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# The Forces on a Cylinder in Shear Flow By A. Thom, LL.D. 

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# The Forces on a Cylinder in Shear Flow 

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## Summary

An arithmetical solution is obtained for the viscous creeping flow past a circular cylinder on the bottom of a channel roughly two diameters deep. The top of the channel is assumed to be in uniform motion so a shear layer exists in the undisturbed channel. The drag of the cylinder is found to be equivalent to 29 times the floor drag on an area equal to the projected area of the cylinder. The resultant vertical force on the cylinder is zero.

## Introduction.

A solution for the flow past a cylinder at the bottom of a shear layer would enable an estimate to be made of the force produced by tidal currents on a cable lying on the bed of the sea. It was accordingly decided to work through an approximate solution by hand to see what kind of difficulties arise. To reduce the problem to a manageable size it was decided to take the case of a cylinder of diameter $D$ in a passage of depth roughly $2 D$, the roof of the passage being assumed to move at a uniform speed across the cylinder. Only the case of zero Reynolds number has been attempted but, even so, the results may be of interest.

## The Non-Viscous Case.

In order to obtain a grid on which to work the viscous case a Laplacian solution had first to be obtained. This is shown in Fig. 1. It will be seen that matters have been arranged so that an integral equipotential line forms the line of symmetry (at the right) and another runs into the cusp or stagnation point. Elsewhere (Thom and Apelt ${ }^{2}$ ) it is suggested that figures with properties of this kind be called symmetromorphic. The method of obtaining the solution to $\nabla^{2} \psi=0$ for cases like this has been described several times and only the difficulties need be mentioned here. These centre round the cusp. In problems previously worked the corners had definite angles and the function $w=Z^{n}$ was available. With zero angle a suitably simple function was not known and the region had to be subdivided and worked over until it was certain that no error was being spread through the field. In Fig. 2 suppose O to be the apex of the cusp (in the $w=\xi+i \eta$ field). As practically all the work was done with the four-square molecule we need to know the values of $\theta$ to put at $O$ for use in each of the three molecules involved, namely, OBCE, JADF and HOEG. As the size of the molecule shrinks towards zero presumably the values tend to $\pi / 4, \pi / 2$ and $3 \pi / 4$. The values found empirically are:

$$
\begin{array}{rl}
- \text { For } a & =1,0.50 \quad 0.89 \quad 1.38 \\
\text { For } a & =\frac{1}{2}, \\
\text { For } a & 0.55 \\
& =\frac{1}{4},
\end{array}, 0.60 \quad 1.09 \quad 1.531 .61
$$

Having, from the run of the figures and the limiting values just stated, guessed the next value the local subdivision can be made and the previous boundary values adjusted to suit.

[^0]As every round of operations involves finding the conjugate function $(\log 1 / Q)$ the process is long but it is believed that a reasonably good solution has been obtained. Unfortunately the size of the cylinder (which is only known when the solution is complete) is rather large. The radius is $1 \cdot 04$ for a channel width of 4 . As so much work had gone into the production of the grid it was decided to go ahead with the viscous solution. Skeleton details of the Laplacian solution will be found in Table 1. The usual squaring formulae enable any necessary subdivisions to be made.

Viscous Solution, $R=0$.
We write

$$
\nabla^{2} \psi=\zeta, \nabla^{2} \zeta=0
$$

and operate alternately on $\psi$ and $\zeta$. The four-square-molecule formulae were used throughout except when changing to a smaller grid size. This change of size was made for the region of the cusp shown by a rectangle in Table 2. The formulae used are

$$
\begin{aligned}
& 20 \zeta_{0}=4 s_{1}+s_{2} \\
& 20 \psi_{0}=4 S_{1}+S_{2}-6\left(a^{2} / Q^{2}\right) \zeta
\end{aligned}
$$

where $s_{1}$ is the sum of the $\zeta$ values in the centre of the side
$s_{2}$ is the sum of the corner values
$S_{1}$ and $S_{2}$ refer similarly to $\psi$ values and $Q$ is the modulus of the transformation.
The boundary formula (Woods ${ }^{3}$ ) used was

$$
\zeta_{13}=3 Q_{13}{ }^{2}\left(\psi_{A}-\psi_{B}\right) / a^{2}-\frac{1}{2} \zeta_{A}\left(Q_{\mathrm{B}} / Q_{A}\right)^{2}
$$

for the lower boundary. For the upper boundary $\psi_{\mathrm{A}}-\psi_{\mathrm{B}}$ is replaced by $\psi_{\mathrm{A}}-\psi_{\mathrm{B}}-u / Q_{\mathrm{B}}, u$ being the velocity of the moving boundary.

The depth of the passage is 4 and the undisturbed $\psi$ is taken as

$$
\psi_{y}=5 y^{2}
$$

which entails $\zeta=10$ and the speed of the moving top boundary $u=-40$.
The usual boundary troubles presented themselves ( $\mathrm{Thom}^{1}$ ) but by using roughly $\frac{1}{2}$ movement a reasonably good solution was obtained. It could be improved by subdividing a larger area of the field. The results are shown in Table 2.

## The Pressures.

Since $u D \rho / \mu$ is zero and $u$ is finite then $\rho$ is zero and the pressures are found by integrating, e.g. along $\eta=$ const.

$$
p_{\mathrm{A}}-p_{\mathrm{B}}=\mu \int_{\mathrm{A}}^{\mathrm{B}} \frac{\partial \zeta}{\partial \xi} d \eta
$$

Thus $\left(p_{\mathrm{A}}-p_{\mathrm{B}}\right) / \mu$ is the function conjugate to $\zeta$ and the formulae developed elsewhere (Thom and Apelt ${ }^{2}$, Section 5.4) are available.

The pressure drop from $\xi=0$, the top of the cylinder to the extreme left was found to be 89 by integrating along $\eta=2$, so the total drop caused by the cylinder is 178 . An identical value was found by integrating along $\eta=1$. The pressures throughout the field are given along with $\psi$ and $\zeta$ in Table 2 and the conformal net ( $\zeta, p / \mu$ ) is shown in Fig. 4. The pressure and vorticity along the top and bottom passage walls are shown in Fig. 5.

## Forces on the Cylinder.

The pressures round the cylinder are shown plotted on the vertical projection in Fig. 6a. The area gives the resultant horizontal force. Fig. 6b shows the same thing for the vertical forces. From the type of symmetry which obtains it appears that there is no resultant vertical force on the cylinder from the pressures. Evidently there is also no vertical force from the skin drag. The horizontal resultant skin drag is obtained from Fig. 3.

As an overall check consider the total forces acting on the water from the extreme left to the extreme right.
We have:
$\left.\begin{array}{lr}\text { From pressure difference on ends } & -4 \times 178 \mu=-712 \mu \\ \text { From skin drag on passage walls (Fig. 5) } & +104 \mu \\ \text { From pressure on cylinder (Fig. 6) } & +440 \mu \\ \text { From skin drag on cylinder (Fig. 3) } & +167 \mu\end{array}\right\}=+711 \mu$.

This is certainly a better balance than was expected in view of the somewhat rough solution. The total horizontal force $F_{C}$ on the cylinder per foot length is $440 \mu+167 \mu$ or $607 \mu$. The vorticity in the undisturbed flow is 10 so the skin drag on the bottom is $10 \mu$.

Put $F_{B}=$ skin friction on an area equal to 1 foot length of cylinder. The cylinder diameter is 2.07 so

$$
F_{B}=2.07 \times 1 \times 10 \mu=20.7 \mu
$$

Thus our final conclusion is that

$$
F_{C}=29 F_{B}
$$

or the force on the cylinder is equal to the undisturbed friction on an area 29 diameters wide.

## Conclusion.

The force on the cylinder has been found for a somewhat artificial case but with the knowledge gained it ought to be possible to programme the problem with a wider channel and a finite if small Reynolds number. The lack of symmetry introduced with the Reynolds number would produce the lift which is actually found experimentally.

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TABLE 1

| $\eta \xi$ | -8 | $-7$ | -6 | -5 | -4 | -3 | -2 | $-1$ | 0 |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 4 | 0 | 0 | 0 | 0 | 0 | 0 | 0 | 0 | 0 |
|  | , 15 | 32 | 66 | 127 | 222 | 340 | 455 | 537 | 567 |
|  | 629 | 531 | 436 | 345 | 261 | 185 | 118 | 57 | 0 |
|  | 400 | 400 | 400 | 400 | 400 | 400 | 400 | 400 | 400 |
| 3 | 10 | 22 | 44 | 77 | 114 | 128 | 107 | 60 | 0 |
|  | 11 | 24 | 52 | 109 | 208 | 341 | 473 | 564 | 597 |
|  | 628 | 531 | 434 | 341 | 256 | 181 | 115 | 56 | 0 |
|  | 301 | 303 | 306 | 312 | 320 | 329 | 337 | 342 | 344 |
| 2 | 15 | 33 | 73 | 149 | 251 | 296 | 243 | 131 | 0 |
|  | 1 | 2 | 9 | 44 | 155 | 345 | 533 | 649 | 694 |
|  | 627 | 529 | 428 | 331 | 242 | 166 | 104 | 51 | 0 |
|  | 202 | 204 | 209 | 220 | 240 | 260 | 277 | 287 | 291 |
| 1 | 11 | 26 | 64 | 174 | 457 | 582 | 431 | 219 | 0 |
|  | $-10$ | - 24 | - 53 | - 97 | $+145$ | 368 | 671 | 820 | 870 |
|  | 626 | 528 | 421 | 314 | 210 | 137 | 87 | 42 | 0 |
|  | 101 | 103 | 107 | 120 | 154 | 196 | 225 | 240 | 245 |
| 0 | 0 | 0 | 0 | 0 |  | 1095 | 651 | 312 | 0 |
|  | - 15 | - 35 | - 85 | $-240$ |  | + 620 | 955 | 1089 | 1124 |
|  | 625 | 527 | 418 | 300 |  | 92 | 63 | 32 | 0 |
|  | 0 | 0 | 0 | 0 |  | 152 | 186 | 202 | 207 |
|  |  |  |  |  |  |  |  |  |  |

$1000 \theta$
Each square contains $\quad 1000 \operatorname{Ln} Q$
$100 x$
$100 y$

TABLE 2


Grid subdivided in this Region

$$
\begin{array}{lc} 
& \psi \\
\text { Each rectangle contains } & \zeta \\
& p / \mu
\end{array}
$$



Fig. 1.


Fig. 2.


Fig. 3. Skin drag on cylinder.


Fig. 4. Vorticity and pressure.



Fig. 5. Pressure and vorticity on channel walls.


Fig. 6. Pressure round cylinder plotted on its horizontal and vertical projections.

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