarly this join produced a slight compression in Gradient B which reduced the upstream Mach number 2.51, but since it would appear that the effect upon the profiles of an adverse gradient, of similar magnitude, is less, there appears no change in the upstream profile from that of the equilibrium shape.

The favourable gradients were free from further disturbance until reaching separation at the downstream stations. One or two weak disturbances were evident in Gradient B and these did affect some of the boundary-layer parameters. In general, disturbances tended initially to increase the skin-friction coefficient, boundary-layer thickness and consequently δ^* , θ and R_{θ} without changing the shape of the velocity profiles plotted in non-dimensional terms. The increase in skin friction and Reynolds number were invariably accompanied by a drop in Mach number. It was difficult to conclude anything concisely due to the experimental error involved in measuring C_f , but it would suffice to add that different razor blades at stations 10, 13 and 15 in Gradient B indicated a higher level of skin friction than predicted by the two theories considered.

For disturbed profiles in Gradient B, which were relatively few, the error involved in measuring δ^* and θ for the worst possible configuration could be as much as ± 10 per cent, whereas for any undisturbed profiles the respective estimates would be ± 1 per cent for δ^* and ± 5 per cent for θ .

A comparison of the two predicted developments in Fig. 11 with Gradient B, m=0 shows that at X = 30 mm the start of the adverse pressure gradient has compressed the boundary layer which develops, with a minor disturbance at X = 7.5 mm, until a stronger disturbance increases the boundary-layer thickness from X = 125 mm onwards. After this change in boundary-layer thickness the non-dimensional profile shape remains unchanged.

Where differences occur in the initial values of δ^* for the two theoretical predictions in Fig. 11 the method of Verma⁵ was started with a slightly different value, by choice, so that the mean θ development in the adverse pressure gradient was in reasonable agreement with experiment. This was to ensure that the value of R_{θ} was not too far in error below experimental values so that the predicted C_f developments would be under similar conditions as the experimental values. The error in the estimated values of C_f for injection is then due to the estimation used rather than differences in conditions.

In the flows where δ^* coincides at the initial station for the two methods, their developments are almost identical and when the initial values are different, interchanging the starting values produces similar developments. Thus in the velocity profile development in Fig. 16, the apparent lack of agreement between the prediction of Bradshaw and Ferriss and the measured profiles is due to the initial value of δ^* used, whereas the

initial value of δ^* and boundary-layer thickness was scaled down for the method of Verma. When the boundary layer was compressed after 25 mm by the disturbance at the start of the pressure gradient, the development predicted by Verma, starting with an initial low value of δ^* , coincides with the experimental development, whereas that of Bradshaw and Ferriss continues at the higher level. If this method were started at the same low value it produces similar agreement as the method of Verma. Direct comparisons between the two methods must be taken from developments starting from identical values of δ^* . Small differences in θ occur at the initial station due to the difference in the temperature distributions through the boundary layer for the two methods.

7. Concluding Remarks

In many of the experimental data on two-dimensional pressure-gradient flows it is difficult to analyse qualitatively the effect of the pressure gradient itself upon the boundary layer. This is basically because the fully developed profile for those particular conditions in zero pressure gradient is unknown. Most experimental work studies the transition from a constant-pressure flow to one in the pressure gradient, but often an insufficient length of boundary layer in the upstream constant pressure flow exists to allow the flow to become fully developed before the start of the designed pressure gradient. Consequently the initial profiles in the pressure gradient often exhibit characteristics associated with the strong upstream favourable pressure gradient which commences at the throat of the wind tunnel. Alternatively, the study of the boundary layer to adjust to the local pressure-gradient conditions. In a pressure gradient where the magnitude varies rapidly along the entire flow, the boundary layer will never be representative of local conditions.

Although it is probably unrealistic to expect the boundary layer to obtain fully developed equilibrium conditions because of minor fluctuations in the imposed pressure gradient, these conditions can be approached to an extent where the velocity profiles collapse onto a profile characteristic of the pressure-gradient parameter describing the local flow, provided the parameter varies slowly along this flow. It is also reasonable to expect that the profiles in adverse pressure gradients should resemble some form of velocity-defect profile in the outer part of the boundary layer, provided the magnitude of the pressure gradient and injection rate can be successfully represented in such a velocity-defect law. Similarly, one would expect the deviation from some form of inner law to be a systematic and continuous function in the range of favourable pressure gradients through to adverse pressure gradients.

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From a comparison of these various forms of velocity profiles it is concluded that most of the other data considered have signs of incomplete development or only one or two profiles which resemble full development. It would seem that very few of the profiles of Julien or Loyd were near to full development, whereas most of the profiles of McQuad and Baker, apart from his favourable-adverse pressure gradient, appeared well developed for the velocity profiles, velocity defect and inner law profiles.

For zero injection, the velocity profiles of Peake *et al.* do not resemble developed profiles in adverse pressure gradients. Those of Voisinet *et al.* were clearly not in local equilibrium but provide well behaved inner law and wake component profiles. The profiles of Sivasegaram seem quite reasonable whenever the flow develops for sufficient length with slowly varying β . The developments of Michel *et al.* do not readjust to the local value of β after the initial larger pressure gradients. Although the inner law profiles of the strongest pressure gradient bear no linear region and are marked throughout by experimental fluctuation, it is not thought that relaminarisation has commenced in the down-stream stations since the value of β reduces very quickly to similar values in other flows.

It is not known how much emphasis can be placed on the ability of developed velocity profiles to reflect the magnitude of the individual pressure gradient. It would appear, however, that a parameter of a form similar, if not equal, to β can be used to indicate the shape of the velocity profile for zero injection. For injection into pressure gradient flows, β is unsuitable and a more appropriate parameter, for example, would be of the form $v_w/U_1 \cdot 2/C_f + \beta$, where β is the zero injection value and C_f is the value in the injected boundary layer.

The two prediction methods considered, have been shown to produce excellent overall agreement for the flows considered. For pressure-gradient flows with moderate injection rates where the magnitude of the pressure gradient changes relatively slowly, both methods can be considered reliable. For rapidly changing wall or free-stream conditions it is expected that most prediction methods will be inadequate, unless the semi-empirical functions employed, also reflect the rapid changes.

The poor agreement of the prediction methods with experiments for high injection rates in adverse pressure gradients is also expressed by Baker for freon injection, which produces density variations through the boundary layer.

The method adopted for measuring the skin-friction coefficient in compressible-flow pressure gradients, using razor blades which are calibrated in constant-pressure flows against the Spalding-Chi values is thought to provide C_f as accurately as any other method at present available. Comparing the results with those predicted by the two calculation methods shows that an estimate of the probable error is ± 5 per cent. This comparison also suggests that an estimate of the skin-friction in favourable pressure gradients with injection is possible. The particular method used does not apply to adverse pressure gradients but a similar method could be adopted for these.

Theoretical methods of obtaining C_f , such as the momentum integral equation or log-law plots are often unsuitable in pressure-gradient flows, especially with the presence of injection, and are liable to produce very large errors due to experimental fluctuations in the boundary-layer parameters and profiles. For flows where the profiles are close to local equilibrium the use of such methods for calculating C_f is probably outdated now that the development of prediction methods has progressed this far.

Considering the velocity profiles, velocity defect and inner-law profiles, it is thought that the overall development of the author's profile in pressure gradients is substantially complete.

It is concluded that the data of McQuaid, Baker and the author, in flows where the pressure gradient varies slowly, are the most reliable velocity profiles which are representative of fully developed profiles for their magnitude of pressure gradient.

The bulk of the data, with pressure gradients where the magnitude changes more rapidly, is probably of greater use to prediction methods for determining the variation of empirical functions with pressure-gradient magnitude when the flow changes so rapidly that it never achieves full development under local conditions.

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LIST OF SYMBOLS

а	Constant in razor-blade calibration
b	Constant in razor-blade calibration
В	Inner-law constant
C_{f}	Local skin-friction coefficient
C_{f0}	Skin-friction coefficient in equivalent zero injection flow
F	Injection parameter $\frac{\rho_w v_w}{\rho_1 U_1}$
G(u)	$= \int_0^u \frac{(\rho)^{\frac{1}{2}} du'}{(\tau_w + \rho_w v_w u')^{\frac{1}{2}}}$
h	Height of razor-blade from wall
k	Mixing-length constant
L_{\max}	Maximum value of mixing-length function, L, in the Bradshaw–Ferriss method
т	Injection-rate parameter $\frac{\rho_w v_w}{(\rho_1 U_1)_{ref}}$, where ref refers to the upstream constant-pressure value
М	Mach number
р	Pressure, static pressure
P_0	Stagnation pressure
r	Recovery factor
<i>r</i> 0	Recovery factor for zero-injection conditions
$R_{ heta}$	Reynolds number based on momentum thickness
Т	Temperature
и	Streamwise velocity
U_p	$= U_{\tau} \beta^{\frac{1}{2}}$
$U_{ au}$	= shearing velocity, $\left(\frac{\tau_w}{\rho_w}\right)^{\frac{1}{2}}$
U^*	$= \left(\frac{T_w}{T_1}\frac{d\theta}{dx}\right)^{\frac{1}{2}}U_1$
v	velocity component away from the wall
$w(y/\delta_c)$	Wake function in inner law, taken as $1 - \cos(\pi y/\delta_c)$
x	Distance along plate
X	Distance measured from first traverse of Gradients A, B
X'	Distance measured from first traverse of Gradient C
у	Distance from wall
<i>y</i> +	$=\frac{U_{\tau}y}{\tau_{w}}$
α	Constant in equation $\theta_i/\theta = 1 + \alpha M_1^2$
β	Pressure-gradient parameter $\frac{\delta_i^*}{\tau_w} \frac{dp}{dx}$

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δ	Boundary-layer thickness, taken as value of y when $\frac{u}{U_1} = 0.995$ unless otherwise stated
δ_c	Value of y where slope of inner-law profile is $1/k$ in outer part of the boundary layer
δ^*	Displacement thickness $\int_0^{\delta} \left(1 - \frac{\rho u}{\rho_1 U_1}\right) dy$
${oldsymbol{\delta}}^{*}_{i}$	Kinematic displacement thickness $\int_0^{\delta} \left(1 - \frac{u}{U_1}\right) dy$
ΔP	Difference between Stanton-tube pressure and wall static pressure
θ	Momentum thickness $\int_0^{\delta} \frac{\rho u}{\rho_1 U_1} \left(1 - \frac{u}{U_1}\right) dy$
$ heta_i$	Kinematic momentum thickness $\int_0^s \frac{u}{U_1} \left(1 - \frac{u}{U_1}\right) dy$
μ	Viscosity
μ_{273}	Reference viscosity at 273 K
ν	Kinematic viscosity
π	Pressure-gradient constant in wake component of inner law
ρ	Density
au	Shear stress
Subscripts	
1	Refers to conditions at edge of boundary layer
0	Refers to stagnation conditions
w	Refers to wall conditions

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The experimental results are presented in the following pages as Tables 1 and 2. The Tables are headed by the particular pressure gradients A, B or C and the respective injection rate, m.

TABLE 1Velocity and Temperature Profiles

								GRAD	IENT A-	-0.000					
X(mms)	0	12.7	25.4	38.1	50.8	63.5	76-2	88.9	101.6	114.3	127.0	139.7	152.4	165-1	177.8
	0.54	2.50	2.57	2.50	2.62	2.67	2.71	2.75	2.79	2.84	2.88	2.90	2.93	2.96	3.00
M_1	2.20	2.20	2.30	2.39	2.03	0.471	0.463	0.403	0.511	0.519	0.539	0.543	0.558	0.598	0.574
θ (mms)	0.424	0.435	1 200	0.4/9	1.022	0.471	2.160	2.248	2.377	2.478	2.587	2.695	2.814	2.942	2.937
ð (mms)	1.790	1.843	1.999	2.030	2.003	2-115	2.100	2 240	2 577	2 470					
Y(mms)	U/U_1	<i>U/U</i> ₁													
0.1	0.511	0.528	0.531	0.520	0.518	0.501	0.533	0.514	0.534	0.515	0.519	0.519	0.511	0.490	0.510
0.2	0.556	0.587	0.588	0.579	0.577	0.566	0.603	0.595	0.622	0.595	0.600	0.600	0.588	0.546	0.601
0.3	0.600	0.623	0.629	0.625	0.635	0.617	0.654	0.661	0.673	0.648	0.656	0.654	0.643	0.610	0.650
0.4	0.636	0.650	0.657	0.660	0.673	0.664	0.693	0.705	0.696	0.683	0.690	0.686	0.683	0.659	0.681
0.5	0.665	0.670	0.681	0.681	0.698	0.693	0.722	0.724	0.712	0.703	0.712	0.708	0.711	0.691	0.701
0.5	0.686	0.686	0.701	0.698	0.714	0.712	0.741	0.739	0.725	0.718	0.728	0.724	0.728	0.712	0-723
0.8	0.711	0.716	0.727	0.723	0.736	0.741	0.761	0.757	0.751	0.738	0.749	0.751	0.753	0.736	0.750
1.0	0.734	0.736	0.747	0.742	0.754	0.756	0.771	0.771	0.766	0.757	0.763	0.766	0.768	0.756	0.761
1.2	0.754	0.757	0.765	0.756	0.769	0.767	0.784	0.782	0.778	0.773	0.776	0.777	0.778	0.769	0.778
1.4	0,772	0.773	0.780	0.771	0.782	0.782	0.796	0.793	0.790	0.790	0.791	0.789	0.789	0.785	0.791
1.6	0.791	0.789	0.794	0.784	0.794	0.793	0.806	0.805	0.804	0.804	0.801	0.800	0.801	0.796	0.802
1.8	0.807	0.804	0.809	0.799	0.808	0.805	0.817	0.817	0.815	0.818	0.813	0.812	0.813	0.804	0-812
2.0	0.874	0.820	0.823	0.811	0.818	0.815	0.828	0.826	0.826	0.827	0.824	0.823	0.823	0.813	0.822
2.0	0.830	0.835	0.837	0.824	0.829	0.828	0.839	0.835	0.837	0.836	0.833	0.831	0.831	0.829	0.832
2.2	0.853	0.850	0.848	0.836	0.840	0.839	0.848	0.844	0.846	0.845	0.843	0.839	0.840	0.832	0-840
2.6	0.869	0.863	0.862	0.850	0.850	0.851	0.857	0.854	0.856	0.853	0.852	0.849	0.850	0.841	0.849
2.8	0.882	0.874	0.875	0.861	0.861	0.863	0.869	0.863	0.863	0.861	0.860	0.858	0.858	0.849	0.856
3.0	0.892	0.886	0.887	0.873	0.871	0.874	0.879	0.871	0.872	0.868	0.868	0.866	0.862	0.856	0.863
3.3	0.910	0.905	0.902	0.889	0.887	0.889	0.890	0.883	0.883	0.879	0.878	0.875	0.873	0.867	0.871
3.6	0.927	0.921	0.919	0.903	0.901	0.903	0.904	0.895	0.894	0.891	0.887	0.882	0.883	0.877	0.881
3.0	0.942	0.938	0.935	0.918	0.917	0.916	0.916	0.908	0.901	0.901	0.896	0.894	0-893	0.887	0.891
4.7	0.956	0.951	0.948	0.932	0.929	0.929	0.927	0.919	0.917	0.911	0.906	0.903	0.903	0.895	0.899
4.5	0.970	0.962	0.962	0.945	0.941	0.941	0.939	0.930	0.923	0.920	0.916	0.912	0.911	0.903	0.908
4.8	0.981	0.975	0.972	0.956	0.953	0.952	0.950	0.940	0.932	0.929	0.924	0.920	0.919	0.911	0.915
5.2	0.990	0.987	0.985	0.971	0.968	0.966	0.961	0.953	0.944	0.941	0.935	0.932	0.928	0.920	0.924
5.6	0.996	0.995	0.993	0.981	0.980	0.978	0.973	0.963	0.954	0.951	0.945	0.941	0.937	0.931	0.933
6.0	0.999	0.999	0.999	0.989	0.988	0.988	0.981	0.973	0.965	0.961	0.954	0.951	0.946	0.940	0.942
6.4	1.000	1.000	1.000	0.994	0.994	0.994	0.989	0.981	0.973	0.971	0.963	0.960	0.955	0.948	0.950
6.8	1 000	1 000	1 000	0.996	0.996	0.998	0.994	0.989	0.981	0.979	0.972	0.968	0.963	0.956	0.956
7.2				0.998	0.998	0.999	0.998	0.995	0.987	0.985	0.980	0.976	0.971	0.963	0.965
7.6				0.999	0.999	1.000	1.000	0.997	0.992	0.990	0.986	0.983	0.978	0.971	0.972
8.0				1.000	1.000			0.998	0.996	0.994	0.989	0.987	0.983	0.978	0.977
8.5								0.999	0.998	0.997	0.993	0.994	0.988	0.985	0-985
0.0								1.000	0.999	1.000	0.996	0.997	0.992	0.989	0.991
0.5									1.000		0.999	0.999	0.996	0.993	0.995
10.0											1.000	1.000	0-998	0.995	0.997
10.5													0.999	0-997	0.998
11.0													1.000	0.999	0-999
11.5														1.000	1.000
113															

TABLE 1 (Cont.)

$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$	
Y(mms) T/T_1 T/T_1 T/T_1 T/T_1 T/T_1 T/T_2	

	TABLE 1 (Cont.)														
X(mms)	0	12.7	25.4	38.1	50.8	63.5	76-2	GRAD 88·9	IENT A- 101·6	-0·001 114·3	127.0	139.7	152.4	165.1	
<u> </u>															
M_1	2.54	2.53	2.56	2.59	2.61	2.67	2.71	2.75	2.76	2.81	2.84 0.785	2.88 0.781	2·82	2·73 0·939	
θ (mms) δ^{x} (mms)	0·572) 2·497	2.509	0·578 2·476	0·592 2·543	2.777	2·910	0.639 3.037	3·269	3.437	3.532	3.759	3.948	4·102	4.175	
Y(mms)	U/U_1	U/U_1	U/U_1	U/U_1	<i>U</i> / <i>U</i> ₁	U/U_1	U/U_1	U/U_1	U/U_1	U/U_1	U/U_1	U/U_1	U/U_1	<i>U</i> / <i>U</i> ₁	
0.1	0.410	0.396	0.422	0.468	0.428	0.443	0.444	0-422	0.439	0.448	0.448	0.490	0.501	0.623	
0.2	0.451	0.439	0.461	0.512	0.474	0.489	0.497	0.489	0.494	0.492	0.497	0.524	0.530	0.631	
0.3	0.478	0.473	0.498	0.542	0.511	0.526	0.529	0.525	0.535	0.536	0.529	0.575	0.568	0.646	
0.4	0.498	0.501	0.528	0.567	0.521	0.556	0.558	0.553	0.594	0.502	0.578	0.502	0.583	0.652	
0.5	0.515	0.525	0.549	0.590	0.578	0.507	0.603	0.502	0.200	0.202	0.599	0.592	0.597	0.658	
0.6	0.534	0.576	0.507	0.634	0.610	0.627	0.631	0.624	0.632	0.634	0.630	0.635	0.622	0.668	
0.8	0.601	0.602	0.626	0.655	0.646	0.652	0.657	0.650	0.654	0.660	0.651	0.658	0.643	0.677	
1.2	0.630	0.627	0.651	0.674	0.670	0.674	0.675	0.671	0.674	0.682	0.673	0.678	0.662	0.687	
1.4	0.651	0.650	0.668	0.692	0.686	0.694	0.694	0.690	0.692	0.697	0.688	0.696	0.679	0.696	
1.6	0.675	0.672	0.688	0.707	0.701	0.708	0.710	0.705	0.706	0.713	0.705	0.713	0.693	0.706	
1.8	0.697	0.693	0.707	0.721	0.715	0.721	0.723	0.720	0.719	0.727	0.720	0.727	0.709	0.716	
2.0	0.717	0.714	0.727	0.737	0.729	0.734	0.737	0.732	0.728	0.739	0.734	0.739	0.718	0.726	
2.2	0.738	0.734	0.746	0.754	0.743	0.746	0.747	0.745	0.740	0.750	0.744	0.748	0.729	0.735	
2.4	0.756	0.753	0.763	0.768	0.756	0.759	0.760	0.754	0.752	0.760	0.753	0.756	0.739	0.744	
2.6	0.774	0.771	0.779	0.782	0.772	0.771	0.772	0.763	0.763	0.771	0.765	0.765	0.749	0.752	
2.8	0.792	0.789	0.795	0.795	0.785	0.782	0.783	0.775	0.772	0.779	0.704	0.705	0.758	0.770	
3.0	0.806	0.804	0.810	0.810	0.798	0.793	0.795	0.785	0.706	0.787	0.709	0.700	0.783	0.781	
3.3	0.832	0-830	0.833	0.830	0.817	0.811	0.812	0.801	0.010	0.010	0.207	0.811	0.704	0.792	
3.6	0.828	0.854	0.858	0.850	0.855	0.849	0.820	0.830	0.823	0.878	0.819	0.822	0.805	0.801	
3.9	0.880	0.877	0.8081	0.000	0.870	0.863	0.855	0.845	0.836	0.841	0.831	0.832	0.816	0.812	
4.2	0.901	0.017	0.016	0.005	0.888	0.880	0.874	0.860	0.850	0.852	0.843	0.843	0.828	0.823	
4.5	0.922	0.917	0.910	0.921	0.902	0.895	0.888	0.872	0.863	0.863	0.855	0.853	0.839	0.834	
5.7	0.961	0.956	0.953	0.944	0.924	0.916	0.906	0.889	0.879	0.878	0.871	0.868	0.851	0.846	
5.6	0.978	0.975	0.972	0.962	0.943	0.934	0.924	0.907	0.895	0.892	0.884	0.881	0.867	0.859	
6.0	0.990	0.984	0.986	0.977	0.959	0.953	0.939	0.924	0.910	0.908	0.896	0.894	0.877	0.870	
6.4	0.995	0.994	0.995	0.989	0.974	0.967	0.954	0.940	0.925	0.920	0.910	0.906	0.889	0.881	
6.8	0.997	0.997	0.998	0.996	0.984	0.980	0.968	0.954	0.938	0.934	0.921	0.919	0.900	0.891	
7.2	0.999	0.999	1.000	0.999	0.992	0.991	0.980	0.967	0.951	0.945	0.932	0.930	0.910	0.901	
7.6	1.000	1.000		1.000	0.996	0.996	0.990	0.977	0.964	0.957	0.944	0.941	0.920	0.911	
8.0					0.999	0-999	0.996	0.987	0.975	0.968	0.950	0.951	0.042	0.033	
8.5					1.000	1.000	0.999	0.995	0.985	0.979	0.909	0.902	0.945	0.933	
9.0							1.000	1 000	0.004	0.987	0.087	0.081	0.950	0.942	
9.5								1.000	0.990	0.006	0.987	0.981	0.977	0.964	
10.0									0.330	0.998	0.995	0.993	0.986	0.972	
10.5									1.000	0.999	0.997	0.996	0.993	0.982	
11.0									1 000	1.000	0.999	0.999	0.996	0.987	
12.0										0	1.000	1.000	0.999	0.991	
12.0													1.000	0.995	
13.0														0.997	
13.5														0.999	
14.0														1.000	

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TABLE 1 (Cont.)

X(mms)	0	12.7	25.4	38.1	50.8	63.5	76.2	GRAI 88-9	DIENT A 101.6	-0.001 114.3	127.0	139.7	152.4	165.1	
<i>M</i> ₁	2.54	2.53	2.56	2.59	2.61	2.67	2.71	2.75	2.76	2.81	2.84	2.88	2.82	2.73	
R_{θ}	27500	28000	27200	27300	29500	28900	29100	29900	31700	31300	32100	32100	36300	41000	
T_w/T_1	2.198	2.176	2.204	2.243	2.264	2.345	2.376	2.417	2.418	2.479	2.503	2.578	2.479	2.379	
Y(mms)	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	
0.1	2.028	2.020	2.024	2.011	2.076	2.134	2.155	2.211	2.199	2.245	2.247	2.268	2.158	1.906	
0.2	1.970	1.968	1.970	1.947	2.010	2.066	2.079	2.121	2.113	2.170	2.166	2.202	2.108	1.884	
0.3	1.927	1.920	1.915	1.895	1.953	2.004	2.023	2.056	2.041	2.094	2.106	2.144	2.066	1.862	
0.4	1.050	1.875	1.807	1.848	1-925	1.949	1.022	2.001	1.985	2.040	2.053	2.094	2.028	1.842	
0.5	1.030	1.800	1.702	1.762	1.889	1.904	1.922	1.954	1.937	1.992	2.006	2.049	1.993	1.824	
0.0	1.763	1.746	1.721	1.702	1.744	1.700	1.000	1.915	1.898	1.942	1.007	2.009	1.958	1.805	
1.0	1.716	1.700	1.683	1.662	1.603	1.732	1.740	1.777	1.772	1.803	1.002	1.937	1.901	1.725	
1.2	1.675	1.664	1.647	1.628	1.651	1.680	1.707	1.735	1.732	1.752	1.784	1.827	1.049	1.710	
1.4	1.645	1.632	1.617	1.598	1.622	1.651	1.672	1.700	1.697	1.710	1.740	1.780	1.771	1,688	
1.6	1.611	1.601	1.586	1.574	1.598	1.626	1.644	1.670	1.670	1.681	1.711	1.740	1.740	1.668	
1.8	1.577	1.569	1.556	1.551	1.575	1.600	1.616	1.642	1.647	1.654	1.681	1.720	1.707	1.646	
2.0	1.546	1.539	1.528	1.524	1.551	1.577	1.591	1.619	1.624	1.630	1.654	1.692	1.689	1.625	
2.2	1.516	1.510	1.498	1.498	1.528	1.555	1.570	1.594	1.602	1.605	1.633	1.671	1.664	1.609	
2.4	1.487	1.478	1.469	1.474	1.506	1.530	1.547	1.575	1.578	1-584	1.610	1.651	1.643	1.591	
2.6	1.458	1.448	1.444	1.450	1.481	1.508	1.523	1.553	1.556	1.560	1.586	1.632	1.624	1.573	
2.8	1.429	1.423	1.418	1.429	1.458	1.488	1.503	1.529	1.537	1.544	1.567	1.610	1.603	1.555	
3.0	1.404	1.396	1.390	1.403	1.434	1.466	1.478	1.511	1.515	1.526	1.545	1.583	1.581	1.538	
3.3	1.363	1.352	1.353	1.366	1.382	1.432	1.444	1.477	1.488	1.492	1.515	1.551	1.548	1.515	
3.6	1.314	1.310	1.309	1.330	$1 \cdot 441$	1.397	1.416	1.445	1.459	1.460	1.493	1.521	1.520	1.494	
3.9	1.271	1.270	1.266	1.295	1.335	1.361	1.387	1.419	1.433	1.437	1-468	1.494	1.496	1.476	
4.2	1.230	1.229	1.232	1.261	1.302	1.329	1.353	1.388	1.403	1.408	1.440	1.469	1.471	1.454	
4.5	1.189	1.193	1.199	1.228	1.266	1.299	1.318	1.355	1.377	1.382	1.412	1.444	1.441	1.430	
4.8	1.149	1.153	1.165	1.195	1.236	1.264	1.285	1.330	1.350	1.358	1.384	1.418	1.414	1.407	
5.2	1.056	1.001	1.116	1.145	1.188	1.224	1.248	1.291	1.312	1.327	1.350	1.384	1.386	1.382	
5·0 6.0	1.025	1.025	1.027	1.067	1.146	1.147	1.209	1.255	1.281	1.297	1.319	1.351	1.351	1.353	
6.4	1.012	1.016	1.011	1.029	1.060	1.112	1.142	1.192	1.245	1.200	1.291	1.318	1.322	1.325	
6.8	1,008	1.003	1.002	1.010	1.020	1.078	1.109	1.146	1.101	1.100	1.220	1.288	1.293	1.301	
7.2	1.002	1.003	1,002	1.019	1.010	1.050	1.078	1.115	1.150	1.171	1.202	1.220	1.240	1.256	
7.6	1.001	1.000	1 000	1.003	1.007	1.031	1.048	1.080	1.110	1.1/0	1.177	1.202	1.242	1.720	
8.0	1.000	1 000		1.002	1.007	1.017	1.028	1.061	1.087	1.112	1.146	1.175	1,180	1.210	
8.5	1 000			1.000	1.000	1.008	1.012	1.032	1.057	1.079	1.112	1.143	1.157	1.182	
9.0				1 000	1 000	1.004	1.005	1.016	1.038	1.054	1.080	1.114	1.124	1.160	
9.5						1.003	1.002	1.006	1.019	1.034	1.055	1.086	1.099	1.136	
10.0						1.002	1.000	1.002	1.008	1.020	1.037	1.062	1.074	1.112	
0.5						1.001		1.000	1.003	1.010	1.023	1.042	1.051	1.087	
1.0						1.000			1.001	1.003	1.012	1.027	1.033	1.062	
1.5									1.000	1.001	1.009	1.017	1.018	1.050	
2.0										1.000	1.002	1.009	1.011	1.034	
2.5											1.001	1.005	1.006	1.025	
3.0											1.000	1.003	1.003	1.018	
3.5												1.002	1.002	1.012	
4.0												1.000	1.000	1.008	
5.0														1.002	
6.0															

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TABLE 1 (Cont.)

Virmms 0 127 254 81 198 635 762 889 1016 1143 1270 1297 Mmm 0.655 0.659 0.738 0.770 0.808 0.810 0.81													
$ \begin{array}{c c c c c c c c c c c c c c c c c c c $									GRAE	IENT A.	_0.002		
Atoms 0 127 234 54 54 54 54 55 128 127 127 128 127 127 127 128 127 127 128 127 128 <th128< th=""> 128 <th128< th=""></th128<></th128<>	1 <i>I</i> ()	0	10.7	25.4	20.1	50.0	62.5	76.0	00.0	101.6	114.3	127.0	130.7
Math 0 2:55 0:48 0:47 0:77 0:80 0:77 0:	X (mms)	0	12.7	25.4	38.1	20.9	03.3	70.2	00.9	101-0	114.3	127.0	155.1
MA 2:53 2:54 2:55 2:58 2:61 2:60 2:70 2:68 2:61 2:67 2:70 0:83 4:40 4:90 5:87 Y (mms) U/U U/								0.50	2.72	0.77	0.01	2.02	0.07
$ \begin{array}{c} d(\mathrm{nms}) \ 0.655 \ 0.680 \ 0.738 \ 0.779 \ 0.808 \ 0.812 \ 0.870 \ 0.934 \ 0.939 \ 0.990 \ 0.990 \ 0.997 \ 0.$	M_1	2.53	2.54	2.55	2.58	2.61	2.67	2.70	2.12	2.11	2.81	2.83	2.91
8 (mms) 3.650 3.194 3.407 3.523 3.720 3.883 4.041 4.402 4.432 4.704 4.704 5.787 Y(mms) U/U, U/U, <td>θ (mms)</td> <td>0.652</td> <td>0.689</td> <td>0.738</td> <td>0.779</td> <td>0.808</td> <td>0.812</td> <td>0.870</td> <td>0.934</td> <td>0.939</td> <td>0.967</td> <td>0.976</td> <td>1.0/1</td>	θ (mms)	0.652	0.689	0.738	0.779	0.808	0.812	0.870	0.934	0.939	0.967	0.976	1.0/1
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	δ (mms)	3.050	3.194	3.407	3.523	3.720	3-853	4.041	4.402	4.535	4.704	4-910	5-387
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$													
	Y(mms)	U/U_1											
12 0.332 0.438 0.436 0.403 0.432 0.432 0.432 0.432 0.432 0.432 0.432 0.432 0.432 0.432 0.432 0.432 0.443 0.443 0.443 0.443 0.443 0.443 0.443 0.443 0.443 0.443 0.443 0.441 0.443 0.441 0.443 0.441 0.443 0.441 0.443 0.441 0.443 0.441 0.443 0.441 0.443 0.441 0.443 0.441 0.443 0.441 0.443 0.441 0.443 0.441 0.443 0.441 0.443 0.441 0.443 0.441 0.443 0.441 0.443 0.441 0.443 0.441 0.443 0.441 0.453 0.443 0.441 0.453 0.443 0.441 0.453 0.443 0.441 0.453 0.441 0.453 0.441 0.453 0.441 0.453 0.441 0.453 0.441 0.453 0.441 0.453 0.441 0.	0.1	0.304	0.320	0.314	0.346	0.330	0.350	0.353	0.316	0.344	0.336	0.346	0.315
0 0.367 0.408 0.448 0.447 0.448 0.447 0.448 0.448 0.448 0.448 0.4 0.449 0.448 0.442 0.448 0.442 0.448 0.548 0.552 <td>0.2</td> <td>0.337</td> <td>0.358</td> <td>0.366</td> <td>0.396</td> <td>0.378</td> <td>0.403</td> <td>0.402</td> <td>0.362</td> <td>0.394</td> <td>0.384</td> <td>0.392</td> <td>0.360</td>	0.2	0.337	0.358	0.366	0.396	0.378	0.403	0.402	0.362	0.394	0.384	0.392	0.360
0 0 0 0 4 0 4 0 4 0 4 0 4 0 4 0 4 0	0.2	0.367	0.300	0.405	0.430	0.417	0.444	0.445	0.417	0.428	0.453	0.428	0.404
0-3 0-37 0-473 0-476 0-476 0-477 0-481 0-485 0-485 0-485 0-485 0-485 0-485 0-485 0-485 0-485 0-485 0-485 0-485 0-485 0-485 0-485 0-485 0-485 0-485 0-485 0-530 0-507 0 0.522 0-521 0-531 0-530 0-530 0-530 0-530 0-531 0-530 0-531 0-530 0-531 0-530 0-531 0-530 0-531 0-530 0-531 0-530 0-531 0-530 0-531 0-530 0-531 0-530 0-531 0-530 0-531 0-530 0-531 0-530 0-531 0-530 0-531 0-531 0-530 0-531 0-531 0-530 0-531 0-531 0-530 0-531 0-530 0-531 0-530 0-531 0-530 0-531 0-530 0-531 0-530 0-531 0-530 0-531 0-530 0-531 0-530 0-531 0-531 0-531 0-531 0-531 0-531 0-531 0-531	0.4	0.200	0.417	0.442	0.459	0.442	0.474	0.473	0.456	0.461	0.480	0.459	0.437
03 0422 0443 0444 0443 <	0.4	0.399	0.442	0.472	0.470	0.472	0.502	0.407	0.484	0.401	0.504	0.485	0.456
0-60 0-430 0-430 0-430 0-430 0-230 0-230 0-234 0-234 0-447 0-447 0-448	0.5	0.427	0.443	0.495	0.476	0.407	0.505	0.516	0.504	0.506	0.525	0.504	0.474
08 0.490 0.498 0.516 0.527 0.534 0.536 0.536 0.537 1-0 0.522 0.527 0.541 0.549 0.558 0.560 0.576 0.576 0.584 0.536 0.537 1-2 0.566 0.570 0.582 0.600 0.610 0.562 0.576 0.584 0.536 1-4 0.569 0.570 0.581 0.593 0.662 0.610 0.618 0.611 0.585 1-60 0.614 0.625 0.663 0.663 0.664 0.646 0.644 0.642 2-0 0.633 0.663 0.663 0.664 0.664 0.664 0.664 0.664 2-4 0.679 0.671 0.670 0.672 0.668 0.662 0.670 0.671 0.670 0.714 0.669 2-4 0.679 0.671 0.670 0.720 0.700 0.718 0.717 0.714 0.707 0.714 0.707 0.714 0.707 0.714 0.707 0.714 0.727 0.737 0.731 <td>0.0</td> <td>0.451</td> <td>0.400</td> <td>0.485</td> <td>0.490</td> <td>0.497</td> <td>0.520</td> <td>0.510</td> <td>0.500</td> <td>0.500</td> <td>0.525</td> <td>0.520</td> <td>0.507</td>	0.0	0.451	0.400	0.485	0.490	0.497	0.520	0.510	0.500	0.500	0.525	0.520	0.507
	0.8	0.490	0.498	0.516	0.527	0.529	0.201	0.554	0.530	0.545	0.228	0.539	0.507
1:2 0.546 0.549 0.561 0.570 0.582 0.600 0.6400 0.587 0.5984 0.5924 0.594 1:4 0.569 0.570 0.581 0.593 0.6612 0.611 0.652 0.627 0.604 0.627 0.606 1:8 0.617 0.612 0.631 0.632 0.632 0.633 0.643 0.644 0.654 0.644 0.644 0.644 0.645 0.643 0.624 2:0 0.633 0.643 0.647 0.666 0.666 0.6675 0.671 0.618 0.652 2:4 0.679 0.671 0.670 0.672 0.688 0.684 0.668 0.6677 2:4 0.679 0.671 0.670 0.712 0.700 0.718 0.717 0.770 0.706 0.788 0.714 0.698 0.477 2:4 0.640 0.777 0.771 0.770 0.718 0.714 0.714 0.714 0.714 0.714 0.714 0.714 0.714 0.714 0.714 0.727 0.731 <t< td=""><td>1.0</td><td>0.522</td><td>0.527</td><td>0.541</td><td>0.549</td><td>0.228</td><td>0.281</td><td>0.280</td><td>0.362</td><td>0.576</td><td>0.384</td><td>0.209</td><td>0.538</td></t<>	1.0	0.522	0.527	0.541	0.549	0.228	0.281	0.280	0.362	0.576	0.384	0.209	0.538
1:4 0.569 0.570 0.581 0.610 0.616 0.618 0.611 0.585 1:6 0.509 0.550 0.5610 0.611 0.622 0.632 0.647 0.642 0.643 0.642 1:8 0.617 0.612 0.613 0.643 0.640 0.661 0.652 0.637 0.624 2:0 0.653 0.643 0.643 0.646 0.661 0.655 0.637 2:4 0.679 0.671 0.670 0.670 0.670 0.670 0.670 0.671 0.670 0.671 0.670 0.671 0.670 0.671 0.670 0.671 0.670 0.671 0.670 0.671 0.707 0.718 0.771 0.774 0.733 0.744 0.735 0.744 0.735 0.744 0.735 0.744 0.736 0.736 0.756 0.731 0.746 0.741 0.738 0.744 0.734 0.738 0.744 0.737 0.741 0.711 0.711 0.756 0.737 3.9 0.810 0.804 0.786 <td< td=""><td>1.2</td><td>0.546</td><td>0.549</td><td>0.561</td><td>0.570</td><td>0.582</td><td>0.600</td><td>0.600</td><td>0.587</td><td>0.268</td><td>0.604</td><td>0.392</td><td>0.564</td></td<>	1.2	0.546	0.549	0.561	0.570	0.582	0.600	0.600	0.587	0.268	0.604	0.392	0.564
1-6 0-590 0-592 0-590 0-610 0-617 0-612 0-623 0-637 0-627 0-606 2-0 0-638 0-630 0-633 0-643 0-640 0-646 0-646 0-643 0-643 2-0 0-638 0-630 0-633 0-643 0-647 0-662 0-630 0-631 0-642 2-4 0-679 0-671 0-670 0-672 0-684 0-668 0-665 0-663 0-653 2-8 0-717 0-705 0-695 0-700 0-716 0-722 0-709 0-707 0-718 0-714 0-664 0-642 0-643 0-644 0-644 0-644 0-645 0-647 0-647 0-647 0-647 0-647 0-647 0-647 0-647 0-647 0-647	1.4	0.569	0.570	0.581	0.593	0.602	0.617	0.619	0.605	0.616	0.618	0.611	0.585
1:8 0-617 0-612 0-614 0-623 0-633 0-634 0-646 0-646 0-646 0-647 2:0 0-658 0-650 0-653 0-653 0-653 0-653 0-653 0-653 2:4 0-679 0-671 0-670 0-670 0-670 0-670 0-670 0-670 0-670 0-688 0-688 0-684 0-681 0-665 2:4 0-679 0-671 0-700 0-700 0-700 0-688 0-688 0-684 0-667 0-665 2:4 0-717 0-707 0-700 0-710 0-710 0-700 0-666 0-710 0-714 0-688 3:0 0-733 0-720 0-700 0-711 0-710 0-714 0-738 0-732 0-730 0-731 0-714 0-738 0-742 0-731 0-741 0-738 0-742 0-731 0-741 0-736 0-741 0-731 0-741 0-731 0-741 0-731 0-741 0-731 0-741 0-731 0-741 0-731 0-741 0-731	1.6	0.590	0.592	0.596	0.610	0.617	0.631	0.634	0.620	0.632	0.637	0.627	0.606
2:0 0:638 0:630 0:643 0:647 0:662 0:650 0:650 0:650 2:4 0:679 0:670 0:670 0:670 0:670 0:671 0:670 0:662 2:4 0:679 0:671 0:670 0:670 0:672 0:688 0:668 0:661 0:665 2:6 0:698 0:688 0:682 0:666 0:700 0:690 0:666 0:700 0:671 0:716 0:673 3:6 0:726 0:720 0:700 0:712 0:700 0:717 0:713 0:714 0:717 0:713 0:724 0:725 0:720 0:700 0:714 0:713 0:724 0:725 0:720 0:700 0:714 0:714 0:713 0:724 0:721 0:714 0:714 0:714 0:714 0:714 0:714 0:714 0:714 0:714 0:714 0:714 0:714 0:725 0:726 0:726 0:726 0:726 0:726 0:726 0:726 0:726 0:726 0:726 0:726 0:727 0:771 0:771	1.8	0.617	0.612	0.614	0.625	0.633	0.647	0.650	0.636	0.646	0.646	0.643	0-624
2:2 0.659 0.650 0.658 0.658 0.674 0.667 0.668 0.652 2:4 0.679 0.671 0.670 0.672 0.688 0.688 0.688 0.688 0.688 0.668 0.668 0.668 0.670 0.672 0.707 0.705 0.675 0.700 0.712 0.709 0.706 0.707 0.705 0.753 0.714 0.711 0.716 0.714 0.738 0.728 0.712 0.736 0.737 0.711 0.711 0.710 0.716 0.712 0.730 0.714 0.711 0.711 0.716 0.711 0.716 0.711 0.716 0.711	2.0	0.638	0.630	0.633	0.643	0.647	0.660	0.662	0.650	0.661	0.658	0.655	0.637
2-4 0.679 0.671 0.670 0.670 0.672 0.688 0.686 0.670 0.684 0.681 0.665 2-6 0.698 0.689 0.688 0.682 0.668 0.700 0.707 0.706 0.668 2-8 0.717 0.707 0.705 0.695 0.700 0.712 0.709 0.696 0.710 0.707 0.706 0.688 3-0 0.738 0.726 0.720 0.730 0.723 0.723 0.723 0.724 0.711 0.714 0.698 3-3 0.766 0.753 0.735 0.734 0.741 0.774 0.771 0.756 0.754 3-9 0.819 0.800 0.766 0.758 0.774 0.771 0.771 0.761 0.754 0.761 0.754 0.761 0.774 0.771 0.771 0.750 4-5 0.861 0.823 0.827 0.826 0.812 0.776 0.771 0.771 0.770 5-6 0.947 0.929 0.930 0.881 0.881 0.881 <td>2.2</td> <td>0.659</td> <td>0.650</td> <td>0.653</td> <td>0.658</td> <td>0.659</td> <td>0.674</td> <td>0.674</td> <td>0.662</td> <td>0.675</td> <td>0.671</td> <td>0.668</td> <td>0.652</td>	2.2	0.659	0.650	0.653	0.658	0.659	0.674	0.674	0.662	0.675	0.671	0.668	0.652
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	2.4	0.679	0.671	0.670	0.670	0.672	0.688	0.686	0.673	0.688	0.684	0.681	0.665
12-8 0-717 0-707 0-700 0-712 0-709 0-696 0-710 0-707 0-706 0-688 3-0 0-738 0-726 0-720 0-709 0-714 0-710 0-717 0-714 0-698 3-3 0-766 0-733 0-725 0-720 0-704 0-712 0-717 0-713 0-712 0-717 3-6 0-794 0-777 0-773 0-773 0-724 0-714 0-738 0-742 0-727 3-9 0-819 0-800 0-776 0-771 0-771 0-771 0-774 0-738 0-744 0-771 0-771 0-771 4-2 0-846 0-829 0-800 0-797 0-774 0-774 0-771 0-771 0-771 4-5 0-871 0-852 0-831 0-819 0-806 0-809 0-797 0-784 0-774 0-771 0-776 5-2 0-922 0-904 0-881 0-847 0-880 0-845 0-831 0-816 0-816 0-816 0-823 0-797 <tr< td=""><td>2.6</td><td>0.698</td><td>0.689</td><td>0.688</td><td>0.682</td><td>0.686</td><td>0.700</td><td>0.699</td><td>0.686</td><td>0.700</td><td>0.697</td><td>0.694</td><td>0.677</td></tr<>	2.6	0.698	0.689	0.688	0.682	0.686	0.700	0.699	0.686	0.700	0.697	0.694	0.677
2.5 0 0.738 0.726 0.709 0.716 0.722 0.720 0.770 0.718 0.717 0.714 0.608 3.3 0.766 0.753 0.744 0.733 0.734 0.738 0.722 0.733 0.742 0.727 3.4 0.746 0.777 0.767 0.771 0.766 0.766 0.771	2.8	0.717	0.707	0.705	0.695	0.700	0.712	0.709	0.696	0.710	0.707	0.706	0.688
33 0.758 0.724 0.725 0.724 0.734 0.722 0.744 0.733 0.728 0.712 3-6 0.794 0.777 0.763 0.754 0.744 0.747 0.736 0.747 3-9 0.819 0.804 0.786 0.777 0.771 0.776 0.761 0.747 0.735 0.748 0.744 0.743	2.0	0.738	0.726	0.720	0.700	0.716	0.725	0.720	0.707	0.718	0.717	0.714	0.698
	2.2	0.766	0.753	0.744	0.735	0.734	0.743	0.738	0.722	0.734	0.733	0.728	0.712
3-9 0.794 0.777 0.703 0.704 0.704 0.724 0.761 0.762 0.727 0.721 4-2 0.846 0.829 0.809 0.776 0.771	3.3	0.700	0.777	0.762	0.756	0.754	0.761	0.747	0.738	0.748	0.746	0.742	0.727
3-9 0.819 0.804 0.780 0.777 0.771 0.771 0.771 0.771 0.771 0.771 4-2 0.846 0.829 0.809 0.778 0.782 0.782 0.764 0.771 0.771 0.770 4-5 0.871 0.852 0.831 0.819 0.806 0.809 0.797 0.781 0.784 0.782 0.776 0.770 5-2 0.922 0.904 0.881 0.863 0.849 0.843 0.816 0.816 0.814 0.809 0.783 5-6 0.947 0.929 0.904 0.881 0.883 0.881 0.851 0.835 0.831 0.823 0.797 6-0 0.968 0.952 0.928 0.914 0.906 0.890 0.867 0.851 0.835 0.811 0.851 0.845 0.813 0.841 0.845 0.837 0.827 6-4 0.994 0.988 0.952 0.934 0.922 0.890 0.867 0.851 0.845 0.811 0.840 0.841 0.840 0.84	3.0	0.794	0.004	0.705	0.777	0.771	0.776	0.761	0.754	0.761	0.750	0.756	0.737
4-2 0.846 0.829 0.809 0.790 0.781 0.781 0.771 0.771 0.770 4-5 0.871 0.852 0.831 0.880 0.800 0.797 0.781 0.778 0.774 0.770 5-2 0.922 0.904 0.881 0.863 0.849 0.848 0.834 0.816 0.816 0.814 0.809 0.777 5-6 0.922 0.904 0.881 0.863 0.849 0.848 0.831 0.823 0.831 0.823 0.778 6-0 0.968 0.952 0.928 0.914 0.893 0.887 0.871 0.851 0.829 0.823 0.781 6-4 0.985 0.972 0.934 0.925 0.906 0.881 0.845 0.851 0.851 0.849 0.845 0.827 6-8 0.994 0.988 0.968 0.952 0.931 0.922 0.939 0.921 0.923 0.914 0.904 0.881 0.874 0.864 0.841 7-2 0.999 0.990 0.925 <td>3.9</td> <td>0.019</td> <td>0.004</td> <td>0.000</td> <td>0.706</td> <td>0.729</td> <td>0.700</td> <td>0.701</td> <td>0.769</td> <td>0.774</td> <td>0.771</td> <td>0.771</td> <td>0.750</td>	3.9	0.019	0.004	0.000	0.706	0.729	0.700	0.701	0.769	0.774	0.771	0.771	0.750
4-5 0.871 0.812 0.813 0.819 0.806 0.797 0.797 0.797 0.770 5-2 0.922 0.904 0.881 0.863 0.849 0.826 0.812 0.796 0.800 0.797 0.797 0.770 5-2 0.922 0.904 0.881 0.863 0.849 0.848 0.831 0.812 0.797 0.797 0.770 5-2 0.922 0.904 0.881 0.863 0.849 0.841 0.814 0.800 0.797 0.771 6.0 0.968 0.952 0.928 0.914 0.886 0.871 0.851 0.849 0.845 0.837 0.813 6.4 0.995 0.922 0.933 0.914 0.906 0.887 0.871 0.851 0.849 0.845 0.831 0.874 0.861 0.873 0.855 7.6 1.000 0.999 0.991 0.982 0.966 0.948 0.933 0.914 0.904 0.882 8.5 0.999 0.990 0.992 0.997 0.983 <td>4.2</td> <td>0.846</td> <td>0.829</td> <td>0.809</td> <td>0.790</td> <td>0.788</td> <td>0.792</td> <td>0.702</td> <td>0.700</td> <td>0.709</td> <td>0.701</td> <td>0.702</td> <td>0.761</td>	4.2	0.846	0.829	0.809	0.790	0.788	0.792	0.702	0.700	0.709	0.701	0.702	0.761
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	4.5	0.8/1	0.822	0.831	0.819	0.806	0.809	0.797	0.781	0.700	0.704	0.704	0.701
	4.8	0.892	0.873	0.854	0.839	0.827	0.826	0.812	0.796	0.800	0.797	0.794	0.7/0
5-6 0-947 0-929 0-904 0-888 0-874 0-868 0-823 0-197 6-0 0-968 0-952 0-928 0-914 0-893 0-887 0-811 0-851 0-849 0-823 0-813 6-4 0-985 0-972 0-9050 0-935 0-914 0-906 0-880 0-867 0-865 0-861 0-823 0-827 6-8 0-994 0-988 0-968 0-952 0-904 0-922 0-904 0-883 0-881 0-874 0-864 0-841 7-2 0-999 0-990 0-982 0-969 0-992 0-992 0-990 0-982 0-969 0-953 0-912 0-923 0-911 0-887 0-864 0-841 7-6 1-000 0-995 0-991 0-982 0-970 0-952 0-931 0-923 0-914 0-904 0-882 8-0 1-000 0-992 0-984 0-935 0-931 0-920 0-897 0-912 9-5 1-000 0-999 0-996 0-997 0-991 </td <td>5.2</td> <td>0.922</td> <td>0.904</td> <td>0.881</td> <td>0.863</td> <td>0.849</td> <td>0.848</td> <td>0.834</td> <td>0.816</td> <td>0.816</td> <td>0.814</td> <td>0.809</td> <td>0.783</td>	5.2	0.922	0.904	0.881	0.863	0.849	0.848	0.834	0.816	0.816	0.814	0.809	0.783
	5.6	0.947	0.929	0.904	0.888	0.874	0.868	0.851	0.835	0.831	0.829	0.823	0.797
	6.0	0.968	0.952	0.928	0.914	0.893	0.887	0.871	0.851	0.849	0.845	0.837	0.813
	6.4	0.985	0.972	0.950	0.935	0.914	0.906	0.890	0.867	0.865	0.861	0.820	0.827
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	6.8	0.994	0.988	0.968	0.952	0.934	0.925	0.906	0.883	0.881	0.874	0.864	0.841
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	7.2	0.999	0.997	0.981	0.969	0.953	0.942	0.922	0.899	0.894	0.887	0.879	0.855
$ \begin{array}{ccccccccccccccccccccccccc$	7.6	1.000	0.999	0.990	0.982	0.969	0.957	0.938	0.915	0.909	0.901	0.891	0.869
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	8.0		1.000	0.995	0.991	0.982	0.970	0.952	0.931	0.923	0.914	0.904	0.882
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	8.5			0.999	0.996	0.992	0.983	0.968	0.948	0.938	0.931	0.920	0.897
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	9.0			1.000	0.998	0.996	0.991	0.982	0.964	0.954	0.945	0.935	0.912
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	0.5			1 000	1.000	0.000	0.997	0.990	0.977	0.968	0.959	0.949	0.927
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	10.0				1 000	1.000	0.000	0.996	0.985	0.979	0.970	0.961	0.940
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	10.5					1 000	1.000	0.008	0.001	0.988	0.979	0.974	0.954
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	11.0						1.000	0.000	0.006	0.003	0.087	0.984	0.966
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	11.0							1.000	0.000	0.007	0.007	0.007	0.977
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	11.2							1.000	1.000	0.000	0.005	0.000	0.086
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	12.0								1.000	1.000	0.993	1.000	0.200
13.0 1.000 0.995 13.5 0.998 14.0 0.999 15.0 1.000	12.5									1.000	0.999	1.000	0.005
13.5 0.998 14.0 0.999 15.0 1.000	13.0										1.000		0.000
14·0 15·0 0·999 1·000	13.5												0.998
15.0 1.000	14.0												0.999
	15.0												1.000

TABLE 1 (Cont.)

								GPAT	JENT A				 	 	
X(mms)	0	12.7	25.4	38.1	50-8	63.5	76-2	88·9	101.6	114.3	127.0	139.7			
<u> </u>	2.52	0.5:				• · -							 	 	
M_1	2.53	2.54	2.55	2.58	2.61	2.67	2.70	2.72	2.77	2.81	2.83	2.87			
T_{m}/T_{1}	2.229	2.246	2.284	2.287	2.328	38400 2.411	2.304	41800	41300	41400	41200	44400			
					2 520	2 411	2 374	2.422	2.400	2.320	2.343	2.373	 		
Y(mms)	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1			
0.1	2.107	2.108	2.140	2.132	2.178	2.248	2.224	2.283	2.319	2.357	2.376	2-429	 	 	
0.2	2.059	2.056	2.076	2.073	2.115	2.178	2.156	2.224	2.253	2.293	2-315	2.374			
0.3	2.015	2.013	2.019	2.024	2.054	2.113	2.098	2.155	2.201	2.200	2.259	2.313			
0.4	1.976	1.976	1.972	1.977	2.013	2.066	2.053	2.101	2.152	2.152	2.208	2.259			
0.5	1.010	1.009	1.932	1.940	1.96/	2.014	2.013	2.056	2.103	2.108	2.161	2.222			
0.8	1.864	1.862	1.866	1.862	1.880	1.005	1.005	2.016	2.066	2.066	2.124	2.187			
1.0	1.823	1.823	1.827	1.826	1.832	1.863	1.905	1.930	1.027	1.024	2.049	2.115			
1.2	1.794	1.791	1.802	1.791	1.796	1.826	1.822	1.854	1.883	1.802	1.032	2.041			
1.4	1.762	1.766	1.772	1.754	1.763	1.796	1.788	1.821	1.849	1.864	1.894	1.947			
1.6	1.735	1.738	1.751	1.729	1.742	1.772	1.759	1.795	1.822	1.838	1.863	1.911			
1.8	1.699	1.710	1.723	1.704	1.717	1.745	1.731	1.769	1.795	1.809	1.832	1.878			
2.0	1.667	1.683	1.696	1.677	1.693	1-722	1.712	1.744	1.766	1.788	1.810	1.851			
2.2	1.637	1.654	1.668	1.655	1.675	1.696	1.692	1.723	1.737	1.763	1.784	1.823			
2.4	1.608	1.623	1.643	1.637	1.655	1.672	1.668	1.700	1.713	1.734	1.757	1.796			
2.0	1.579	1.597	1.614	1.614	1.633	1.650	1.646	1.676	1.690	1.711	1.733	1.772			
2.0	1.520	1.540	1.569	1.593	1.610	1.630	1.627	1.659	1.668	1.693	1.711	1.751			
3.3	1.320	1.500	1.526	1.522	1.540	1.570	1.575	1.639	1.652	1.672	1.692	1.731			
3.6	1.432	1.459	1.403	1.332	1.549	1.538	1.550	1.570	1.505	1.637	1.662	1.703			
3.9	1.386	1.415	1.454	1.461	1.488	1.510	1.533	1.549	1.560	1.583	1.605	1.649			
4-2	1.341	1.372	1.417	1.427	1.457	1.480	1.492	1.526	1.543	1.559	1.574	1.621			
4.5	1.296	1.333	1.377	1.389	1.425	1.447	1.463	1.501	1.514	1.532	1.550	1.597			
4.8	1.255	1.294	1.333	1.356	1.388	1.416	1.432	1.471	1.489	1.504	1.518	1.578			
5.2	1.194	1.233	1.286	1.309	1.345	1.372	1.391	1.433	1.455	1.467	1.490	1.550			
5.6	1.137	1.183	1.239	1.261	1.301	1.331	1.356	1.394	1.422	1.435	1.460	1.518			
6·0	1.088	1.128	1.188	1.212	1.261	1.290	1.318	1.365	1.387	1.400	1.427	1.483			
0·4 6.9	1.010	1.020	1.138	1.120	1.221	1.253	1.280	1.331	1.352	1.366	1.400	1.451			
7.2	1.008	1.020	1.056	1.027	1.125	1.172	1.245	1.296	1.316	1.336	1.369	1.418			
7.6	1.001	1.006	1.032	1.054	1.008	1.136	1.177	1.200	1.285	1.306	1.335	1.388			
8.0	1.000	1.002	1.014	1.032	1.066	1.103	1.141	1.194	1.223	1.245	1.275	1.326			
8.5		1.000	1.006	1.015	1.036	1.069	1.100	1.154	1.184	1.245	1.273	1.288			
9.0			1.001	1.005	1.019	1.039	1.066	1.117	1.146	1.172	1.200	1.253			
9.5			1.000	1.002	1.008	1.022	1.038	1.078	1.110	1.138	1.165	1.216			
10.0				1.000	1.001	1.010	1.018	1.054	1.078	1.106	1-133	1.181			
10.5					1.000	1.004	1.008	1.033	1.055	1-077	1.103	1.144			
11.5						1.001	1.002	1.018	1.032	1.052	1.077	1.116			
12.0						1.000	1.000	1.010	1.018	1.035	1.049	1.086			
12.0								1.000	1.008	1.021	1.033	1.057			
13.0								1.000	1.004	1.007	1.012	1.039			
13.5									1,000	1.007	1.009	1.019			
14.0									1 000	1.002	1.006	1.014			
15.0										1.000	1.002	1.008			
16.0										- 000	1.001	1.004			
17.0											1.000	1.002			
18.0												1.001			
19.0															

TABLE 1 (Cont.)

X (mms)	0	12.7	25.4	38.1	50.8	63.5	76·2	GRAD 88-9	IENT B- 101·6	-0.000 114.3	127.0	139.7	152-4	165.1	177-8
$\frac{M_1}{\theta(\text{mms})}$ $\delta^{x}(\text{mms})$	2·52 0·496) 2·018	2·52 0·474 2·027	2·53 0·450 1·913	2·52 0·456 1·933	2·48 0·455 1·920	2·45 0·469 2·004	2·44 0·496 2·033	2·41 0·513 2·059	2·39 0·517 2·059	2·34 0·566 2·216	2·33 0·538 2·185	2·30 0·593 2·218	2·28 0·604 2·228	2·27 0·615 2·258	2·21 0·680 2·500
Y(mms)	<i>U</i> / <i>U</i> ₁	U/U_1	U/U_1	U/U_1	U/U1	U/U_1	<i>U</i> / <i>U</i> ₁	<i>U</i> / <i>U</i> ₁	U/U_1	U/U_1	U/U_1	U/U_1	U/U_1	U/U_1	<i>U/U</i> ₁
$\begin{array}{c} 0.1 \\ 0.2 \\ 0.3 \\ 0.4 \\ 0.5 \\ 0.6 \\ 0.8 \\ 1.0 \\ 1.2 \\ 1.4 \\ 1.6 \\ 1.8 \\ 2.0 \\ 2.2 \\ 2.4 \\ 2.6 \\ 2.8 \\ 3.0 \\ 3.3 \\ 3.6 \\ 3.9 \\ 4.5 \\ 4.8 \\ 5.2 \\ 5.6 \\ 6.0 \\ 6.4 \\ 6.8 \\ 7.2 \end{array}$	0.498 0.558 0.605 0.636 0.660 0.674 0.702 0.722 0.741 0.758 0.775 0.789 0.802 0.816 0.829 0.843 0.856 0.867 0.883 0.901 0.917 0.931 0.917 0.935 0.968 0.925 0.968 0.992 0.991 0.997 1.000	0.532 0.578 0.622 0.648 0.668 0.668 0.668 0.711 0.749 0.763 0.777 0.791 0.805 0.819 0.831 0.846 0.858 0.870 0.888 0.906 0.922 0.936 0.921 0.961 0.975 0.986 0.992 0.998 1.000	0.531 0.531 0.589 0.626 0.657 0.678 0.693 0.720 0.738 0.757 0.774 0.787 0.803 0.817 0.830 0.844 0.856 0.868 0.882 0.899 0.915 0.930 0.945 0.935 0.9957 0.969 0.991 0.997 1.000	0.539 0.606 0.640 0.663 0.681 0.698 0.720 0.738 0.756 0.771 0.786 0.801 0.814 0.827 0.840 0.855 0.868 0.879 0.896 0.913 0.930 0.944 0.956 0.967 0.980 0.990 0.995 0.998 1.000	0.528 0.528 0.578 0.610 0.635 0.654 0.672 0.698 0.719 0.737 0.754 0.771 0.754 0.771 0.786 0.803 0.819 0.833 0.848 0.862 0.875 0.888 0.914 0.931 0.949 0.994 0.997 0.998 1.000	0.527 0.527 0.582 0.613 0.638 0.660 0.700 0.721 0.738 0.755 0.773 0.785 0.825 0.825 0.845 0.845 0.856 0.870 0.881 0.905 0.924 0.925 0.905 0.905 0.905 0.908 0.998 1.000	0.513 0.572 0.607 0.629 0.647 0.664 0.689 0.711 0.730 0.749 0.763 0.779 0.763 0.779 0.763 0.779 0.763 0.779 0.763 0.820 0.833 0.846 0.881 0.889 0.917 0.932 0.948 0.961 0.976 0.988 0.995 0.999 1.000	0.518 0.577 0.603 0.625 0.644 0.655 0.684 0.706 0.724 0.744 0.758 0.774 0.748 0.774 0.788 0.804 0.832 0.844 0.858 0.878 0.878 0.878 0.878 0.878 0.895 0.912 0.929 0.943 0.955 0.9970 0.984 0.997 0.9997 0.9991 1.000	0.558 0.599 0.625 0.645 0.645 0.660 0.676 0.698 0.712 0.727 0.743 0.757 0.772 0.743 0.757 0.772 0.787 0.787 0.801 0.814 0.828 0.842 0.864 0.873 0.892 0.909 0.925 0.941 0.955 0.971 0.983 0.992 0.997 0.998 0.999	0.501 0.568 0.607 0.627 0.645 0.658 0.680 0.698 0.712 0.725 0.741 0.725 0.741 0.755 0.768 0.780 0.794 0.808 0.833 0.852 0.833 0.852 0.833 0.852 0.833 0.852 0.871 0.924 0.924 0.924 0.924 0.925 0.995 0.999 1.000	0.533 0.583 0.614 0.634 0.651 0.668 0.707 0.722 0.738 0.752 0.766 0.780 0.793 0.805 0.805 0.817 0.831 0.844 0.862 0.881 0.884 0.915 0.928 0.928 0.928 0.946 0.964 0.964 0.992 0.997 0.999 1.000	0.506 0.563 0.601 0.620 0.636 0.650 0.673 0.707 0.723 0.738 0.738 0.738 0.752 0.765 0.778 0.791 0.803 0.814 0.829 0.848 0.848 0.848 0.848 0.848 0.848 0.901 0.917 0.933 0.952 0.967 0.982 0.997 1.000	0.518 0.572 0.606 0.624 0.643 0.656 0.677 0.693 0.709 0.724 0.739 0.724 0.739 0.753 0.766 0.779 0.791 0.802 0.814 0.825 0.844 0.825 0.844 0.881 0.881 0.881 0.881 0.995 0.947 0.964 0.987 0.999	0.545 0.583 0.614 0.632 0.647 0.660 0.680 0.696 0.712 0.726 0.739 0.752 0.764 0.777 0.788 0.801 0.812 0.824 0.843 0.861 0.877 0.893 0.910 0.924 0.942 0.942 0.942 0.945 0.995 0.998	0.479 0.537 0.537 0.637 0.603 0.621 0.635 0.657 0.679 0.704 0.718 0.729 0.742 0.778 0.775 0.765 0.778 0.791 0.802 0.802 0.818 0.837 0.854 0.872 0.889 0.904 0.924 0.924 0.943 0.958 0.971 0.992
7.6 8.0 8.5 9.0 9.5									1.000				1.000	0.999 1.000	0·995 0·997 0·999 1·000

TABLE 1 (Cont.)

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X (mms)	0	12.7	25.4	38-1	50.8	63.5	76-2	GRA 88·9	DIENT I 101·6	3—0·000 114·3	127.0	139.7	152.4	165-1	177.8	,, <u>,,,</u> ,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,
<i>M</i> ₁	2-52	2.52	2.53	2.52	2.48	2.45	2.44	2.41	2.39	2.34	2.33	2.30	2.28	2.27	2.21	
R_{θ}	14200	14200	13100	13300	13600	14400	15100	16000	16500	18400	17900	19500	20000	20700	24000	
T_w/T_1	2.168	2.231	2.214	2.203	2.166	2.163	2.129	2.112	2.100	2.058	2.081	2.005	1.991	1.992	1.957	
Y(mms)	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1								
0.1	1.915	1.939	1.916	1.902	1.887	1.888	1.868	1.847	1.799	1.826	1.813	1.767	1.747	1.722	1.760	
0.2	1.835	1.868	1.829	1.798	1.813	1.815	1.785	1.769	1.739	1.744	1.747	1.699	1.684	1.675	1.702	
0.3	1.760	1.795	1.766	1.738	1.763	1.763	1.727	1.726	1.696	1.691	1.700	1.651	1.639	1.632	1.655	
0 ∙4	1.710	1.746	1.716	1.695	1.716	1.719	1.695	1.688	1.660	1.657	1.669	1.621	1-612	1.606	1.622	
0.5	1.670	1.705	1.675	1.659	1.679	1.681	1.667	1.654	1.632	1.627	1.637	1.597	1.582	1.582	1.597	
0.6	1.641	1.671	1.643	1.626	1.646	1.652	1.638	1.633	1.603	1.604	1.608	1.574	1.561	1.560	1.575	
0.8	1.589	1.611	1.588	1.581	1.599	1.604	1.590	1.583	1.562	1.563	1.571	1-535	1.524	1.523	1.543	
$1 \cdot 0$	1.547	1.567	1.545	1.543	1.557	1.563	1.551	1.543	1.533	1.532	1.541	1.507	1.498	1.496	1.511	
1.2	1.517	1.533	1.513	1.513	1.524	1.532	1.519	1.515	1.504	1.509	1.513	1.482	1.473	1.472	1.492	
1.4	1.488	1.506	1.483	1.485	1.495	1.503	1.485	1.484	1.497	1.487	1 - 488	1.461	1.453	1.449	1.473	
1.6	1.460	1.480	1.457	1.459	1.469	1.475	1.464	1.460	1.454	1.464	1.464	1.441	1.433	1.433	1.452	
1.8	1.437	1.454	1.430	1.433	1.441	1.451	1.437	1.437	1.432	1.441	1.443	1.419	1.412	1.412	1.438	
2.0	1.410	1.430	1.405	1.411	1.412	1.426	1.412	1.414	1.409	1.423	1.423	1.400	1.394	1.396	1.422	
2.2	1.386	1.404	1.380	1.387	1.384	1.401	1.393	1.390	1.387	1.402	1.403	1.382	1.376	1.379	1.404	
2.4	1.363	1.383	1.357	1.364	1.361	1.375	1.367	1.369	1.367	1.380	1.382	1.364	1.359	1.360	1.389	
2.6	1.340	1.356	1.333	1.337	1.335	1.347	1.346	1.340	1.344	1.359	1.364	1.347	1.340	1.341	1.373	
2.8	1.317	1.334	1.310	1.313	1.310	1.327	1.324	1.320	1.321	1.341	1.342	1.330	1.322	1.325	1.353	
3.0	1.297	1.311	1.284	1.290	1.286	1.303	1.300	1.297	1.286	1.320	1.322	1.308	1.306	1.307	1.338	
3.3	1.266	1.274	1.250	1.260	1.246	1.269	1.267	1.261	1.270	1.291	1.293	1.280	1.278	1.279	1.315	
3.6	1.232	1.240	1.219	1.224	1.212	1.238	1.233	1.233	1.238	1.264	1.258	1.253	1.251	1.253	1.288	
3.9	1.197	1.208	1.188	1.188	1.179	1.202	1.201	1.202	1.208	1.236	1.231	1.224	1.225	1.228	1.260	
4.2	1.166	1.174	1.154	1.160	1.144	1.168	1.169	1.171	1.178	1.206	1.201	1.100	1.107	1.204	1.236	
4.5	1.140	1.141	1.126	1.129	1.110	1.136	1.139	1.141	1.147	1.180	1.177	1.173	1.173	1.177	1.212	
4.8	1.110	1.111	1.091	1.098	1.076	1.107	1.110	1.116	1.120	1.140	1.144	1.146	1.140	1.15/	1.187	
5.2	1.072	1.073	1.057	1.061	1.045	1.071	1.075	1.076	1.085	1.113	1.112	1.111	1.117	1.125	1.155	
5.6	1.042	1.044	1.026	1.033	1.024	1.041	1.043	1.052	1.053	1.077	1.075	1.082	1.084	1.005	1.125	
6·0	1.016	1.024	1.011	1.014	1.013	1.020	1.022	1.027	1.032	1.048	1.049	1.051	1.058	1.065	1.008	
6.4	1.004	1.007	1.003	1.006	1.004	1.008	1.008	1.012	1.014	1.025	1.032	1,078	1.038	1.041	1.071	
6.8	1.000	1.001	1.000	1.003	1.001	1.001	1.004	1.005	1.006	1.010	1.018	1.017	1.015	1.022	1.042	
7.2	1 000	1.000	1 000	1.000	1.000	1.000	1.003	1.001	1.001	1.003	1.010	1.007	1.007	1.014	1.025	
7.6		1 000		1 000	1 000	1 000	1.000	1.000	1.000	1.002	1,006	1.007	1.007	1.007	1.016	
8.0							1 000	1 000	1.000	1.002	1.002	1.0002	1.002	1.002	1.000	
8.5										1.000	1.0002	1.000	1.002	1.000	1.003	
9.0											1.000		1.000	1.000	1.001	
9.5															1.000	
, ,															1.000	

TABLE 1 (Cont.)

						· · · · · · · · · · · ·										
V(mme)	٥	12.7	25.4	38.1	50.8	63.5	76.2	GRAI	DIENT B	-0.001	127.0	130.7	152.4	165.1	177.8	
A (mms)	U	12.7	23.4	20.1	50.8	05.5	70-2	00.9	101-0	114.5	127 0	1397	152 4	105 1	1// 0	
М.	2.51	2.50	2.55	2.48	2.46	2.44	2.41	2.39	2.38	2.35	2.32	2.27	2.28	2.27	2.19	
A(mms)	0.674	0.665	0.614	0.671	0.671	0.724	0.752	0.773	0.815	0.822	0.842	0.913	0.904	0.926	0.991	
$\delta^{\mathbf{x}}$ (mms)	2.877	2.905	2.689	2.941	2.975	2.007	3.152	3,164	3.310	3.321	3.397	3.523	3.502	3.596	3.767	
0 (mms)	2 011		2.007				5 152	5 104	5 510	5 521			5 502			
Y(mms)	U/U_1	U/U_1	U/U_1	U/U_1	U/U_1	U/U_1	U/U_1	U/U_1	U/U_1	U/U_1	U/U_1	U/U_1	U/U_1	U/U_1	U/U_1	
0.1	0.411	0.374	0.464	0.408	0.411	0.416	0.403	0.406	0.397	0.405	0.413	0.385	0.394	0.403	0.357	
0.2	0.444	0.403	0.485	0.434	0.445	0.448	0.433	0.435	0.437	0.442	0.444	0.419	0.438	0.450	0-390	
0.3	0.477	0.443	0.509	0.462	0.470	0.479	0.464	0.466	0-469	0.476	0.472	0.445	0.468	0.478	0.419	
0.4	0.502	0.473	0.530	0.492	0.494	0.501	0.487	0.484	0.485	0.495	0.494	0.466	0.490	0.507	0.443	
0.5	0.523	0.500	0.549	0.516	0.516	0.519	0.504	0.501	0.504	0.514	0.510	0.482	0.506	0.525	0.462	
0.6	0.540	0.519	0.566	0.534	0.532	0.534	0.517	0.516	0.517	0.533	0.521	0.495	0.518	0.536	0.478	
0.8	0.562	0.556	0.593	0.561	0.557	0.557	0.542	0.540	0.541	0.560	0.543	0.514	0.542	0.556	0.505	
1.0	0.594	0.584	0.617	0.585	0.578	0.578	0.561	0.560	0.562	0.573	0.562	0.531	0.556	0.573	0.527	
1.2	0.616	0.607	0.640	0.605	0.598	0.535	0.581	0.578	0.578	0.590	0.577	0.550	0.571	0.587	0.544	
1.4	0.635	0.628	0.660	0.624	0.613	0.613	0.500	0.594	0.593	0.602	0.592	0.563	0.587	0.598	0.559	
1.6	0.655	0.645	0.676	0.645	0.632	0.620	0.613	0.612	0.611	0.616	0.600	0.579	0.600	0.612	0.571	
1.9	0.673	0.661	0.604	0.662	0.651	0.647	0.630	0.625	0.624	0.631	0.625	0.503	0.612	0.627	0.584	
2.0	0.601	0.692	0.710	0.677	0.670	0.665	0.645	0.641	0.636	0.644	0.630	0.610	0.625	0.640	0.601	
2.0	0.7091	0.602	0.720	0.607	0.696	0.400	0.660	0.659	0.652	0.654	0.654	0.674	0.641	0.652	0.612	
2.2	0.700	0.090	0744	0.714	0.705	0.000	0.670	0.674	0.660	0.670	0.449	0.629	0.652	0.664	0.624	
2.4	0.724	0.725	0.744	0.722	0.703	0.090	0.070	0.601	0.605	0.070	0.600	0.650	0.667	0.676	0.620	
2.0	0.750	0.753	0.770	0.732	0.740	0.713	0.097	0.091	0.716	0.000	0.600	0.442	0.4007	0.690	0.651	
2.8	0.775	0.760	0.702	0.748	0.759	0.749	0.713	0.703	0.710	0.710	0.704	0.670	0.604	0.701	0.664	
3.0	0.705	0.705	0.793	0.700	0.738	0.771	0.750	0.725	0.726	0.772	0.706	0.600	0.094	0.701	0.695	
3.3	0.795	0.795	0.814	0.787	0.778	0.701	0.750	0.745	0.730	0.754	0.751	0.098	0.722	0.720	0.701	
3.0	0.818	0.817	0.837	0.809	0.804	0.794	0.773	0.700	0.701	0.734	0.770	0.719	0.750	0.741	0.701	
3.9	0.837	0.839	0.857	0.831	0.826	0.814	0.797	0.789	0.783	0.777	0.7/0	0.744	0.758	0.757	0.719	
4-2	0.858	0.858	0.877	0.854	0.848	0.833	0.817	0.812	0.804	0.796	0.791	0.764	0.778	0.777	0.742	
4.5	0.876	0.878	0.897	0.874	0.870	0.855	0.838	0.833	0.823	0.816	0.811	0.785	0.798	0.794	0.760	
4.8	0-897	0-898	0.917	0.894	0.889	0.867	0.859	0.856	0.845	0.835	0.830	0.805	0.817	0.813	0.780	
5.2	0.918	0.920	0.940	0.919	0.914	0.904	0.887	0.884	0.871	0.863	0.857	0.832	0.844	0.837	0.804	
5.6	0.940	0.941	0.958	0.941	0.939	0.927	0.913	0.912	0.896	0.890	0.883	0.860	0.863	0.860	0.832	
6.0	0.958	0.961	0.974	0.961	0.960	0.949	0.938	0.934	0.918	0.914	0.908	0.886	0.890	0.881	0-857	
6.4	0.970	0.977	0.987	0.978	0.977	0.967	0.959	0.955	0.939	0.936	0.929	0.910	0.912	0.902	0.880	
6.8	0.983	0.988	0.995	0.988	0.992	0.981	0.976	0.972	0.957	0.954	0.947	0.934	0.934	0.921	0.900	
7.2	0-992	0-994	0.998	0.993	0.998	0.991	0.990	0.985	0.973	0.971	0.964	0.954	0.951	0.939	0.926	
7.6	0.997	0.997	1.000	0.995	1.000	0.997	0.996	0.994	0.982	0.982	0.978	0.971	0.967	0.956	0.949	
8.0	0.999	0.999		0.997		0.999	0.998	0.997	0.989	0.992	0.988	0.985	0.979	0.971	0.967	
8.5	1.000	1.000		0.999		1.000	0.999	0.998	0.994	0.998	0.995	0.994	0.990	0.984	0.983	
9.0				1.000			1.000	0.999	0.998	1.000	0.999	0.998	0.995	0.991	0.995	
9.5								1.000	1.000		1.000	1.000	0.997	0.996	0.998	
10.0													0.998	0.998	1.000	
10.5													1.000	1.000		
11.0																
TABLE 1 (Cont.)

······································										0.001			· · · · —			
X (mms)	0	12.7	25-4	38.1	50.8	63.5	76-2	6881 88-9	101.6	-0.001 114.3	127.0	139.7	152-4	165-1	177.8	
м.	2.51	2.50	2.55	2.48	2.46	2.44	2.41	2.39	2.38	2.35	2.32	2.27	2.28	2.27	2.19	
R.	19900	20000	18200	20800	21200	22300	23900	24600	26200	27100	28400	30900	30700	31800	35500	
T_w/T_1	2.153	2.164	2.216	2.165	2.165	2.099	2.079	2.051	2.046	2.037	2.020	1.941	1.974	1.974	1.910	
Y(mms)	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1								
0.1	1.970	2.008	1.968	1.983	1.977	1.914	1.910	1.878	1.883	1.869	1.852	1.800	1.820	1.814	1.789	
0.2	1.930	1.974	1.937	1.954	1.940	1.878	1.875	1.848	1.846	1.834	1.820	1.767	1.783	1.772	1.763	
0.3	1.890	1.925	1.899	1.919	1.907	1.838	1.842	1.811	1.810	1.798	1.790	1.742	1.752	1.742	1.737	
0.4	1.859	1.893	1.866	1.879	1.876	1.813	1.812	1.789	1.789	1.771	1.765	1.720	1.729	1.708	1.713	
0.5	1.830	1.858	1.836	1.847	1.848	1.790	1.791	1.768	1.766	1.748	1.744	1.702	1.712	1.684	1.695	
0.6	1.807	1.829	1.808	1.820	1.826	1.770	1.772	1.748	1.749	1.726	1.726	1.688	1.697	1.667	1.678	
0.8	1.768	1.779	1.762	1.778	1.783	1.737	1.735	1.714	1.710	1.688	1.698	1.664	1.667	1.641	1.646	
1.0	1.721	1.735	1.722	1.740	1.751	1.703	1.708	1.688	1.682	1.664	1.672	1.642	1.647	1.619	1.625	
1.2	1.691	1.703	1.684	1.709	1.718	1.676	1-681	1.663	1.660	1.640	1.649	1.622	1.625	1.605	1.603	
1.4	1.663	1.672	1.653	1.683	1.696	1.653	1.658	1.643	1.640	1.625	1.628	1.609	1.604	1.591	1.585	
1.6	1.633	1.649	1.630	1.651	1.668	1.629	1.638	1.621	1.617	1.606	1.608	1.590	1.588	1.574	1.572	
1.8	1.603	1.624	1.598	1.627	1.642	1.605	1.615	1.605	1.600	1.588	1.590	1.572	1.574	1.557	1.558	
2.0	1.576	1.592	1.571	1.606	1.615	1.580	1.594	1.581	1.585	1.574	1.573	1.553	1.557	1.543	1.542	
2.2	1.550	1.569	1.544	1.577	1.594	1.561	1.574	1.561	1.563	1.556	1.552	1.538	1.539	1.528	1.531	
2.4	1.525	1.539	1.519	1.551	1.565	1.537	1.551	1.539	1.544	1.536	1.534	1.521	1.525	1.515	1.519	
2.6	1.499	1.511	1.489	1.525	1.538	1.511	1.525	1.517	1.522	1.516	1.519	1.503	1.508	1.501	1.504	
2.8	1.473	1.486	1.461	1.499	1.509	1.488	1.505	1.498	1.480	1.498	1.503	1.490	1.490	1.486	1.489	
3.0	1.447	1.457	1.436	1.471	1.480	1.462	1.486	1.473	1.479	1.483	1.487	1.472	1.472	1.471	1.473	
3.3	1.412	1.418	1.400	1.436	1.448	1.425	1.452	1.441	1.453	1.454	1.460	1.448	1.445	1.446	1.450	
3.6	1.378	1.379	1.360	1.300	1.411	1.394	1.418	1.414	1.417	1.425	1.427	1.474	1.422	1.420	1.431	
3.0	1.344	1.345	1.322	1.366	1.374	1.359	1.384	1.379	1.387	1.396	1.400	1.395	1.389	1.398	1.410	
4.2	1.300	1.310	1.283	1.325	1.335	1.326	1.352	1.346	1.359	1.367	1.370	1.368	1.365	1.371	1.383	
4.5	1.275	1.273	1.205	1.289	1.297	1.288	1.321	1.312	1.329	1.336	1.340	1.342	1.335	1.348	1.361	
4.8	1.235	1.234	1.209	1.252	1.261	1.254	1.286	1.278	1.297	1.310	1.315	1.317	1.300	1.324	1.336	
5.2	1.197	1.192	1.163	1.201	1.215	1.214	1.200	1.234	1.255	1.267	1.273	1.281	1.274	1.293	1.307	
5.6	1.1/0	1.150	1.110	1.156	1.164	1.170	1.195	1.190	1.217	1.227	1.235	1.243	1.245	1.259	1.272	
6.0	1.100	1.106	1.078	1.111	1.118	1.178	1.151	1.151	1.179	1.187	1.196	1.206	1.206	1.230	1.240	
6.4	1.077	1.067	1.042	1.072	1.076	1.086	1.111	1.113	1.141	1.150	1.160	1.170	1.171	1.198	1.207	
6.8	1.045	1.038	1.021	1.042	1.042	1.058	1.074	1.076	1.106	1.113	1.125	1.133	1.138	1.166	1.176	
7.2	1.020	1.024	1.000	1.025	1.010	1.020	1.040	1.047	1.075	1.077	1.095	1.101	1.110	1.137	1.138	
7.6	1.006	1.012	1.004	1.012	1.007	1.012	1.018	1.024	1.049	1.052	1.066	1.067	1.083	1.110	1.102	
8.0	1.001	1.006	1.004	1.006	1.007	1.003	1.008	1.010	1.032	1.031	1.044	1.043	1.056	1.083	1.074	
8.5	1.000	1.002	1.000	1.002	1.007	1.000	1.002	1.002	1.018	1.015	1.074	1.018	1.033	1.057	1.045	
0.0	1.000	1.002		1.002	1,000	1.000	1.002	1.002	1.000	1.006	1.010	1.006	1.018	1.037	1.026	
0.5		1-000		1.000	1.000	1 000	1 000	1 000	1.004	1.007	1.003	1.001	1.008	1.024	1.012	
10.0									1.004	1.002	1.000	1.001	1.004	1.014	1.005	
10.5									1.000	1.000	1.000	1.000	1.007	1.005	1.002	
10.0									1.000				1.0002	1.002	1.002	
11.5													1.000	1.002	1.000	
11.2														1.000		

TABLE 1 (Cont.)

		• • • • • • • • • • • • • • • • • • • •			· · · · · ·			GRAT	DIENT B	-0.002						
X(mms)	0	12.7	25•4	38.1	50.8	63.5	76-2	88.9	101.6	114.3	127.0	139.7	152-4	165-1	177.8	
M_1	2.50	2.51	2.52	2.46	2.43	2.42	2.39	2.38	2.36	2.33	2.29	2.23	2.29	2.25	2.12	
$\theta(\text{mms})$	0.816	0.798	0.845	0-868	0.923	0.953	0.982	1.031	1.095	1.113	1.184	1.253	1.207	1.270	1-435	
δ (mms)	3.676	3-673	3.864	3.986	4.149	4.261	4.426	4.491	4.643	4.638	4.904	5.047	4.851	5.003	5.768	
Y(mms)	U/U_1	U/U_1	U/U_1	U/U_1	U/U_1	U/U_1	U/U_1	U/U_1	U/U_1	U/U_1	U/U_1	U/U_1	U/U_1	U/U_1	<i>U</i> / <i>U</i> ₁	
0.1	0.344	0.335	0.382	0.350	0.348	0.339	0.320	0.348	0.325	0.356	0.322	0.282	0.381	0.377	0-243 .	
0.2	0.362	0.353	0.394	0.372	0.364	0.360	0.347	0.365	0.359	0.374	0.353	0.315	0.400	0.388	0.269	
0.3	0.381	0.371	0.404	0.383	0.380	0.374	0.363	0.386	0.382	0.394	0.371	0.338	0.418	0.403	0.286	
0.4	0.401	0.388	0.416	0.404	0.394	0.386	0.378	0.398	0.401	0.407	0.384	0.350	0.434	0.412	0.294	
0.5	0.418	0.425	0.428	0.420	0.408	0.399	0.391	0.422	0.414	0.410	0.396	0.301	0.443	0.421	0.303	
0.0	0.450	0.455	0.440	0.431	0.420	0.414	0.404	0.422	0.445	0.446	0.400	0.3/1	0.451	0.449	0.315	
1.0	0.439	0.433	0.482	0.449	0.456	0.459	0.425	0.453	0.440	0.440	0.427	0.393	0.409	0.440	0.351	
1.2	0.507	0.506	0.501	0.488	0.473	0.477	0.461	0.455	0.478	0.400	0.457	0.425	0.400	0.475	0.368	
1.4	0.527	0.527	0.519	0.506	0.491	0.493	0.474	0.484	0.491	0.494	0.468	0.438	0.501	0.487	0.384	
1.6	0.548	0.546	0.539	0.522	0.507	0.508	0.491	0.502	0.503	0.507	0.481	0.454	0.511	0.497	0.398	
1.8	0.568	0.563	0.556	0.539	0.526	0.524	0.509	0.514	0.516	0.518	0.495	0.466	0.520	0.507	0.412	
2.0	0.587	0.579	0.573	0.555	0.541	0.538	0.524	0.525	0.528	0.531	0.508	0.480	0.531	0.521	0.422	
2.2	0.606	0.594	0.588	0.573	0.558	0.554	0.537	0.540	0.542	0.544	0.519	0.492	0.541	0.529	0.434	
2.4	0.623	0.612	0.603	0.591	0.573	0.567	0.551	0.556	0.557	0.556	0.531	0.507	0.552	0.538	0-444	
2.6	0.642	0.634	0.621	0.608	0.588	0.581	0.569	0.568	0.572	0.568	0.542	0.519	0.560	0.547	0.456	
2.8	0.659	0.652	0.638	0.626	0.605	0.598	0.584	0.583	0.584	0.580	0.554	0.529	0.573	0.556	0.470	
3.0	0.675	0.671	0.654	0.641	0.621	0.613	0.598	0.596	0.595	0.591	0.565	0.543	0.586	0.569	0.479	
3.3	0.699	0.695	0.679	0.664	0.645	0.637	0.618	0.616	0.612	0.609	0.584	0.560	0.600	0.588	0.499	
3.6	0.722	0.720	0.703	0.692	0.668	0.656	0.641	0.640	0.633	0.627	0.603	0.582	0.613	0.605	0.519	
3.9	0.746	0.747	0.726	0.715	0.693	0.681	0.664	0.662	0.652	0.644	0.621	0.603	0.633	0.621	0.534	
4.2	0.702	0.705	0.750	0.741	0.717	0.704	0.687	0.683	0.675	0.663	0.643	0.622	0.651	0.638	0.553	
4.3	0.916	0.010	0.709	0.700	0.740	0.751	0.722	0.705	0.090	0.706	0.603	0.662	0.692	0.676	0-502	
5.2	0.848	0.846	0.838	0.210	0.703	0.783	0.764	0.757	0.746	0.700	0.004	0.600	0.715	0.600	0.620	
5.6	0.877	0.876	0.856	0.840	0.825	0.814	0.704	0.783	0.773	0.757	0.736	0.715	0.741	0.723	0.647	
6.0	0.902	0.909	0.885	0.877	0.855	0.842	0.823	0.812	0.800	0.791	0.764	0.742	0.764	0.748	0.675	
6.4	0.926	0.935	0.912	0.904	0.884	0.871	0.849	0.838	0.827	0.819	0.790	0.770	0.788	0.773	0.700	
6.8	0.948	0.957	0.936	0.928	0.912	0.895	0.878	0.864	0.852	0.846	0.816	0.795	0.813	0.799	0.726	
7.2	0.969	0.974	0.955	0.948	0.934	0.919	0.906	0.893	0.876	0.872	0.842	0.823	0.839	0.824	0.755	
7.6	0.984	0.987	0.973	0.967	0.955	0.944	0.930	0.916	0.897	0.897	0.867	0.848	0.863	0.846	0.784	
8.0	0.991	0.994	0.986	0.982	0.972	0.965	0.952	0.939	0.920	0.921	0.891	0.872	0.884	0.869	0.812	
8.5	0-995	1.000	0.994	0.992	0.987	0.983	0.976	0.964	0.945	0.947	0.920	0.903	0.914	0.898	0.844	
9.0	0.999		0.999	0.997	0.994	0.993	0.992	0.981	0.966	0.966	0.946	0.928	0.939	0.925	0.875	
9.5	1.000		1.000	0.999	0.997	0.997	0.999	0.993	0.980	0.979	0.967	0.951	0.959	0.948	0.906	
10.0				1.000	1.000	0.999	1.000	0.998	0.988	0.989	0.982	0.973	0.978	0.969	0.931	
10.5						1.000		0.999	0.992	0.995	0.992	0.989	0.991	0.982	0.951	
11.0								1.000	0.996	0.997	0.996	0.997	0.998	0.991	0.969	
11.0									0.997	0.998	0.999	1.000	1.000	0.996	0.097	
12.0									1.000	1.000	1.000			1.000	0.002	
12.0									1.000	1.000				1.000	0.006	
13.5															0.000	
14.0															1,000	
17.0															1 000	

TABLE 1 (Cont.)

X(mms)	0	12.7	25.4	38.1	50.8	63.5	76.2	GRAI 88·9	DIENT B 101.6	-0.002 114.3	127.0	139.7	152.4	165-1	177.8		
$\overline{M_1}$	2.50	2.51	2.52	2.46	2.43	2.42	2.39	2.38	2.36	2.33	2.29	2.23	2.29	2.25	2.12	 	
$\frac{R_6}{T_w}/T_1$	24300 2·170	23800 2·186	$25200 \\ 2 \cdot 204$	27300 2·174	29200 2·130	$29800 \\ 2.108$	31500 2·095	33400 2·089	$35300 \\ 2.051$	36200 2·022	$39900 \\ 1.999$	42600 1·919	$40200 \\ 1.984$	$43100 \\ 1.938$	52100 1·838		
Y(mms)	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	 	
0.1	2.027	2.049	2.027	2.042	1.993	1.979	1.979	1.953	1.936	1.889	1.887	1.841	1.844	1.804	1.780		
0.2	2.003	2.021	2.005	2.023	1.9/1	1.954	1.952	1-931	1.903	1.869	1.860	1.814	1.821	1.767	1.703		
0.3	1.974	1.996	1.983	2.014	1.020	1.934	1.930	1.004	1.054	1.845	1.022	1.776	1.777	1.752	1.725		
0.4	1.027	1.9/1	1.962	1.094	1.012	1.910	1.914	1.868	1.830	1.813	1.800	1.764	1.766	1.738	1.727		
0.5	1.006	1.024	1.022	1.964	1.912	1.878	1.878	1.851	1.874	1.801	1.796	1.752	1.754	1.725	1.717		
0.0	1.900	1.924	1.925	1.955	1.868	1.8//	1.840	1.823	1.794	1.772	1.771	1.728	1.727	1.703	1.695		
1.0	1.837	1-848	1.860	1.840	1.838	1.810	1.826	1.801	1.773	1.750	1.751	1.709	1.711	1.685	1.681		
1.2	1.807	1.818	1.835	1.823	1.815	1.799	1.803	1.787	1.753	1.731	1.730	1.695	1.694	1.671	1.668		
1.4	1.783	1.792	1.812	1.804	1.793	1.777	1.787	1.767	1.736	1.713	1.718	1.682	1.683	1.662	1.657		
1.6	1.755	1.770	1.787	1.782	1.771	1.759	1.769	1.745	1.725	1.699	1.703	1.670	1.672	1.649	1.648		
1.8	1.730	1.749	1.764	1.764	1.750	1.743	1.746	1.729	1.713	1.689	1.687	1.658	1.662	1.641	1.637		
2.0	1.706	1.725	1.744	1.744	1.731	1.728	1.730	1.717	1.699	1.674	1.673	1.646	1.651	1.625	1.629		
2.2	1.682	1.706	1.723	1.721	1.713	1.710	1.711	1.702	1.683	1.660	1.661	1.633	1.638	1.617	1.622		
2.4	1.659	1.683	1.700	1.699	1.696	1.692	1.697	1.683	1.663	1.647	1.649	1.619	1.627	1.607	1.613		
2.6	1.634	1.654	1.677	1.678	1.674	1.676	1.677	1.668	1.646	1.632	1.638	1.609	1.619	1.596	1.603		
2.8	1.611	1.628	1.654	1.656	1.653	1.655	1.660	1.652	1.633	1.618	1.624	1.599	1.603	1.588	1.593		
3.0	1.588	1.602	1.632	1.636	1.633	1.638	1.644	1.637	1.619	1.605	1.611	1.583	1.589	1.575	1.583		
3.3	1.553	1.566	1.595	1.605	1.603	1.604	1.620	1.610	1.596	1.583	1.589	1.46/	1.574	1.557	1.552		
3.6	1.517	1.528	1.560	1.565	1.572	1.578	1.592	1.580	1.572	1.540	1.509	1.525	1.539	1.530	1.533		
3.9	1.482	1.486	1.528	1.331	1.538	1.549	1.503	1.534	1.510	1.517	1.524	1.503	1.512	1.500	1.520		
4.2	1.440	1.451	1.490	1.493	1.440	1.491	1.502	1.406	1.401	1.402	1.501	1.479	1.488	1.478	1.505		
4.9	1.272	1.272	1.412	1.404	1.430	1.450	1.460	1.490	1.491	1.492	1.476	1.457	1.468	1.456	1.485	· · · ·	
4.0	1.210	1.326	1.365	1.377	1.301	1.402	1.403	1.427	1.427	1.438	1.443	1.425	1.434	1.432	1.460		
5.6	1.260	1.270	1.313	1.325	1.345	1.357	1.383	1.389	1.391	1.399	1.409	1.309	1.400	1.403	1.434		
6.0	1.209	1.213	1.262	1.275	1.298	1.311	1.338	1.348	1.354	1.355	1.374	1.366	1.371	1.371	1.406		
6.4	1.175	1.160	1.212	1.225	1.251	1.266	1.299	1.307	1.315	1.314	1.339	1.333	1.339	1.340	1.379		
6.8	1.130	1.115	1.160	1.180	1.202	1.229	1.256	1.268	1.280	1-276	1.302	1.303	1.305	1.308	1.351		
7.2	1.083	1.076	1.116	1.136	1.157	1.187	1.208	1.223	1.241	1.239	1.268	1.269	1.270	1.277	1.321		
7.6	1.042	1.040	1.068	1.096	1.116	1.141	1.166	1.182	1.209	1.199	1.232	1.236	1.237	1.248	1.290		
8.0	1.021	1.020	1.033	1.061	1.080	1.101	1.126	1.142	1.169	1.163	1.197	1.203	1.206	1.218	1.259		
8.5	1.005	1.008	1.012	1.030	1.042	1.057	1.077	1.092	1.125	1.119	1.155	1.164	1.163	1.177	1.222		
9.0	1.002	1.004	1.001	1.009	1.022	1.029	1.037	1.052	1.086	1.082	1.112	1.128	1.124	1.142	1.185		
9.5	1.000	1.000	1.000	1.001	1.009	1.013	1.017	1.024	1.053	1.051	1.076	1.091	1.090	1.108	1.147		
10.0				1.000	1.001	1.006	1.010	1.009	1.031	1.031	1.048	1.056	1.056	1.073	1.112		
10.5					1.000	1.002	1.002	1.004	1.018	1.015	1.025	1.026	1.032	1.020	1.083		
11.0						1.000	1.000	1.000	1.005	1.007	1.005	1.002	1.006	1.015	1.027		
11.5							1.000		1.002	1.001	1.001	1.000	1.002	1.009	1.022		
12.0									1.000	1.001	1,000	1.000	1.005	1.000	1.013		
12.5									1.000	1.000	1.000		1,000	1.007	1.005		
13.5													1 000	1.002	1.002		
14.0														1 000	1.000		
14.0															1 000		

								GRAD	IENT B	-0.003						
X(mms)	0	12.7	25.4	38.1	50.8	63.5	76-2	88.9	101.6	114.3	127.0	139.7	152.4	165.1	177.8	
<u></u>	2.51	2.50	2.50	2.45	2.44	2.40	2.37	2.36	2.34	2.29	2.27	2.21	2.24	2.11	2.07	
$\theta(\text{mms})$	0.957	0.992	1.026	1.084	1.162	1.184	1.250	1.306	1.378	1.478	1.536	1.604	1.680	1.756	1.877	
δ (mms)	4.574	4.854	4.937	5.331	5.689	5.925	6.040	6.120	6.423	6.727	7.065	7.397	7.292	8.303	8.546	
Y(mms)	U/U_1	U/U_1	U/U_1	U/U_1	U/U_1	U/U_1	U/U_1	U/U_1	<i>U</i> / <i>U</i> ₁	<i>U</i> / <i>U</i> ₁	U/U_1	<i>U</i> / <i>U</i> ₁	U/U_1	U/U_1	U/U_1	
0.1	0.332	0.330	0.345	0.308	0.296	0.258	0.251	0.284	0.286	0.257	0.261	0.217	0.309	0.133	0.112	
0.2	0.340	0.334	0.352	0.315	0.304	0.267	0.262	0.294	0.296	0.264	0.269	0.227	0.314	0.143	0-127	
0.3	0.350	0.341	0.358	0.322	0.311	0.275	0.273	0.305	0.303	0.267	0.276	0.236	0.320	0.154	0.134	
0.4	0.359	0.347	0.364	0.329	0.319	0.284	0.283	0.313	0.310	0.274	0.284	0.242	0.328	0.163	0.146	
0.2	0.368	0.353	0.369	0.335	0.330	0.292	0.292	0.319	0.316	0.281	0.290	0.247	0.333	0.172	0.161	
0.6	0.376	0.359	0.379	0.342	0.335	0.300	0.301	0.326	0.325	0.289	0.296	0.253	0.338	0.180	0.173	
0.8	0.392	0.376	0.389	0.353	0.347	0.314	0.320	0.344	0.341	0.308	0.309	0.266	0.344	0.194	0.183	
1.0	0.411	0.395	0.401	0.365	0.360	0.327	0.337	0.358	0.352	0.320	0.318	0.279	0.349	0.208	0.192	
1.2	0.429	0.409	0.417	0.374	0.367	0.343	0.345	0.300	0.362	0.332	0.325	0.202	0.338	0.219	0.201	
1.4	0.446	0.422	0.430	0.387	0.379	0.300	0.330	0.294	0.391	0.343	0.335	0.303	0.370	0.243	0.210	
1.0	0.402	0.454	0.442	0.419	0.400	0.201	0.292	0.200	0.301	0.363	0.355	0.316	0.376	0.253	0.227	
2.0	0.407	0.471	0.437	0.430	0.409	0.405	0.302	0.413	0.391	0.375	0.366	0.324	0.383	0.263	0.242	
2.0	0.512	0.488	0.471	0.444	0.435	0.419	0.413	0.423	0.403 0.417	0.386	0.375	0.333	0.390	0.203 0.273	0.253	
2.4	0.512 0.528	0.503	0.503	0.459	0.447	0.431	0.419 0.426	0.432	0.428	0.395	0.384	0.344	0.398	0.282	0.263	
2.6	0.544	0.522	0.520	0.473	0.457	0.445	0.437	0.444	0.440	0.403	0.389	0.358	0.405	0.291	0.273	
2.8	0.560	0.536	0.534	0.488	0.471	0.460	0.448	0.453	0.451	0.414	0.398	0.372	0.414	0.298	0.286	
3.0	0.576	0.551	0.550	0.505	0.488	0.474	0.462	0.467	0.460	0.427	0.409	0.381	0.425	0.308	0.298	
3-3	0.605	0.571	0.574	0.531	0.509	0.494	0.480	0-486	0.476	0.445	0.425	0.397	0.438	0.321	0.316	
3.6	0.631	0.593	0.597	0.552	0.530	0.516	0.499	0.502	0.494	0.461	0.441	0.413	0.449	0.337	0.333	
3.9	0.658	0.620	0.619	0.576	0.553	0.534	0.520	0.525	0.513	0.476	0.459	0.425	0.462	0.355	0.349	
4.2	0.681	0.646	0.643	0.602	0.574	0.555	0.541	0.545	0.531	0.495	0.477	0.443	0.476	0.373	0.369	
4.5	0.709	0.669	0.663	0.622	0.598	0.577	0.567	0.564	0.550	0.515	0.495	0.464	0.495	0.391	0.402	
4.8	0.732	0.693	0.687	0.642	0.619	0.602	0.581	0.611	0.502	0.555	0.515	0.510	0.521	0.431	0.432	
5.2	0.704	0.757	0.752	0.712	0.600	0.662	0.642	0.629	0.610	0.585	0.560	0.534	0.552	0.456	0.460	
5.0	0.873	0.700	0.784	0.744	0.713	0.003	0.672	0.668	0.644	0.000	0.588	0.558	0.578	0.482	0.486	
6.4	0.850	0.821	0.813	0.775	0.743	0.732	0.700	0.694	0.672	0.634	0.611	0.582	0.602	0.507	0.512	
6.8	0.879	0.852	0.843	0.804	0.772	0.754	0.728	0.725	0.699	0.662	0.636	0.607	0.624	0.537	0.536	
7.2	0.906	0.883	0.872	0.836	0.802	0.783	0.759	0.752	0.727	0.695	0.664	0.630	0.648	0.561	0.562	
7.6	0.932	0.909	0.900	0.867	0.831	0.812	0.788	0.779	0.755	0.719	0.691	0.656	0.674	0.587	0.587	
8.0	0.948	0.935	0.925	0.894	0.859	0.842	0.815	0.804	0.781	0.745	0.717	0.682	0.699	0.613	0.613	
8.5	0.969	0.963	0.951	0.927	0.893	0.876	0.852	0.849	0.810	0.784	0.751	0.722	0.729	0.647	0.645	
9.0	0.987	0.987	0.974	0.955	0.923	0.907	0.889	0.874	0.844	0.815	0.784	0.757	0.763	0.682	0.677	
9.5	0.995	0.996	0.989	0.976	0.951	0.938	0.921	0.903	0.875	0.848	0.818	0.791	0.794	0.715	0.726	
10.0	0.998	0.999	0.996	0.993	0.972	0.963	0.951	0.929	0.904	0.879	0.849	0.824	0.825	0.779	0.764	
10.5	1.000	1.000	0.998	0.998	0.985	0.980	0.972	0.954	0.934	0.907	0.007	0.820	0.891	0.200	0.702	
11.0			1.000	1.000	0.006	0.990	0.998	0.0974	0.937	0.955	0.035	0.01/	0.001	0.841	0.820	
12.0			1.000		0.008	0.008	0.000	0.005	0.975	0.976	0.955	0.939	0.927	0.869	0.849	
12.5					0.000	0.000	1.000	0.999	0.995	0.988	0.973	0.959	0.945	0.896	0.876	
13.0					1.000	1.000	1 000	1.000	0.999	0.994	0.986	0.974	0.961	0.923	0.902	
13.5					- 000				1.000	0.998	0.994	0.986	0.974	0.951	0.924	
14.0										0.999	0.997	0.991	0.982	0.973	0.939	
15.0										1.000	1.000	0.999	0.993	0.993	0.965	
16.0												1.000	0.997	1.000	0.981	
17.0													1.000		0.992	
18.0															0.997	
19.0															1.000	
20.0															1.000	

TABLE 1 (Cont.)

								GRAI	DIENT B	G-0.003						
X(mms)	0	12.7	25.4	38.1	50.8	63.5	76-2	88.9	101.6	114.3	127.0	139.7	152.4	165.1	177.8	
M_1	2.51	2.50	2.50	2.45	2.44	2.40	2.37	2.36	2.34	2.29	2.27	2.21	2.24	2.11	2.07	
R_{ϵ}	28100	29500	30700	33600	36300	38200	40000	41800	44800	48500	51900	55400	56800	63100	69000	
T_w/T_1	2.186	2.192	2.192	2.152	2.147	2.133	2.065	2.063	2.048	1.994	1.978	1.921	1.934	1.830	1.796	
Y(mms)	T/T_1	$T/T_{\rm i}$	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1								
$0 \cdot 1$	2.057	2.062	2.054	2.043	2.047	2.058	1.996	1.973	1.962	1.928	1.911	1.871	1.844	1.754	1.781	
0.2	2.039	2.050	2.038	2.029	2.032	2.047	1.982	1.959	1.948	1.919	1.897	1.861	1.831	1.750	1.772	
0.3	2.019	2.038	2.025	2.014	2.019	2.034	1.969	1.945	1.937	1.907	1.886	1.848	1.819	1.748	1.762	
0.4	2.000	2.026	2.010	2.002	2.007	2.023	1.958	1.934	1.926	1.897	1.875	1.838	1.808	1.746	1.754	
0.5	1.076	2.001	1.095	1.097	1.093	2.001	1.021	1.925	1.916	1.887	1.867	1.830	1.702	1.720	1.727	
0.0	1.052	2.001	1.980	1.982	1.982	2.003	1.010	1.917	1.905	1.857	1.844	1.810	1.793	1.722	1.724	
1.0	1.932	1.950	1.945	1.043	1.902	1.965	1.801	1.870	1.870	1.840	1.828	1.707	1.773	1.726	1.712	
1.2	1.906	1.930	1.978	1.070	1.033	1.905	1.880	1.866	1.857	1,870	1.820	1.784	1.763	1.722	1.705	
1.4	1.888	1.914	1.912	1.915	1.919	1.927	1.868	1.852	1.845	1.817	1.811	1.776	1.755	1.715	1.699	
1.6	1.871	1.895	1.898	1.898	1.903	1.910	1.858	1.843	1.836	1.806	1.801	1.773	1.749	1.710	1.694	
1.8	1.849	1.879	1.880	1.883	1.888	1.895	1.846	1.828	1.826	1.797	1.793	1.767	1.745	1.706	1.690	
2.0	1.828	1.861	1.862	1.870	1.874	1.881	1.832	1.816	1.815	1.789	1.786	1.762	1.738	1.703	1.685	
2.2	1.811	1.840	1.843	1.857	1-862	1.869	1.818	1.806	1.803	1.781	1.777	1.756	1.732	1.698	1.680	
2.4	1.790	1.820	1.822	1.840	1.849	1.857	1.807	1.797	1.790	1.722	1.770	1.747	1.727	1.691	1.675	
2.6	1.770	1.800	1.804	1.822	1.836	1.841	1.794	1.786	1.780	1.765	1.765	1.738	1.720	1.687	1.669	
2.8	1.752	1.784	1.784	1.807	1-821	1.825	1.785	1.775	1.768	1.758	1.757	1.727	1.712	1.684	1.663	
3.0	1.732	1.763	1.766	1.787	1.804	1.812	1.770	1.763	1.759	1.745	1.748	1.721	1.704	1.677	1.656	
3.3	1.695	1.737	1.732	1.755	1.779	1.789	1.752	1.745	1.743	1.730	1.732	1.707	1.691	1.699	1.646	
3.6	1.661	1.709	1.702	1.731	1.753	1.764	1.733	1.726	1.725	1.713	1.718	1.695	1.682	1.661	1.637	
3.9	1.618	1.671	1.670	1.702	1.727	1.744	1.711	1.701	1.702	1.699	1.701	1.685	1.671	1.650	1.629	
4.2	1.584	1.635	1.638	1.672	1.703	1.717	1.686	1.680	1.685	1.680	1.685	1.671	1.657	1.638	1.616	
4.5	1.547	1.604	1.610	1.642	1.672	1.694	1.657	1.655	1.663	1.659	1.669	1.655	1.639	1.628	1.604	
4.8	1.512	1.567	1.574	1.616	1.643	1.661	1.641	1.631	1.643	1.640	1.651	1.636	1.625	1.618	1.593	
5.4	1.405	1.471	1.525	1.520	1.604	1.570	1.565	1.602	1.610	1.619	1.627	1.612	1.502	1.601	1.574	
5.0	1.271	1.471	1.475	1.476	1.517	1.520	1.521	1.522	1.550	1.28/	1.572	1.569	1.583	1.583	1.530	
6.4	1.377	1.371	1.377	1.478	1.473	1.486	1.406	1.408	1.516	1.530	1.550	1.541	1.535	1.545	1.515	
6.8	1.273	1.316	1.328	1.384	1.478	1.453	1.456	1.456	1.483	1.400	1.510	1.515	1.507	1.521	1.407	
7.2	1.220	1.262	1.277	1.335	1.384	1.409	1.414	1.410	1.440	1.459	1.486	1.491	1.481	1.501	1.476	
7.6	1.171	1.213	1.230	1.281	1.336	1.366	1.374	1.382	1.410	1.428	1.453	1.463	1.451	1.477	1.455	
8.0	1.131	1.162	1.182	1.234	1.291	1.322	1.336	1.344	1.373	1.393	1.422	1.431	1.422	1.455	1.430	· · · ···
8.5	1.079	1.100	1.128	1.176	1.234	1.265	1.281	1.279	1.332	1.344	1.382	1.389	1.389	1.428	1.401	
9.0	1.036	1.047	1.077	1.119	1.178	1.214	1.224	1.241	1.284	1.299	1.338	1.348	1.348	1.397	1.371	
9.5	1.011	1.019	1.041	1.075	1.125	1.159	1.174	1.196	1.237	1.255	1.293	1.306	1.308	1.367	1.339	
10.0	1.002	1.008	1.017	1.034	1.076	1.108	1.122	1.154	1.193	1.210	1.248	1.264	1.272	1.335	1.312	
10.5	1.001	1.002	1.005	1.017	1.046	1.067	1.077	1.109	1.143	1.169	1.205	1.227	1.236	1.303	1.286	
11.0	1.000	1.000	1.002	1.007	1.022	1.037	1.044	1.071	1.105	1.129	1.164	1.189	1.200	1.269	1.256	
11.5			1.000	1.002	1.009	1.023	1.024	1.041	1.072	1-087	1.124	1.150	1.164	1.232	1.227	
12.0				1.000	1.003	1.012	1.013	1.023	1.047	1.057	1.090	1.112	1.134	1.199	1.196	
12.5					1.001	1.006	1.006	1.013	1.029	1.036	1.062	1.084	$1 \cdot 104$	1.164	1.165	
13.0					1.000	1.003	1.003	1.004	1.014	1.020	1-039	1.060	1.078	1.127	1.139	
13.5						1.000	1.000	1.002	1.010	1.009	1.022	1.038	1.059	1.082	1.110	
14.0								1.000	1.005	1.003	1.013	1.033	1.040	1.050	1.090	
15.0									1.000	1.000	1.004	1.009	1.005	1.018	1.056	
10.0											1.002	1.002	1.005	1.003	1.031	
12.0											1.000	1.000	1.000	1.000	1.002	
10.0															1.000	
20.0															1.000	

TABLE 1 (Cont.)

$ \begin{array}{c c c c c c c c c c c c c c c c c c c $			<u> </u>		., s, s				GRAD	IENT C	-0.000			,					
	X(mms)	0	12.7	25.4	38.1	50.8	63.5	76-2	88.9	101.6	114.3	127.0	139•7	152.4	165.1	177.8	190-5	203.2	215.9
efferms 0.404 0.404 0.442 0.444 0.442 0.444 <	M_1	2.57	2.61	2.58	2.61	2.61	2.67	2.72	2.77	2.84	2.90	2.96	3.01	3.05	3.10	3.13	3.17	3.22	3·24
Ymmel U/U, U/U, <t< td=""><td>θ (mms) δ (mms)</td><td>0:404 1:727</td><td>0·398 1·710</td><td>$0.439 \\ 1.869$</td><td>$0.414 \\ 1.812$</td><td>0·484 2·046</td><td>$0.442 \\ 1.985$</td><td>$0.446 \\ 2.062$</td><td>0·486 2·214</td><td>0·487 2·298</td><td>0·504 2·418</td><td>2.530</td><td>0·532 2·640</td><td>0.538 2.779</td><td>2.963</td><td>3·174</td><td>3·114</td><td>3.200</td><td>3.432</td></t<>	θ (mms) δ (mms)	0:404 1:727	0·398 1·710	$0.439 \\ 1.869$	$0.414 \\ 1.812$	0·484 2·046	$0.442 \\ 1.985$	$0.446 \\ 2.062$	0·486 2·214	0·487 2·298	0·504 2·418	2.530	0·532 2·640	0.538 2.779	2.963	3·174	3·114	3.200	3.432
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	Y(mms)	<i>U</i> / <i>U</i> ₁	U/U_1	U/U_1	U/U_1	U/U_1	U/U_1	U/U_1	U/U_1	<i>U</i> / <i>U</i> ₁	U/U_1	<i>U</i> / <i>U</i> ₁	U/U_1	U/U_1	U/U_1	U/U_1	U/U_1	U/U_1	U/U_1
0:20 0:600 0:613 0:610 0:643 0:643 0:643 0:643 0:643 0:643 0:644 0:643	0.1	0.539	0.576	0.543	0.548	0.549	0.568	0.590	0.579	0.598	0.571	0.587	0.584	0.592	0.579	0.568	0.581	0.573	0.586
0-3 0-43 0-430 0-430 0-430 0-437 0-727 0-721 0-721 0-721 0-721 0-721 0-720 0-740 0-740 0-740 0-740 0-740 0-740 0-740 0-720 0-720 0-740 0-740 0-740 0-720 0-740 0-740 0-740 0-740 0-740 0-740 0-740 0-740 0-740 0-740 0-740 0-740 0-740 0-740 0-740 0-730 0-740 0-730 0-740 0-730 0-740 0-720 0-740 0-720 0-740 0-720 0-740 0-720 0-740 0-720 0-740 0-720 0-740 0-720 0-740 0-720 0-740 0-720 0-740 0-720 0-730 0-740 0-720 0-730 0-740 0-720 0-730 0-740 0-720 0-730 0-740 0-720 0-730 0-740 0-720 0-730 0-740 0-722 0-730 0-740 0-722 0-730 0-	0.2	0.600	0.625	0.610	0.660	0.610	0.643	0.601	0.681	0.649	0.624	0.693	0.680	0.648	0.630	0.07	0.024	0.018 0.657	0.013 0.642
0.653 0.705 0.705 0.705 0.705 0.705 0.716 0.720 0.744 0.744 0.747 0.741 0.742 0.729 0.729 0.720 0.714 0.767 0.66 0.790 0.723 0.717 0.725 0.756 0.757 0.757 0.778 0.730 0.739 0.739 0.739 0.739 0.739 0.730 0.735 0.755 0.755 0.755 0.756 0.757 0.757 0.758 0.788 0.797 0.798 0.799 0.730 0.730 0.730 0.730 0.730 0.730 0.730 0.730 0.730 0.739 0.739 0.739 0.739 0.739 0.730 0.730 0.730 0.730 0.730 0.730 0.730 0.730 0.730 0.730 0.730 0.730 0.730 0.730 0.730 0.730 0.730 0.730 0.731 0.730 0.731 0.730 0.731 0.730 0.730 0.731 0.730 0.73	0.3	0.643	0.038	0.620	0.687	0.049	0.698	0.091 0.727	0.031 0.714	0.030	0.034 0.721	0.729	0.009	0.0719	0.707	0.698	0.698	0.690	0.670
0-6 0.733 0.717 0.723 0.716 0.736 0.755 0.748 0.737 0.757 0	0.5	0.693	0.705	0.702	0.708	0.700	0.720	0.744	0.734	0.744	0.743	0.747	0.741	0.742	0.729	0.722	0.720	0.714	0.697
0-88 0.734 0.750 0.741 0.757 0.777 0.778 <th0< td=""><td>0.6</td><td>0.709</td><td>0.723</td><td>0.717</td><td>0.725</td><td>0.716</td><td>0.736</td><td>0.755</td><td>0.748</td><td>0.759</td><td>0.763</td><td>0.762</td><td>0.757</td><td>0.757</td><td>0.748</td><td>0.739</td><td>0.739</td><td>0.731</td><td>0.717</td></th0<>	0.6	0.709	0.723	0.717	0.725	0.716	0.736	0.755	0.748	0.759	0.763	0.762	0.757	0.757	0.748	0.739	0.739	0.731	0.717
1-0 0-755 0-765 0-756 0-750 0-756 0-776 0-780 0-778 0-788 0-792 0-791 0-786 0-792 0-778 0-720 0-789 0-775 0-797 0-788 0-792 0-778 0-720 0-780 0-775 0-797 0-786 0-797 0-786 0-780 0-780 0-780 0-780 0-780 0-780 0-780 0-780 0-780 0-780 0-780 0-775 0-797 0-786 0-803 0	0.8	0.734	0.750	0.741	0.748	0.735	0.757	0.774	0.765	0.777	0.779	0.782	0.778	0.779	0.770	0.765	0.761	0.755	0.742
1:2 0.7/0 0.780 0.772 0.782 0.791 0.772 0.793 0.794 0.793 0.733 0.733 0.733 0	1.0	0.755	0.765	0.755	0.763	0.750	0.775	0.784	0.778	0.788	0.788	0.792	0.791	0.207	0.784	0.782	0.702	0.780	0.773
114 07.08 07.97 07.97 07.00 0.010 0.000 0.011 0.011 0	1.2	0.770	0.707	0.722	0.701	0.776	0.201	0.206	0.801	0.808	0.808	0.803	0.803	0.818	0.793	0.794	0.792	0.803	0.786
18 0.807 0.822 0.811 0.819 0.820 0.821 0.827 0.820 0.827 0.820 0.827 0.820 0.821 0.825 0.823 0.823 0.837 0.830 0.843 0.839 0.843 0.839 0.843 0.839 0.843 0.839 0.843 0.839 0.843 0.839 0.844 0.843 0.843 0.843 0.843 0.843 0.843 0.843 0.843 0.844 0.841 0.833 0.834 0.844 0.842 0.843 0.843 0.843 0.843 0.843 0.843 0.843 0.843 0.844 0.841 0.843 0.843 0.843 0.843 0.843 0.843 0.843 0.	1.4	0.803	0.812	0.796	0.805	0.787	0.801	0.816	0.801 0.812	0.808	0.818	0.812 0.822	0.814	0.826	0.818	0.818	0.814	0.814	0.798
220 0.831 0.832 0.833 0.835 0.837 0.830 0.836 0.838 0.839 0.843 0.839 0.833 0.834 0.844 2.2 0.844 0.852 0.836 0.845 0.845 0.844 0.844 0.844 0.843 0.843 0.844 0.846 0.867 0.861 0.877 0.880 0.883 0.887 0.884 0.884 0.884 0.884 0.884	1.8	0.817	0.812	0.811	0.819	0.800	0.824	0.828	0.821	0.827	0.827	0.830	0.832	0.835	0.828	0.829	0.825	0.823	0.807
2:2 0.844 0.852 0.836 0.845 0.846 0.844 0.843 0.847 0.848 0.850 0.846 0.844 0.841 0.843 0.850 0.850 0.850 0.850 0.851 0.841 0	$\hat{2}\cdot\hat{0}$	0.831	0.840	0.822	0.833	0.813	0.835	0.837	0.830	0.836	0.835	0.838	0.839	0.843	0.839	0.837	0.833	0.834	0.816
2:4 0.859 0.863 0.847 0.857 0.857 0.853 0.855 0.864 0.864 0.864 0.864 0.864 0.864 0.864 0.864 0.864 0.864 0.864 0.864 0.864 0.864 0.865 0.864 0.867 0	2.2	0.844	0.852	0.836	0.845	0.824	0.846	0.847	0.839	0.844	0.843	0.847	0.848	0.850	0.846	0.844	0.841	0.843	0.824
2:6 0.873 0.877 0.859 0.850 0.864 0.850 0.860 0.861 0.864 0.864 0.861 0.864 0.864 0.867 0.867 0.865 0.864 0.867 0.867 0.865 0.864 0.867 0.867 0.867 0.867 0.867 0.867 0.867 0.867 0.867 0.867 0.867 0.867 0.867 0.867 0.867 0.867 0.867 0.867 0.877 0.873 0.872 0.870 0.868 0.881 0.878 0.885 0.887 0.885 0.885 0.884 0.881 0.878 0.885 0.881 0.878 0.885 0.884 0.881 0.878 0.885 0.885 0.884 0.883 0.889 0.885 0.885 0.885 0.884 0.883 0.885 0.886 0.885 0.886 0	2.4	0.859	0.863	0.847	0.857	0.834	0.857	0.856	0.848	0.852	0.852	0.855	0.855	0.858	0.853	0.851	0.849	0.851	0.831
2-8 0-886 0-885 0-875 0-875 0-875 0-807 0-907 0-903 0	2.6	0.873	0.877	0.859	0.870	0.845	0.865	0.864	0.858	0.859	0.860	0.861	0.860	0.870	0.867	0.865	0.864	0.829	0.846
533 0.936 0.937 0.947 0.844 0.909 0.887 0.893 0.892 0.889 0.893 0.892 0.893 0.892 0.893 0.893 0	2.8	0.800	0.001	0.894	0.804	0.855	0.885	0.884	0.800	0.875	0.873	0.876	0.876	0.877	0.873	0.872	0.870	0.869	0.853
3.6 0.935 0.934 0.917 0.926 0.933 0.909 0.889 0.887 0.892 0.893 0.889 0.885 0.890 0.882 0.971 0.913 0.910 0.910 0.900 0.900 0.900 0.900 0.900 0.905 0.907 0.888 0.893 0.892 0.822 0.917 0.915 0.901 0.915 0.912 0.913 0.924 0.924 0.924 0.924 0.924 0.924 0.924 0.924 0.924 0.924 0	3.3	0.016	0.901	0.004	0.910	0.884	0.900	0.896	0.887	0.887	0.885	0.885	0.884	0.884	0.881	0.881	0.878	0.877	0.861
5-9 0.951 0.948 0.940 0.913 0.921 0.901 0.901 0.902 0.900 0.896 0.895 0.893 0.892 0.874 4-2 0.964 0.961 0.948 0.933 0.920 0.917 0.913 0.910 0.910 0.910 0.910 0.910 0.900 0.900 0.900 0.895 0.893 0.892 0.874 4-5 0.977 0.974 0.960 0.964 0.943 0.930 0.922 0.917 0.915 0.900 0.900 0.899 0.899 0.899 0.882 5.2 0.994 0.992 0.990 0.968 0.971 0.955 0.944 0.932 0.921 0.912 0.919 0.902 0.922 0.922 0.924 0.924 0.921 0.913 0.933 0.931 0.924 0.924 0.923 0.927 0.909 0.933 0.916 0.947 0.944 0.940 0.932 0.923 0.927 0.904	3.6	0.935	0.934	0.917	0.926	0.899	0.913	0.909	0.898	0.897	0.895	0.894	0.893	0.892	0.889	0.889	0.885	0.885	0.867
4:2 0.964 0.961 0.948 0.9917 0.913 0.911 0.910 0.908 0.902 0.903 0.889 0.882 4:5 0.977 0.974 0.960 0.964 0.943 0.943 0.930 0.926 0.922 0.919 0.915 0.909 0.909 0.905 0.907 0.882 4:8 0.986 0.985 0.977 0.977 0.955 0.904 0.923 0.926 0.924 0.921 0.916 0.915 0.912 0.912 0.913 0.895 5.2 0.994 0.996 0.983 0.990 0.968 0.971 0.965 0.953 0.944 0.938 0.931 0.924 0.924 0.923 0.923 0.927 0.909 6.0 1.000 1.000 0.996 0.999 0.980 0.982 0.974 0.969 0.955 0.944 0.932 0.923 0.923 0.921 0.904 0.933 0.916 0.955 0.947 0.946 0.923 0.921 0.966 0.955 0.947 0.946 0.922	3.9	0.951	0.948	0.934	0.940	0.915	0.926	0.921	0.910	0.907	0.904	0.902	0.900	0.900	0.896	0.895	0.893	0.892	0.874
4.5 0.977 0.974 0.960 0.964 0.943 0.948 0.930 0.926 0.922 0.917 0.915 0.909 0.909 0.909 0.909 0.901 0.910 0.915 0.901 0.902 0.913 0.911 0.921 0.910 0.921 0.913 0.921 0.921 0.912 0.912 0.921 0.921 0.912 0	4.2	0.964	0.961	0.948	0.953	0.929	0.937	0.933	0.920	0.917	0.913	0.911	0.910	0.908	0.902	0.903	0.899	0.899	0.882
4.8 0.986 0.987 0.977 0.977 0.955 0.960 0.953 0.930 0.926 0.921 0.921 0.913 0.912 0.913 0.912 0.913 0.912 0.913 0.924 0.924 0.921 0.913 0.924 0.921 0.912 0.923 0.924 0	4.5	0.977	0.974	0.960	0.964	0.943	0.948	0.943	0.930	0.926	0.922	0.919	0.917	0.915	0.909	0.909	0.905	0.907	0.805
5:2 0:994 0:995 0:995 0:994 0:995 0:951 0:951 0:952 0:931 0:952 0:932 0:922 0:923 0:927 0:909 5:6 0:999 0:998 0:999 0:998 0:999 0:989 0:991 0:985 0:974 0:969 0:952 0:947 0:943 0:943 0:931 0:922 0:923 0:925 0:955 0:951 0:947 0:946 0:928 0:976 0:945 0:947 0:945 0:947 0:945 0:947 0:946 0:947 0:946 0:947 0:945 0:947 0:946 0:955 0:951 0:945 0:952 0:933 0:948 0:947	4.8	0.986	0.985	0.972	0.977	0.955	0.960	0.953	0.940	0.936	0.930	0.926	0.924	0.921	0.910	0.915	0.912	0.913	0.902
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	5.6	0.000	0.008	0.007	0.006	0.908	0.971	0.903	0.955	0.948	0.941	0.933	0.942	0.940	0.932	0.932	0.923	0.927	0.909
6:4 0.999 1.000 0.995 0.995 0.992 0.982 0.978 0.971 0.964 0.959 0.947 0.945 0.940 0.922 8:8 1.000 0.998 0.997 0.996 0.989 0.997 0.991 0.966 0.962 0.955 0.951 0.947 0.946 0.928 7.2 1.000 0.999 0.998 0.997 0.994 0.991 0.986 0.972 0.969 0.961 0.958 0.953 0.952 0.933 7.6 1.000 0.999 0.997 0.994 0.990 0.998 0.972 0.969 0.968 0.972 0.970 0.966 0.963 0.947 0.946 0.953 0.952 0.933 7.6 1.000 0.999 0.997 0.995 0.985 0.970 0.972 0.970 0.966 0.963 0.947 0.972 0.970 0.957 0.963 0.997 0.991 0.985 0.997 0.991 0.985 0.992 0.984 0.997 0.992 0.998 0.997 0.992	5·0 6·0	1.000	1.000	0.992	0.999	0.989	0.991	0.985	0.974	0.969	0.961	0.956	0.950	0.948	0.940	0.939	0.934	0.933	0.916
8.8 1.000 0.998 0.997 0.996 0.989 0.979 0.971 0.966 0.962 0.955 0.951 0.947 0.946 0.928 7.2 1.000 0.999 0.998 0.993 0.991 0.986 0.978 0.972 0.969 0.961 0.958 0.953 0.952 0.933 7.6 1.000 0.999 0.997 0.994 0.990 0.985 0.979 0.969 0.961 0.958 0.953 0.952 0.933 8.0 1.000 0.999 0.997 0.994 0.990 0.997 0.995 0.985 0.979 0.967 0.965 0.997 0.966 0.963 0.940 8.0 1.000 0.999 0.997 0.997 0.992 0.983 0.984 0.981 0.965 0.997 0.975 0.965 0.997 0.975 0.965 0.991 0.988 0.984 0.981 0.965 0.991 0.988 0.984 0.981 0.965 0.991 0.995 0.991 0.998 0.997 0.995 0.993	6·4	1 000	1 000	0.999	1.000	0.995	0.995	0.992	0.982	0.978	0.971	0.964	0.959	0.956	0.947	0-945	0.940	0.940	0.922
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	8.8			1.000		0.998	0.997	0.996	0.989	0.986	0.979	0.971	0.966	0.962	0.955	0.951	0.947	0.946	0.928
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	7.2					1.000	0.999	0.998	0.993	0-991	0.986	0.978	0.972	0.969	0.961	0.958	0.953	0.952	0.933
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	7.6						1.000	0.999	0.997	0.994	0.990	0.985	0.979	0.975	0.968	0.965	0.959	0.957	0.940
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	8.0							1.000	1.000	0.997	0.995	0.989	0.080	0.980	0.972	0.970	0.900	0.903	0.940
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	8.2								1.000	1.000	1.000	0.992	0.989	0.991	0.985	0.982	0.979	0.975	0.959
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	9.5										1 000	0.998	0.997	0.995	0.991	0.988	0.984	0.981	0.965
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	10.0											0.999	0.998	0.997	0.994	0.992	0.989	0.986	0.970
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	10.5											1.000	0.999	0.998	0.996	0.995	0.993	0.990	0.976
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	11.0												1.000	0.999	0.998	0.997	0.996	0.993	0.982
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	11.5													1.000	0.999	0.998	0.009	0.007	0.002
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	12.0														1.000	1.000	0.998	0.997	0.993
13.5 1.000 1.000	12.5															1.000	1-000	0.999	0.999
	13.5																	1.000	1.000

TABLE 1 (Cont.)

X(mms)	0	12.7	25.4	38.1	50.8	63.5	76.2	GRA 88-9	DIENT (101-6	C = 0.000 114.3	127.0	139.7	152.4	165-1	177.8	100.5	203.2	215.0
<u>.</u>	2.57	2.61	2.58	2.61	2.61	2.67	2.72	2.77	7.01	2.00		2 01	2.05	2 10	2.12			
R_{θ}	15600	15000	17100	16100	18400	16500	16400	17100	16700	16300	16400	16300	16300	16800	3.13	3.17	3.22	3.24
$\tilde{T_{w}}/T_{1}$	2.242	2.272	2.278	2.313	2.291	2.374	2.452	2.478	2.551	2.586	2.670	2.730	2.780	2.822	2.806	2.702	13900	18500
									2 3 3 1	2 500	2 010	2 7 50	2 709	2 852	2.800	2.192		
Y (mms)	1/11	I/I ₁	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1
0.1	1.903	1.872	1.916	1.939	1.918	1.963	1.980	2.015	2.039	2.101	2.131	2.181	2.201	2.262	2.259	2.200	2.253	2.221
0.2 0.3	1.747	1.736	1.753	1.039	1.759	1.042	1.057	1.894	1.939	1.998	1.999	2.048	2.072	2.141	2.132	2.083	2.152	2.155
0.4	1.698	1.690	1.701	1.709	1.702	1.724	1.707	1.745	1.773	1.792	1.803	1.860	1.803	2.028	2.035	2.000	2.039	2.004
0.5	1.657	1.647	1.653	1.667	1.661	1.676	1.666	1.658	1.720	1.736	1.751	1.801	1.827	1.881	1.902	1.868	1.973	1.030
0.6	1.624	1.612	1.621	1.629	1.628	1.638	1.636	1.658	1.679	1.685	1.705	1.754	1.779	1.818	1.855	1.821	1.863	1.871
0.8	1.569	1.551	1.569	1.573	1.581	1.585	1.583	1.608	1.620	1.632	1.639	1.687	1.703	1.740	1.781	1.750	1.793	1.795
1.0	1.525	1.518	1.533	1.533	1.544	1.541	1.548	1.568	1.579	1.593	1.604	1.636	1.654	1.686	1.732	1.698	1.736	1.735
1.2	1.494	1.485	1.502	1.501	1.514	1.510	1.518	1.536	1.552	1.561	1.569	1.591	1.609	1.648	1.694	1.654	1-688	1.688
1.4	1.432	1.433	1.451	1.472	1.469	1.479	1.494	1.505	1.518	1.532	1.539	1.557	1.573	1.607	1.658	1.622	1.647	1.647
1.8	1.404	1.300	1.424	1.440	1.403	1.433	1.445	1.480	1.491	1.492	1.512	1.528	1.550	1.578	1.623	1.593	1.613	1.611
2.0	1.379	1.372	1.403	1.389	1.416	1.408	1.443	1.4401	1.4/1	1.464	1.460	1.497	1.502	1.532	1.590	1.503	1.584	1.580
$2\cdot 2$	1.354	1.348	1.378	1.366	1.395	1.384	1.399	1.416	1.427	1.441	1.449	1.461	1.480	1.525	1.542	1.530	1.524	1.522
2.4	1.325	1.325	1.356	1.341	1.375	1.359	1.380	1.395	1.410	1.417	1.427	1.441	1.457	1.478	1.518	1.489	1.497	1.525
2.6	1.297	1.298	1.333	1.315	1.354	1.341	1.362	1.373	1.390	1.397	1-412	1.423	1.439	1.452	1.497	1.466	1.475	1.477
2.8	1.274	1.274	1.306	1.289	1.334	1.318	1.339	1.355	1.369	1.379	1.395	1.404	1.420	1.432	1.476	1.443	1.455	1.453
3.0	1.252	1.248	1.282	1.268	1.314	1.300	1.318	1.335	1.351	1.364	1.375	1.387	1.399	1.417	1.455	1.427	1.440	1.432
3.3	1.170	1.101	1.250	1.233	1.280	1.267	1.289	1.307	1.322	1.335	1.349	1.362	1.378	1.389	1-424	1.400	1.416	1.408
3.0	1.144	1.148	1.180	1.172	1.249	1.242	1.201	1.280	1.296	1.309	1.325	1.334	1-355	1.365	1.402	1.375	1.387	1.387
4-2	1.109	1.118	1.147	1.141	1.184	1.188	1.201	1.238	1.272	1.267	1.302	1.313	1.332	1.345	1.383	1.352	1.364	1.366
4.5	1.076	1.085	1.147 1.118	1.111	1.154	1.158	1.177	1.205	1.240	1.232	1.258	1.267	1.200	1.325	1.301	1.332	1.342	1.341
4.8	1.049	1.054	1.084	1.083	1.129	1.130	1.152	1.180	1.199	1.217	1.236	1.200	1.270	1.783	1.340	1.202	1.207	1.301
5.2	1.022	1.022	1.053	1.041	1.094	1.099	1.124	1.149	1.168	1.187	1.205	1.219	1.243	1.260	1.292	1.292	1.278	1.276
5.6	1.007	1.010	1.026	1.022	1.061	1.069	1.090	1.118	1.138	1.160	1.178	1.195	1-215	1.237	1.266	1.260	1.252	1.254
6.0	1.001	1.004	1.011	1.010	1.035	1.043	1.063	1.090	1.110	1.135	1.154	1.170	1.193	1.211	1.241	1-225	1.233	1.231
6.4	1.000	1.000	1.002	1.004	1.019	1.024	1.041	1.064	1.084	1.106	1.131	1.145	1.166	1.189	1.216	1.202	1.211	1.212
0.8			1.000	1.002	1.009	1.014	1.022	1.040	1.064	1.081	1.104	1.124	$1 \cdot 144$	1.165	1.194	1.181	1.188	1.194
7.6				1.000	1.000	1.007	1.006	1.023	1.039	1.059	1.080	1.100	1.122	1.145	1.173	1.162	1.168	1.174
8.0					1.000	1.002	1.000	1.005	1.010	1.026	1.042	1.059	1.104	1.123	1.153	1.142	1.153	1.155
8.5						1.000	1.002	1.001	1.004	1.014	1.026	1.027	1.052	1.007	1.107	1.119	1.133	1.140
9.0							1 000	1.000	1.004	1.007	1.015	1.021	1.037	1.062	1.087	1.077	1.000	1.100
9.5								1 000	1 000	1.001	1.005	1.013	1.026	1.040	1.064	1.058	1.070	1.084
10.0										1.000	1.002	1.004	1.015	1.024	1.046	1.042	1.052	1.064
10-5											1.001	1.002	1.010	1.015	1.031	1.026	1.037	1.049
11.0											1.000	1.001	1.002	1.009	1.021	1.018	1.026	1.038
11.5												1.000	1.001	1.004	1.014	1.010	1.015	1.031
12.0													1.000	1.002	1.004	1.006	1.005	1.024
12.5														1.000	1.000	1.003	1.004	1.018
13.5																1.001	1.000	1.014
14.0																1.000		1.010
15.0																		1.006
16.0																		1.003
· 7.()																		1.001

								GRAD	IENT C	-0.001							
X(mms)	0	12.7	25•4	38.1	50.8	63.5	76-2	88-9	101.6	114.3	127.0	139.7	152.4	165.1	177.8	190.5	203.2
<u>.</u>	2.55	2.55	2.59	2.59	2.61	2.67	2.74	2.80	2.85	2.89	2.93	2.97	3.02	3.05	3.08	3.15	3.18
θ (mms)	0.529	Ō-551	0.560	0.600	0.648	0.644	0.653	0.663	0.658	0.719	0.716	0.755	0.787	0.832	0.874	0.885	0.885
δ^x (mms)	2.268	2.325	2.426	2.532	2.809	2.818	2.892	3.024	3.070	3.418	3-500	3.692	3.927	4.198	4.632	4.714	4.774
Y(mms)	U/U_1	U/U_1	U/U_1	U/U_1	U/U_1	U/U_1	U/U_1	U/U_1	U/U_1	<i>U</i> / <i>U</i> ₁							
0.1	0.442	0.435	0.446	0.475	0.433	0.449	0.478	0.481	0.470	0.443	0.473	0-465	0.481	0-476	0.450	0.461	0.499
0.2	0.492	0.489	0.492	0.506	0.467	0.500	0.532	0.533	0.520	0.491	0.511	0.496	0.509	0.498	0.470	0.484	0.505
0.3	0.524	0.529	0.534	0.542	0.499	0.545	0.572	0.576	0.554	0.534	0.546	0.539	0.532	0.551	0.522	0.532	0.524
0.4	0.552	0.559	0.561	0.569	0.532	0.572	0.596	0.603	0.585	0.570	0.604	0.500	0.582	0.575	0.552	0.553	0.534
0.2	0.574	0.583	0.584	0.592	0.568	0.596	0.618	0.645	0.621	0.610	0.625	0.616	0.202	0.594	0.573	0.575	0.545
0.6	0.593	0.601	0.602	0.610	0.622	0.645	0.670	0.674	0.668	0.656	0.658	0.651	0.637	0.630	0.617	0.615	0.566
0.8	0.625	0.659	0.659	0.662	0.647	0.664	0.680	0.604	0.603	0.681	0.688	0.679	0.666	0.659	0.647	0.644	0.593
1.2	0.677	0.670	0.678	0.681	0.665	0.004	0.009	0.074 0.711	0.711	0.702	0.708	0.703	0.687	0.680	0.670	0.666	0.620
1.4	0.608	0.608	0.695	0.697	0.683	0.699	0.720	0.725	0.728	0.717	0.723	0.716	0.704	0.698	0.685	0.682	0.643
1.6	0.030	0.0716	0.711	0.712	0.000	0.709	0.732	0.737	0.741	0.732	0.736	0.729	0.717	0.715	0.699	0.697	0.665
1.8	0.734	0.733	0.727	0.727	0.715	0.724	0.742	0.751	0.753	0.745	0.748	0.743	0.741	0.727	0.715	0.713	0.686
2.0	0.750	0.749	0.742	0.742	0.729	0.738	0.753	0.763	0.764	0.754	0.758	0.754	0.754	0.740	0.727	0.727	0.707
2.2	0.768	0.764	0.758	0.756	0.741	0.755	0.765	0.772	0.774	0.764	0.768	0.767	0.759	0.753	0.739	0.739	0.726
2.4	0.784	0.779	0.772	0.769	0.755	0.767	0.777	0.783	0.785	0.774	0.779	0.778	0.767	0.765	0.750	0.750	0.741
2.6	0.800	0.796	0.787	0.783	0.769	0.779	0.787	0.790	0.796	0.783	0.789	0.786	0.778	0.792	0.771	0.771	0.772
2.8	0.816	0.812	0.801	0.797	0.780	0.790	0.796	0.793	0.806	0.793	0.799	0.794	0.707	0.700	0.791	0.780	0.785
3.0	0.832	0.829	0.814	0.811	0.790	0:800	0.805	0.810	0.815	0.803	0.810	0.802	0.200	0.802	0.707	0.793	0-798
3.3	0.858	0.850	0.837	0.831	0.807	0.818	0.819	0.824	0.871	0.877	0.830	0.827	0.809	0.814	0.803	0.802	0.810
3.6	0.880	0.871	0.857	0.849	0.845	0.855	0.874	0.843	0.854	0.827	0.841	0.837	0.831	0.825	0.805	0.813	0.822
3.9	0.022	0.012	0.001	0.887	0.862	0.868	0.864	0.861	0.866	0.848	0.852	0.848	0.842	0.835	0.825	0.826	0.832
4.2	0.922	0.912	0.901	0.003	0.880	0.883	0.878	0.876	0.876	0.860	0.863	0.858	0.851	0.844	0.834	0.835	0.842
4.8	0.955	0.944	0.938	0.920	0.895	0.898	0.891	0.888	0.887	0.869	0.873	0.867	0.861	0.853	0.843	0.844	0.851
5.2	0.974	0.964	0.960	0.941	0.918	0.916	0.908	0.902	0.901	0.885	0.886	0.879	0.874	0.865	0.855	0.856	0.863
5.6	0.986	0.979	0.976	0.961	0.936	0.933	0.926	0.918	0.917	0.899	0.900	0.891	0.886	0.877	0.866	0.866	0.873
6.0	0.994	0.992	0.989	0.975	0.955	0.950	0.940	0.933	0.930	0.912	0.912	0.901	0.897	0.887	0.877	0.878	0.884
6.4	0.998	0.996	0.994	0.987	0.971	0.966	0.955	0.948	0.944	0.924	0.925	0.912	0.908	0.897	0.888	0.886	0.893
6.8	1.000	1.000	0.998	0.991	0.985	0.979	0.970	0.961	0.957	0.936	0.936	0.925	0.919	0.907	0.006	0.890	0.902
7.2			1.000	0.999	0.994	0.987	0.981	0.972	0.969	0.949	0.946	0.935	0.027	0.025	0.900	0.013	0.911
7.6				1.000	0.997	0.994	0.992	0.000	0.007	0.900	0.930	0.944	0.937	0.925	0.915	0.921	0.927
8.0					1.000	1.000	0.994	0.004	0.003	0.970	0.900	0.955	0.958	0.946	0.933	0.932	0.935
8.2					1.000	1.000	0.997	0.007	0.995	0.988	0.985	0.976	0.967	0.955	0.945	0.941	0.943
9.0							1.000	1.000	0.999	0.993	0.991	0.983	0.975	0.964	0.954	0.950	0.951
10.0							1 000	1 000	1.000	0.997	0.996	0.989	0.983	Q·972	0.962	0.958	0.958
10.5										1.000	0.998	0.994	0.988	0.980	0.970	0.966	0.964
11.0											1.000	0.997	0.992	0.986	0.977	0.972	0.970
11.5												0.999	0.997	0.994	0.990	0.984	0.980
12.0												1.000	0.998	0.996	0.993	0.989	0.985
12.5													0.999	0.998	0.996	0.993	0.988
13.0													1.000	0.999	0.000	0.007	0.004
13.5														1.000	0.000	1,000	0.994
14.0															1.000	1.000	0.999
15.0															1 000		1.000
10.0																	
1/10																	

TABLE 1 (Concluded)

X(mms)	0	12.7	25-4	38.1	50.8	63.5	76.2	88·9	101.6	114.3	127.0	139.7	152.4	165-1	177.8	190.5	203
M_1	2.55	2.55	2.59	2.59	2.61	2.67	2.74	2.80	2.85	2.89	2.93	2.97	3.02	3.05	3.08	3.15	3.18
$\frac{R_{\theta}}{T_w}/T_1$	29000 2·195	$30000 \\ 2.175$	30200 2·237	32100 2·225	35100 2·279	33200 2·324	32300 2·386	32000 2·453	30800 2·500	32700 2·540	32300 2·607	33000 2·642	33600 2·690	34700 2·725	$36900 \\ 2.810$	35400 2·846	342 2·8:
Y(mms)	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/T_1	T/ 2
0.1	1.973	1.960	1.996	1.960	2.044	2.070	2.085	2.135	2.189	2.254	2.269	2.309	2.322	2.356	2.473	2.489	2.4
0.2	1.909	1.892	1.935	1.913	1.988	2.002	2.001	2.049	2.099	2.178	2.195	2.241	2.260	2.303	2.421	2.430	2.4
0-3	1.862	1.836	1.881	1.859	1.940	1.931	1.931	1.971	2.034	2.104	2.123	2.159	$2 \cdot 207$	2.248	2.347	2.376	2.3
0.4	1.821	1.794	1.837	1.814	1.897	1.880	1.884	1.914	1.974	2-035	2.056	$2 \cdot 104$	2.145	$2 \cdot 189$	2.286	2.318	2.3
0.5	1.787	1.758	1.802	1.776	1.843	1.838	1.837	1.864	1.926	1.979	2.005	2.047	2.096	2.138	2.238	2.267	2.3
0.6	1.754	1.728	1.772	1.743	1.807	1.793	1.795	1.824	1.878	1.933	1.955	1.991	2.046	2.092	2.187	2.215	2.2
0.8	1.698	1.663	1.715	1.693	1.746	1.736	1.729	1.758	1.799	1.850	1.873	1.907	1.959	2.003	2.084	2.114	2.2
1.0	1.649	1.635	1.674	1.648	1.700	1.696	1.684	1.712	1.740	1.790	1.805	1.837	1.889	1.928	2.005	2.038	2.1
1.2	1.613	1.600	1.637	1.618	1.665	1.658	1.647	1.672	1.695	1.741	1.754	1.778	1.836	1.874	1.944	1.980	2.0
1.4	1.581	1.571	1.604	1.587	1.633	1.628	1.618	1.642	1.656	1.704	1.715	1.745	1.793	1.829	1.902	1.933	$\overline{2}\cdot 0$
1.6	1.552	1.543	1.578	1.563	1.604	1.628	1.595	1.619	1.628	1.669	1.686	1.716	1.765	1 786	1.865	1.893	1.9
1.8	1.524	1.516	1.552	1.539	1.580	1.606	1.574	1.590	1.603	1.638	1.659	1.682	1.705	1.754	1.825	1.851	1.9
2.0	1.497	1.490	1.526	1.514	1.555	1.559	1.554	1.568	1.578	1.619	1.632	1.654	1.673	1.723	1.791	1.812	1.8
2.2	1.466	1.464	1.499	1.489	1.534	1.528	1.531	1.544	1.553	1.597	1.606	1.625	1.658	1.692	1.759	1.780	1.8
2.4	1.439	1.442	1.473	1.467	1.511	1.503	1.507	1.520	1.506	1.552	1.557	1.576	1.613	1.636	1.699	1.722	1.7
2.6	1.413	1.413	1.448	1.445	1.486	1.479	1.487	1.506	1.484	1.527	1.535	1.555	1.589	1.614	1.672	1.695	1.7
2.8	1.386	1.384	1.421	1.421	1.467	1.459	1.469	1.498	1.464	1.504	1.515	1.537	1.566	1.595	1.648	1.669	1.6
3.0	1.358	1.358	1.399	1.394	1.448	1.442	1.449	1.464	1.432	1.476	1.487	1.506	1.536	1.565	1.619	1.631	1.6
3.3	1.318	1.318	1.357	1.357	1.416	1.407	1.426	1.434	1.405	1.450	1.460	1.476	1.509	1.535	1.591	1.606	1.5
3.6	1.276	1.283	1.319	1.327	1.379	1.372	1.394	1.418	1.377	1.425	1.432	1.450	1.478	1.507	1.561	1.576	1.5
3.9	1.234	1.244	1.278	1.290	1.344	1.340	1.365	1.396	1.350	1.400	1.405	1.423	1.451	1.478	1.531	1.540	1.5
4.2	1.195	1.210	1.235	1.258	1.312	1.309	1.333	1.355	1.325	1.375	1.382	1.397	1.427	1.451	1.503	1.515	1.5
4.5	1.158	1.177	1.197	1.227	1.278	1.280	1.301	1.319	1.302	1.352	1.358	1.376	1.401	1.430	1.480	1.490	1.4
4.8	1.122	$1 \cdot 144$	1.162	1.192	1.247	1.249	1.274	1.294	1.268	1.312	1.325	1.346	1.365	1.399	1.444	1.455	1.4
5.2	1.076	1.100	1.115	1.150	1.204	1.213	1.238	1.262	1.230	1.281	1.293	1.316	1.334	1.366	1.415	1.425	1.4
5.6	1.042	1.064	1.073	1.107	1.159	1.174	1.200	1.223	1.198	1.250	1.261	1.287	1.308	1.340	1.384	1.391	1.3
6.0	1.016	1.031	1.035	1.071	1.118	1.135	1.166	1.187	1.168	1.220	1.230	1.258	1.281	1.315	1.354	1.366	1.34
6.4	1.001	1.011	1.011	1.039	1.079	1.097	1.130	1.153	1.134	1.188	1.202	1.228	1.250	1.285	1.330	1.338	1.32
6.8	1.000	1.004	1.005	1.024	1.044	1.063	1.093	1.120	1.104	1.160	1.174	1.198	1.222	1.257	1.306	1.310	1.29
7.2		1.000	1.000	1.006	1.022	1.039	1.060	1.092	1.075	1.130	1.145	1.172	1.197	1.233	1.278	1.283	1.2
7.6				1.000	1.008	1.022	1.032	1.065	1.050	1.100	1.120	1.147	1.174	1.207	1.253	1.259	1.24
8.0					1.002	1.009	1.024	1.044	1.034	1.068	1.090	1.116	1.143	1.178	1.224	1.228	1.21
8.5					1.000	1.004	1.010	1.023	1.017	1.044	1.064	1.087	1.114	1.149	1.194	1.201	1.19
9.0						1.002	1.002	1.010	1.005	1.025	1.042	1.058	1.090	1.121	1.165	1.175	1.16
9.5						1.000	1.001	1.004	1.003	1.012	1.025	1.037	1.068	1.097	1.139	1.148	1.14
10.0							1.000	1.001	1.002	1.004	1.015	1.022	1.049	1.073	1.114	1-127	1.13
10.5								1.000	1.000	1.000	1.011	1.013	1.033	1.052	1.093	1.107	1.11
11.0											1.003	1.007	1.021	1.038	1.073	1.084	1.09
11.5											1.001	1.005	1.012	1.019	1.055	1.063	1.07
12.0											1.000	1.003	1.007	1.012	1.038	1.045	1.06
12.5												1.000	1.003	1.004	1.028	1.030	1.04
13.0													1.000	1.001	1.020	1.018	1.03
13.5														1.000	1.014	1.010	1.02
14.0															1.005	1.001	1.00
1															1 001	1 000	

TABLE 2Boundary Layer Parameters

Gradie P _o = 4.	nt A , m 12 x 10 ⁵	= 0 . Nm ⁻² , T _o	= 291.9°K	:					
X(mm)	$\delta_i^{\star}(mm)$	$\Theta_i(mm)$	ε _i (mm)	E(mm)	Т°К	Cfx10 ⁶	mx10	Fx10	-ß
0 12.7 25.4 38.1 50.8 63.5 76.2 88.9 101.6 114.3 127.0 139.7 152.4 165.1 177.8	0.849 0.859 0.926 0.910 0.916 0.923 0.923 0.954 0.987 1.012 1.031 1.058 1.140 1.088	0.614 0.628 0.627 0.687 0.682 0.683 0.672 0.707 0.737 0.757 0.755 0.800 0.823 0.880 0.849	1.087 1.117 1.118 1.227 1.223 1.223 1.215 1.280 1.338 1.372 1.426 1.454 1.499 1.597 1.547	0.759 0.781 0.776 0.863 0.858 0.852 0.846 0.901 0.937 0.950 0.989 0.997 1.026 1.097 1.057	289.6 289.7 289.8 289.9 290.0 290.1 290.2 290.2 290.2 290.2 290.1 290.0 289.9 289.8 289.7 289.6	$1530 \\ 1520 \\ 1510 \\ 1535 \\ 1565 \\ 1565 \\ 1550 \\ 1550 \\ 1550 \\ 1550 \\ 1555 \\ 1525 \\ 1525 \\ 1515 \\ 1505 \\ 1005 \\ $	000000000000000000000000000000000000000	000000000000000000000000000000000000000	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
Gradie P _o = 5.	nt A , m 15 x 10 ⁵	m = 0.001 Nm ⁻² , T _o =	294.1°K						
X(mm)	$\delta_i^{\star}(mm)$	$\Theta_{i}(mm)$	$\epsilon_i(mm)$	E(mm)	ТоК	CfxlO ⁵	mx10 ⁶	Fx10	6
0 12.7 25.4 38.1 50.8 63.5 76.2 88.9 101.6 114.3 127.0 139.7 152.4 165.1	1.340 1.356 1.271 1.403 1.388 1.588 1.518 1.581 1.579 1.666 1.661 1.829 1.811	0.872 0.883 0.870 0.963 0.968 1.008 1.071 1.133 1.142 1.207 1.221 1.341 1.382	1.483 1.503 1.492 1.535 1.666 1.684 1.760 1.872 1.988 2.014 2.127 2.162 2.368 2.470	0.987 1.008 1.039 1.118 1.112 1.165 1.230 1.319 1.333 1.402 1.400 1.568 1.693	289.8 289.7 289.7 289.6 289.6 289.6 289.5 289.5 289.5 289.4 289.4 289.3 289.3 289.3 289.2 289.2	83 82 81 83 83 78 75 75 75 75 73 71 68 70 72	1020 1020 1020 1025 1031 1036 1042 1053 1058 1064 1056 1041	102 102 107 109 115 121 127 129 135 140 146 139 127	0000614336089132
Gradie $P_0 = 5$.	nt A , m 15 x 10 ⁵	m = 0.002 Nm ⁻² , T _o =	291.9°K						
X(mm)	$\delta_i^{\star}(mm)$	$\Theta_i(mm)$	$\epsilon_i(mm)$	£(mm)	Т°К	Cfxl0 ⁵	mx10 ⁶	Fx10	6
0 12.7 25.4 38.1 50.8 63.5 76.2 88.9 101.6 114.3 127.0 139.7	1.744 1.801 1.915 1.974 2.043 2.222 2.205 2.249 2.318 2.593	1.037 1.092 1.164 1.218 1.268 1.364 1.364 1.472 1.489 1.535 1.572 1.734	1.717 1.814 1.950 2.052 2.146 2.196 2.518 2.563 2.650 2.708 2.977	$1.102 \\ 1.163 \\ 1.254 \\ 1.331 \\ 1.387 \\ 1.406 \\ 1.510 \\ 1.621 \\ 1.639 \\ 1.694 \\ 1.706 \\ 1.867 \\ 1.86$	290.7 290.6 290.4 290.3 290.2 290.1 290.0 289.8 289.7 289.6 289.5 289.4	47 46 47 44 47 44 49 38 36 35	1990 1990 1990 1995 2001 2006 2012 2017 2023 2028 2034	199 199 208 215 227 237 241 253 264 271 280	0 0 0 0 0 1 1 1 7 4 2 5 9

TABLE 2 (Cont.)

Gradie $P_o = 3$.	nt B , m 08 x 10 ⁵	= 0. Nm ⁻² , T _o =	294.1°K						
X(mm)	$\delta_i^{\star}(mm)$	Θ_{i} (mm)	$\epsilon_i(mm)$	E(mm)	Т°К	Cfx10 ⁶	mxlO	F x10	ß
0 12.7 25.4 38.1 50.8 63.5 76.2 88.9 101.6 114.3 127.0 139.7 152.4 165.1 177.8	0.965 0.930 0.875 0.908 0.932 0.978 1.003 0.992 1.102 1.046 1.135 1.142 1.150 1.307	0.707 0.686 0.654 0.658 0.680 0.710 0.729 0.730 0.799 0.765 0.822 0.832 0.844 0.940	1.253 1.220 1.153 1.167 1.204 1.253 1.287 1.293 1.406 1.352 1.446 1.4467 1.491 1.648	0.888 0.809 0.809 0.821 0.810 0.837 0.913 0.923 1.004 0.959 1.051 1.073 1.094 1.203	291.6 291.7 291.7 291.8 291.8 291.9 292.0 291.9 291.8 291.9 291.8 291.7 291.7 291.7 291.6	1885 1590 1605 1620 1585 1550 1515 1490 1465 1445 1445 1430 1420 1410 1400 1395	000000000000000000000000000000000000000	00000000000000000000000000000000000000	0 0 0 .49 .52 .55 .55 .608 .615 .62 .84
Gradie $P_0 = 3.$	nt B , m 08 x 10 ⁵	= 0.001 Nm ⁻² , T _o =	289.1°K						
X(mm)	$\delta_i^*(mm)$	$\theta_i(mm)$	$\mathcal{E}_{i}(mm)$	E(mm)	Т°К	Cfx10 ⁵	mx10 ⁶	Fx10 ⁶	
0 12.7 25.4 38.1 50.8 63.5 76.2 88.9 101.6 114.3 127.0 139.7 152.4 165.1 177.8	1.535 1.567 1.383 1.569 1.656 1.760 1.789 1.858 1.858 1.907 2.100 2.016 2.012 2.273	$\begin{array}{c} 1.016\\ 1.013\\ 0.935\\ 1.026\\ 1.035\\ 1.083\\ 1.133\\ 1.152\\ 1.205\\ 1.215\\ 1.243\\ 1.326\\ 1.309\\ 1.334\\ 1.426\end{array}$	1.733 1.717 1.605 1.743 1.751 1.835 1.909 1.940 2.036 2.056 2.100 2.216 2.211 2.267 2.380	1.165 1.143 1.066 1.155 1.149 1.282 1.317 1.393 1.406 1.439 1.544 1.543 1.589 1.672	285.0 284.9 284.9 284.7 284.7 284.7 284.6 284.6 284.5 284.4 284.4 284.3 284.3 284.2 284.2 284.2 284.2	91 92 992 998 8866 887 887 887 887	$\begin{array}{c} 1030\\ 1030\\ 1030\\ 1030\\ 1022\\ 1014\\ 1005\\ 997\\ 989\\ 980\\ 972\\ 964\\ 956\\ 948\\ 940\\ \end{array}$	1030 1030 996 975 944 907 883 866 838 811 762 770 759 702	
Gradie P _o = 3.	nt B , m 08 x 10 ⁵	= 0.002 Nm ⁻² , T _o =	290.2°K						
X(mm)	$\delta_i^x(mm)$	$\theta_i(mm)$	$\ell_i(mm)$	E(mm)	Т ^о К	Cfx10 ⁵	mx10 ⁶	Fx10 ⁶	
0 12.7 25.4 38.1 50.8 63.5 76.2 88.9 101.6 114.3 127.0 139.7 152.4 165.1 177.8	2.144 2.147 2.241 2.334 2.485 2.559 2.692 2.730 2.818 2.848 3.089 3.313 2.985 3.141 3.988	1.281 1.267 1.346 1.379 1.451 1.493 1.543 1.598 1.668 1.668 1.686 1.784 1.850 1.802 1.869 2.086	2.112 2.081 2.216 2.262 2.370 2.436 2.504 2.606 2.734 2.606 2.734 2.757 2.898 2.982 2.958 3.058 3.308	1.336 1.331 1.412 1.446 1.531 1.578 1.617 1.705 1.820 1.844 1.949 2.047 2.006 2.103 2.310	288.6 288.4 288.3 288.2 288.1 288.0 287.9 287.8 287.7 287.6 287.5 287.4 287.2 287.1 287.0	55555555555555555555555555555555555555	2030 2030 2030 2024 2017 2011 2005 1998 1992 1985 1979 1973 1966 1960	2030 2030 1950 1885 1866 1815 1793 1751 1697 1630 1532 1620 1548 1380	

TABLE 2 (Concluded)

Gradie: P _o = 3.0	nt B , m 08 x 10 ⁵	= 0.003 Nm ⁻² , T _o =	290.2°K						
X(mm)	$\delta_i^{\star}(mm)$	$\Theta_i(mm)$	$\epsilon_i(mm)$	E(mm)	Τ°K	Cfxl0 ⁵	mx10 ⁶	Fx10 ⁶	
0 12.7 25.4 38.1 50.8 63.5 76.2 88.9 101.6 114.3 127.0 139.7 152.4 165.1 177.8	$\begin{array}{c} 2.786\\ 3.012\\ 3.027\\ 3.401\\ 3.649\\ 3.842\\ 4.008\\ 4.217\\ 4.595\\ 4.858\\ 5.247\\ 4.961\\ 6.235\\ 6.455\end{array}$	1.552 1.634 1.680 1.778 1.900 1.940 2.007 2.078 2.185 2.277 2.392 2.455 2.555 2.616 2.717	2.503 2.608 2.695 2.811 3.002 3.050 3.143 3.278 3.445 3.554 3.723 3.788 4.015 3.973 4.167	1.568 1.610 1.673 1.744 1.869 1.897 1.991 2.095 2.209 2.315 2.432 2.519 2.684 2.712 2.936	289.8 289.7 289.6 289.5 289.3 289.3 289.2 289.1 289.0 288.9 288.8 288.7 288.6 288.5 288.4	32235432112233346	3030 3030 3030 3022 3014 3005 2997 2981 2973 2965 2956 2948 2940	3030 3030 2879 2879 2652 2652 2652 2453 2453 2258 2393 2265 2393 2393 2395 2395 2395 2395 2395 239	
Gradie $P_o = 4.$	ent C , m 12 x 10 ⁵	$Mm^{-2}, T_{o} =$	290.2°K						
X'(mm)	$\delta_{i}^{\star}(mm)$	$\Theta_{i}(mm)$	$\mathcal{E}_{i}(mm)$	8(mm)	Τ°Κ	Cfxl0 ⁶	mx10	F x10	-ß
0 12.7 25.4 38.1 50.8 63.5 76.2 88.9 101.6 114.3 127.0 139.7 152.4 165.1 177.8 190.5 203.2 215.9	0.784 0.755 0.835 0.790 0.912 0.819 0.815 0.885 0.881 0.914 0.930 0.955 0.967 1.036 1.058 1.101 1.117 1.301	0.581 0.568 0.628 0.699 0.632 0.639 0.695 0.699 0.725 0.745 0.745 0.768 0.782 0.835 0.852 0.889 0.901 1.048	1.037 1.020 1.125 1.068 1.237 1.144 1.163 1.266 1.278 1.326 1.326 1.369 1.413 1.441 1.536 1.567 1.657 1.924	0.727 0.720 0.793 0.749 0.875 0.808 0.819 0.893 0.897 0.929 0.961 0.986 0.999 1.061 1.061 1.138 1.144 1.359	287.6 287.7 287.8 287.9 288.0 288.1 288.2 288.3 288.4 288.5 288.6 288.7 288.8 288.9 289.0 289.1 289.2 289.3	1540 1540 1560 1590 1600 1595 1580 1580 1580 1580 1575 1565 1550 1555 1550 1550 1550 1510 1500	000000000000000000000000000000000000000	000000000000000000000000000000000000000	0 0 0 0 0.57 0.59 0.67 0.70 0.82 0.67 0.70 0.88 0.75 0.64 0.53 0.44 0.36 0.30
$P_0 = 5$	$.84 \times 10^{5}$	$Nm^{-2}, T_{o} =$	289.1°K		•	5	. 6		4
X'(mm)	$\delta_i^{(mm)}$	$\Theta_{i}(mm)$	E _i (mm)	(mm)	TK	Cfx10°	mx10°	Fx10	-
0 12.7 25.4 38.1 50.8 63.5 76.2 88.9 101.6 114.3 127.0 139.7 152.4 165.1 177.8 190.5 203.2	1.162 1.188 1.225 1.266 1.411 1.360 1.355 1.355 1.355 1.498 1.498 1.563 1.642 1.746 1.888 1.910 1.948	0.792 0.816 0.844 0.888 0.975 0.965 0.974 0.995 0.995 1.097 1.097 1.217 1.295 1.389 1.411 1.420	1.365 1.412 1.460 1.546 1.690 1.687 1.719 1.764 1.764 1.949 2.059 2.164 2.301 2.463 2.505 2.510	0.925 0.964 0.980 1.055 1.136 1.138 1.164 1.187 1.180 1.289 1.287 1.359 1.417 1.499 1.573 1.595 1.593	285.1 285.2 285.4 285.5 285.7 285.9 286.1 286.2 286.2 286.2 286.5 286.5 286.7 286.9 287.1 287.2 287.3 287.4 287.5	82 83 83 796 772 685 596 596 596 596 596 596 596 596 596 59	970 970 970 977 985 999 1006 1014 1021 1028 1035 1043 1050 1057	970 970 100 108 110 125 132 138 146 149 160 166 173 184 190	50755105467304849

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FIG. 1. X-Section of Tunnel.



FIG. 2. Design of Pressure Gradients A and C.





FIG. 4. Variation of m and F.



FIG. 5. Gradient B Disturbed Profiles.







FIG. 7. Free-Stream Mach Number Variation.



FIG. 8. Variation of Skin Friction.



FIG. 9. Variation of Skin Friction.



FIG. 10. Variation of Skin Friction.



FIG. 11. Variation of Displacement Thickness.







FIG. 13. Velocity Profiles Gradient A m = 0.











FIG. 17. Velocity Profiles Gradient B m = 0.001.



FIG. 18. Velocity Profiles Gradient B m = 0.002.











FIG. 21. Velocity Profiles Gradient C m = 0.001.

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FIG. 22. Velocity profiles $\beta > 0$, $\nu_{\omega}/U_1 = 0$.



FIG. 23. Velocity Profiles $\beta > 0$, $\nu_{\omega}/U_1 > 0$.



FIG. 24. Velocity Profiles $\beta < 0$, $\nu_{\omega}/U_1 = 0$.



FIG. 25. Velocity Profiles $\beta < 0$, $\nu_{\omega}/U_{1} > 0$.



FIG. 26. Temperature Profiles Gradient A.



FIG. 27. Temperature Profiles Gradient B.



FIG. 28. Temperature Profiles Gradient C.



FIG. 29. Variation of T_0 with y.



FIG. 30. G(u) vs log y⁺ Gradient A m = 0.



FIG. 31. G(u) vs log y⁺ Gradient A m = 0.002.










FIG. 34. G(u) vs log y⁺ Gradient C m = 0.







FIG. 36. The Effect of the Pressure Gradient Term on G(u).



FIG. 37. Variation of π with F Along Plate.



FIG. 38. Variation of B with F.



FIG. 39. Velocity Defects in Gradient B.



FIG. 40. Velocity Defects in Favourable Gradients.



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FIG. 42. Velocity Defects for Positive β Flows.

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